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Publication Date

2015-09-01

DOI

10.1016/j.geothermics.2015.05.007

Peer reviewed

1 **Impact of Coupled Heat Transfer and Water Flow on Soil Borehole Thermal Energy**
2 **Storage (SBTES) Systems: Experimental and Modeling Investigation**

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29 Abstract

30 A promising energy storage option is to inject and store heat generated from renewable energy
31 sources in geothermal borehole arrays to form soil-borehole thermal energy storage (SBTES)
32 systems. Although the method is gaining attention, there is no general agreement on the best
33 numerical modeling approach to determine system effectiveness. Although it is widely
34 recognized that the movement of water in liquid and vapor forms is closely coupled to heat
35 transfer process, these coupled processes are often not considered in modeling of SBTES
36 systems. Oftentimes, approaches assume that the soil is a purely conductive medium with
37 constant hydraulic and thermal properties, which may affect SBTES system predictions.
38 Numerical modeling tools that are available to consider these coupled processes, have not been
39 applied to SBTES systems, partly due to the scarcity of field or laboratory data needed to
40 validate these models. Thus, the need exists to systematically compare modeling efforts and
41 experimental observations. The goal of this work is to test different conceptual and mathematical
42 formulations that are used in heat and mass transfer theories and determine their importance to
43 modeling SBTES systems. Such a comparison required the modification of a non-isothermal
44 numerical model that simulates coupled heat, water vapor and liquid water flux through soil and
45 considers non-equilibrium liquid/gas phase change. This model was used to investigate different
46 processes (e.g. considering conduction and convection) and hydraulic and thermal
47 parameterizations (e.g. considering temperature effect on saturation-capillary relation and
48 thermal conductivity) on SBTES system behavior. Precision data under well controlled boundary
49 conditions were generated and results from numerical simulations were compared to
50 observations. Results demonstrate the need to include thermally induced moisture flow in
51 modeling efforts as well as convective heat transfer, especially when modeling unsaturated flow
52 systems. Convective heat flux arising from thermally induced moisture flow leads to greater heat
53 transfer than to conductive flux alone. Comparisons of different formulation validate the need for
54 further research for better modeling accuracy.

55 Key words: SBTES systems, Vadose zone, Convective heat transfer, Phase change, Numerical
56 model, Experimental investigation

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60 **1 Introduction**

61 The rapidly growing gap between consumption and production of energy associated with
62 non-renewable energy sources can be addressed by introducing new cost-effective and clean
63 energy sources such as wind or solar energy. An important issue limiting the implementation and
64 use of renewable sources is energy storage as it is not possible to control the timing of the supply
65 of solar or wind energy in spite of their abundance. For example, unlocking solar energy's full
66 potential becomes relatively complex because its rate of generation is highest mid-day and
67 during summer months, which is offset from the timing of the highest rates of consumption in
68 winter (Pinel et al., 2011). Although a significant amount of research is being devoted to storage
69 of electricity, the storage of heat can be more cost-effective and can be done on different scales.
70 Soil-borehole thermal energy storage (SBTES) systems are one such technology that has been
71 shown to be effective at storing heat collected by solar thermal panels in the summer and
72 extracting it during the winter (Sibbitt et al., 2007; 2012). SBTES systems involve direct
73 circulation of heated fluid through closed-loop geothermal heat exchangers in vertical borehole
74 arrays (Pinel et al., 2011). The geothermal heat exchangers are typically designed with a closer
75 spacing than in ground-source heat pump (GSHP) systems. The subsurface soil and rock
76 provides an excellent medium for heat storage due to their relative abundance along with their
77 relatively high specific heat capacities (Gabrielsson et al. 2000). The top or surface of a SBTES
78 system typically includes a heat insulated cap to reduce thermal losses to the environment
79 (Sibbitt et al., 2007; Pavlov and Olesen, 2012).

80 SBTES systems are attractive from an energy sustainability perspective for many reasons.
81 They usually harvest their energy from renewable energy sources (solar-thermal), are low cost
82 compared to other energy storage systems, and space efficient (i.e. underground) and therefore
83 implementable in many locations (e.g. populated and rural environments). In addition, SBTES
84 systems do not require long-distance energy transportation (localized energy storage), and are
85 scalable from residential- to community- to utility-scale applications.

86 Although pilot programs are successfully utilizing SBTES systems (e.g., Sibbitt et al.,
87 2007), two of the main limitations in large-scale implementation are low system efficiency and
88 high initial installation costs (Hughes, 2008). Efficiency is usually defined as the ratio of the total

89 heat extracted from the SBTES space during discharge or usage periods to the total heat injected
90 into the SBTES space. In general, efficiency depends on the volume and geometry of the SBTES
91 space, number, length and spacing of the boreholes, injection/withdrawal scheme, and
92 mechanical, hydrological, and thermal properties of the soil/ rock (Ohga and Mikoda 2001).
93 Zhang et al., (2012) numerically simulated heat transfer of a SBTES system at Drake Landing
94 Solar Community (DLSC), Alberta, Canada. In their numerical model, they imposed time-
95 dependent heat injection and withdrawal rates measured at the site but did not include variable
96 soil thermal properties and water flow through unsaturated soil. They predicted an energy
97 recovery efficiency of approximately 27% after 10 years. Despite the low efficiency, Sibbitt et
98 al. (2007) found that the SBTES system at DLSC provided over 90% of the heat required for 52
99 single-family homes. However, Zhang et al. (2012) noted that in most SBTES implementations
100 the parameters controlling the efficiency of the system have not been clearly delineated. Pavlov
101 and Olesen (2012) mentioned that although seasonal storage plants are used in some countries
102 (e.g. Germany, Sweden, Canada, etc.), the concept is not widely implemented due to the low
103 efficiency versus initial cost. Increasing the efficiency of these systems will result in a decrease
104 in installment and implementation costs, making the systems more attractive. However, central
105 solar heating plants with seasonal storage require further research, specifically into the storage
106 efficiency and how to best increase the efficiency.

107 An opportunity to enhance the efficiency of SBTES systems is to install them in the
108 vadose zone (the unsaturated zone of soil above the water table) as proposed by McCartney et al.
109 (2013). In this case, it is possible to take advantage of phase change and convective heat transfer
110 phenomena in the pore water to obtain greater heat injection and extraction rates by formation of
111 a convective cell between the borehole heat exchangers making the SBTES system more
112 efficient. Convection can play a major role in transporting energy in unsaturated soils subject to a
113 temperature gradient. For example, when the water around the heat exchanger array is heated, it
114 can vaporize and move towards colder soil regions (i.e. away from the heat source). The water
115 vapor then cools and condenses, releasing latent heat. Depending on the soil properties and
116 initial moisture conditions, the liquid water can move due to the hydraulic gradient back toward
117 the dry soil (i.e. towards the heat source) or accumulate.

118 Numerical modeling of ground heat exchangers can be performed either from the fluid
119 within the U-tube to the borehole wall or from the surface of the borehole to the surrounding soil

120 (Shirazi and Bernier, 2013). In the first category, attention has been paid to modeling heat
121 transfer processes through the fluid and grout inside and within the borehole with the aim of
122 estimating the borehole's thermal resistance and the outlet fluid temperature (e.g. Hellstrom,
123 1991; Zeng et al., 2003; Diao et al., 2004). The grout consists of a mixture of silica sand and
124 bentonite clay with some thermally-enhanced additives, and is used to backfill the borehole to
125 assure maximum heat transfer between the heat exchanger and the borehole (Florides and
126 Kalogirou, 2007). For heat transfer outside of the borehole (i.e. from the surface of the borehole
127 to the surrounding soil), several analytical and numerical models have been proposed, for
128 instance, Kelvin's line source model (Ingersoll and Plass, 1948), the cylindrical source model
129 (Carslaw and Jaeger, 1946), the model of Eskilson (1987), and the finite line source model (Zeng
130 et al., 2002). A few numerical studies are also available in the literature in which both fluid flow
131 inside the borehole and heat transfer outside of the borehole are modeled (e.g. Rees and He,
132 2013). A detailed review of analytical and numerical models for analyzing the thermal behavior
133 inside and outside of the U-tube can be found in the review paper presented by Yang et al.
134 (2010) and Lamarche et al. (2010). It is important to note that none of these analytical models
135 have incorporated coupled heat and mass transfer processes.

136 A common assumption in most SBTES numerical model approaches is to consider the
137 soil as a purely conductive medium with constant hydraulic and thermal properties (Angelotti et
138 al., 2014). Nonetheless, inlet fluid temperatures can create considerable temperature gradients
139 and consequently moisture flow in regions surrounding the heat exchangers (Reuss et al., 1997).
140 In soil science and hydrology literature, there are many experimental/numerical studies that
141 investigate both heat and mass transfer simultaneously. As much understanding to SBTES can
142 be gained from this literature, the next few paragraphs provide a brief review of some of the
143 pertinent studies.

144 A large body of experimental observations is available on the movement of moisture
145 under non-isothermal conditions (e.g., Bouyoucos, 1915; Smith, 1943; Taylor and Gavazza,
146 1954; Philip and de Vries, 1957). Bouyoucos (1915) demonstrated that in a soil column of
147 uniform saturation, water flows from the warmer portion towards the colder portion. His finding
148 was later confirmed in more detail by others (e.g., Smith, 1943; Maclean and Gwatkin 1946),
149 who concluded that for each soil type, there is an optimum degree of saturation in which
150 maximum transfer of water occurs. Several experimental studies have been conducted thereafter

151 in developing hypotheses to describe the mechanisms of thermally induced moisture movement.
152 Gurr et al. (1952) performed a series of experiments on a closed column of loam soil to assess
153 the contribution of liquid water and water vapor flow due to temperature gradients. They showed
154 that water vapor moves toward the colder regions in the soil, condenses, and returns to the
155 warmer regions in the form of liquid water. They theoretically demonstrated that when sufficient
156 moisture exists in the soil, equilibrium is not reached and water circulates continuously. After
157 1960, several papers were published which were mostly devoted to quantifying the importance of
158 thermal gradients on moisture transfer rather than confirming the occurrence of the phenomena
159 (e.g., Cary, 1965; Cassel et al., 1969; Bach, 1992). The purpose of most of these studies was to
160 develop and evaluate the theoretical relationships, validated by experimental results.

161 There are a few works related to the uncertainties associated with hydraulic and thermal
162 properties of the soil with application to GSHP systems. Based on the Philip and de Vries (1957)
163 theory of heat and mass transfer, Reuss et al. (1997) developed a computer model to simulate
164 combined heat and moisture transport for temperatures up to 90 °C. In their study, the model is
165 validated using several laboratory and field scale experiments. They showed that thermal
166 conductivity, heat capacity and overall thermal performance of seasonal heat storage systems
167 highly depend on the soil degree of saturation. However, they did not show the overall
168 importance of including these thermal properties under varying soil saturation conditions in
169 modeling efforts. The study by Leong et al. (1998) showed that the degree of saturation has a
170 crucial effect on performance of GHP systems. Their study suggested that a higher degree of
171 saturation results in higher system efficiency, although variations in degrees of saturation above
172 50% has a relatively insignificant effect. Pavlov and Olesen (2012) discussed that thermal
173 properties (e.g., heat capacity, thermal conductivity) of soil dictate spacing of boreholes that
174 contain heat exchangers. However, they did not consider the effect of soil degree of saturation
175 and temperature on soil thermal properties. Pinel et al. (2011) highlighted the effect of water
176 diffusion or time/space variation of humidity on the performance of buried heat sources. They
177 suggested that to account for the heat convection due to moisture transfer in the soil, a
178 comprehensive model including both heat and mass transfer processes is required. What
179 previous research demonstrates is that any experimental or theoretical study of SBTES systems
180 behavior should involve both heat and mass transfer as well as non-isothermal conditions. In

181 addition, the soil thermal and hydraulic properties should be defined as a function of
182 environmental conditions.

183 One important property that needs to properly understand soil thermal performance is
184 thermal conductivity which is subject to change in both space and time. Most models of SBTES
185 assume that the thermal conductivity is constant although it is well known that it varies
186 significantly with changes in saturation, temperature, soil density, grain size, porosity (η),
187 mineral content, organic content, soil structure, and soil texture (e.g., Yadav and Saxena, 1977;
188 Abu-Hamdeh, 2003). Several models have been proposed to estimate the thermal
189 conductivity/soil degree of saturation relationship based on easily measurable soil parameters
190 (e.g., de Vries, 1963; Johansen, 1975; Campbell, 1985; Campbell et al., 1994; Tarnawski et al.,
191 2000), very few consider the influence of changes in temperature. Campbell et al. (1994) as well
192 as Tarnawski et al. (2000) proposed models to predict thermal conductivity of soil as a function
193 of temperature, soil moisture and composition of the porous media based on de Vries model
194 (1957) and Johansen (1975) models, respectively. Overall, these studies highlight the need for
195 considering the effect of temperature and soil moisture variability on soil thermal properties
196 applicable to design and implement more efficient SBTES systems. Furthermore, as mentioned
197 by She and Sleep (1998), the knowledge of temperature effect on capillary pressure-saturation
198 relationship for multiphase fluid systems under non-isothermal conditions is necessary.

199 Based on the aforementioned studies, it is notable that although the assumption of
200 constant ground hydraulic and thermal properties is valid for many cases (e.g. when completely
201 dry or saturated conditions exist in the soil.), there is no clear definition of situations in which the
202 effect of mass transfer in efficiency of seasonal heat storage systems can be neglected (Pinel et
203 al., 2011). Most of previous studies were performed without consideration of high temperature
204 gradients which is of critical importance for implementing SBTES systems (Reuss et al., 1997).
205 Generally, the validation behind the physics governing the coupling of multiphase flow and heat
206 transfer has not been implemented in both design and operation of SBTES systems to date.
207 Consequently, developing new modeling techniques along with suitable experimental tools to
208 add more complexity in defining the physics of the heat and mass transport has critical
209 importance in obtaining necessary knowledge in efficient design and implementation of SBTES
210 systems.

211 The goal of this paper is to better understand heat and mass transfer processes for SBTES
212 systems installed in the vadose zone. We modified a fully coupled numerical model previously
213 developed by Smits et al. (2011, 2012) that solves for heat, liquid water and water vapor flux and
214 allows for non-equilibrium liquid/gas phase change. We then used this model to investigate the
215 influence of different hydraulic and thermal parameterizations on system behavior as well as
216 further examine the importance of considering convection and conduction in heat transfer for
217 SBTES modeling efforts. To better understand the physical processes and test the numerical
218 model formulation, we performed a series of two dimensional experiments. A two-dimensional,
219 heated tank apparatus was designed, constructed and implemented with a series of sensors to
220 monitor changes in temperature, volumetric water content and soil thermal properties. Four
221 experiments were performed with different sands with varying grain size. The numerical model
222 along with experimental results were used to test system behavior, perform a series of sensitivity
223 analysis, and determine the importance of including/excluding certain processes from SBTES
224 modeling efforts. Numerical modeling is aimed at better understanding of the physical processes
225 within the system and illustrating any discrepancies between experimental and numerical results.
226 The validated numerical model can also be used to simulate behavior of different soil types
227 without conducting experiments. Although experimental test cases provide insight to coupled
228 heat and moisture transfer, it is not possible to draw general conclusions with limited number of
229 tests. Accordingly, validated numerical models are a good tool to investigate the effect of
230 different parameters and processes on SBTES system efficiency.

231 **2 Material and methods**

232 In this section, a detailed review of the experiment apparatus and procedures along with a
233 description of sand materials is presented. A review of governing equations of numerical model
234 for the heat, liquid and water vapor transport is also provided.

235 **2.1 Sand Material**

236 Three types of uniform specialty silica sands (from Unimin Corp., Ottawa, MN) were
237 used during experimentation. Identified by the effective sieve number, these include #12/20,
238 #30/40, and #50/70 and a mixture of #12/20 and #50/70 sands. The mixing fraction for the 12/20
239 mixture was 70% 12/20 and 30% 50/70, herein referred to as C7F3. This mixing fraction was
240 selected to ensure that the minimum porosity (i.e. maximum density) of the mixture was
241 achieved; a minimum porosity can be achieved for mixtures containing 30% by volume of fine

242 particles (i.e., C: F ratio of 7:3) as demonstrated by Koltermann and Gorelick (1995), and Sakaki
243 and Smits 2014. The geotechnical and hydraulic properties of the different soils are presented in
244 Table 1. The properties for Bonny silt is also included in the table, as the properties for this soil
245 are used in the validated numerical model to evaluate the role of a soil having a wider grain size
246 distribution and different water retention characteristics. All three sands have different mean
247 diameter sizes but have similar porosities. The uniformity coefficient for the sands is
248 approximately 1.2, the grain density is 2650 kg.m⁻³, the grain shape is rounded, and the
249 dominating mineral composition is quartz (99.8%) (Accusands, Unimin Corps., Ottawa).

250 [Table 1 here]

251 The thermal conductivity-degree of saturation relationships and drainage-path water
252 retention curves (WRC) measured at room temperature for the four sands are shown in Figure 1.
253 These results were obtained using a modified Tempe cell that allowed continuous monitoring of
254 water content, capillary pressure, temperature, and soil thermal properties. Details of
255 experimental apparatus and procedures can be found in Smits et al. (2010, 2013). As seen from
256 this figure, the apparent λ increases with decreasing degree of saturation. #12/20 and #30/40
257 sands have similar trends while λ values for the sand mixture (C7F3) are considerably higher
258 than for the other uniform sands. In the sand mixture, the fine particles fill the void spaces
259 between the coarse particles, increasing the contact between sand particles and in the case of the
260 C7F3, decreasing the porosity. As a result, the overall thermal conductivity of the mixture
261 increases. The shape of the WRC depends on the particle size distribution (or pore space
262 distribution). For uniform sands, since the pore spaces are uniformly distributed, they drain
263 simultaneously once the displacement pressure is reached, resulting in the flat shape of WRC.
264 However, for the mixed sand case, mixing is not as ideal or uniform, and some pores are filled
265 more with the fines and other are filled less. Under such conditions, the less or unfilled pores
266 drain early but after the large pores drain, the suction continues to increase. The influence of the
267 fine soil particles controls the behavior, and the resulting WRC is steeper than that of the
268 unmixed soils.

269 [Figure 1 here]

270 2.2 Experimental Apparatus

271 Experiments were conducted using a two dimensional test tank with dimensions of 609.6
272 mm high, 609.6 m in depth, and 89 mm in width. The tank was formed from rectangular pieces
273 of 12.7 mm-thick Plexiglas. Custom-made aluminum heat plates from ABM Fabrication &
274 Machining of Arvada, CO were placed inside the tank on the left and right boundaries to serve as
275 constant temperature sources. Within the aluminum plates, a U-shape flow channel was
276 incorporated to permit flow of heated water from the heat plate's inlet port, through the flow
277 channels inside the tank, and out of the outlet port. The inlet and outlet ports were located at the
278 top of each heat plate and connected to tubing, providing constant temperature water from the
279 circulator. Schematics of the 2D tank along with the sensor locations and plumbing details are
280 shown in Figure 2.

281 At each inlet and outlet port, temperature was monitored using pipe plug thermocouples
282 (RT-1, 2 cm probe length with 0.1 °C resolution, Decagon Devices Inc.) Heated fluid was
283 supplied and pumped by a circulating bath machine with precise temperature control
284 (Polyscience model AD07R-20). A total of 22 temperature (EC-T, 38 mm probe length,
285 Decagon Devices Inc.) and 22 dielectric (ECH2O EC-5, 55-mm prong length, 70-MHz
286 measurement frequency, Decagon Devices Inc.) sensors were installed throughout the tank at the
287 locations shown in Figure 2. Prior to experimentation, all EC-5 sensors were calibrated using the
288 method developed by Sakaki et al. (2008) to account for sensor-to-sensor variability readings for
289 the analog-to-digital converter counts. Em50 (Decagon, Inc.) data loggers with five sensor ports
290 were used to read and log data. A thermal property analyzer (KD-2 Pro, Decagon Devices Inc.)
291 connected to a 30 mm SH-1 dual needle heat pulse sensor was used to monitor changes in soil
292 thermal properties 50 mm below the soil surface during the experiment. The SH-1 thermal sensor
293 is a dual needle probe, where the needles are 30 mm in length and separated by a distance of 6
294 mm. In these sensors, Heat is applied in one needle in a set heating time followed by a cooling
295 period. The temperature is measured in the monitoring needle and thermal properties of thermal
296 conductivity (λ), volumetric heat capacity (C), and diffusivity (D) are then calculated based on
297 the line heat source analysis.

298 To test the accuracy of moisture sensors, possible sources of error were considered. Air
299 gaps between sensor rods and soil can be a source of error in sensor readings (Ruelle and
300 Laurent, 2008). Air gaps can occur during installation or soil shrinkage due to drying (Hillel,
301 1998). One way to avoid these gaps is working with moist soil (Varble and Chávez, 2011).

302 Therefore, the tank was wet packed to eliminate this source of error. Furthermore, accuracy of
303 EC-5 sensors can be influenced by temperature changes in the soil. This is due to change in
304 dielectric transitivity of the bulk soil by temperature. As shown by Kizito et al. (2008),
305 temperature sensitivity of EC-5 sensors can be corrected through data processing if the
306 temperature of the soil is known in the same location. To evaluate the accuracy of temperature
307 sensitivity correction method used in this study, a set of isothermal experiments were conducted.
308 In these experiments, the moisture readings of the sensors were compared to the actual moisture
309 values of the soil sample which were experimentally measured. Based on the results, it was
310 found that temperature sensitivity up to 60°C is negligible for moisture sensors used in our
311 experimentation. Five temperature sensors were placed outside of the experimental apparatus to
312 monitor heat losses from the tank as well as ambient conditions.

313 Two constant head devices supplied by a constant water source through the use of a
314 pump were connected to valves on either side of the tank (see Figure 2) and used to supply
315 constant water head to the system. The constant head devices allowed us to maintain the water
316 table at a predetermined level throughout the course of each experiment. Top and bottom sides of
317 the tank were thermally insulated.

318 [Figure 2 here]

319 **2.3 Experimental Procedure**

320 Four experiments were performed as part of this study, as summarized in Table 1. For
321 each experiment, the sand was carefully wet-packed with deionized water in 20-mm lifts using
322 the procedure outlined by Sakaki and Illangasekare (2007). This method is used to assure that a
323 homogenous soil sample is achieved. This packing method result in greater densities by the
324 repeated tapping of the tank side walls following the procedures outlined in ASTM D 4253. An
325 advantage of using this method instead of a vibratory device is that damage to the sensitive
326 network of sensors in the 2D tank is minimized. After wet-packing the sand into the tank, the
327 constant head device was adjusted to allow the soil sample drain to a predetermined water table
328 level. Based on the air entry value of each sand type, the constant hydraulic head devices were
329 adjusted to establish a water table such that the first row of sensors from bottom of the tank was
330 located in the capillary fringe region. The purpose of this was to study the soil hydraulic and
331 thermal behavior under both saturated and unsaturated conditions. After establishing the initial

332 condition for degree of saturation distribution, the circulating heat bath machine was turned on to
333 circulate the water through the heat plates on the left and right sides of the tank at a constant
334 temperature of 60 °C. All tests were conducted for 7 days.

335 **3 Experimental results and discussion**

336 In this section, we present a demonstration of experimental results for all experiments.
337 The discussion was mostly based on data from EX-2 with comparison to other experiments (EX-
338 1, 3, and 4) where observed trends and differences between experiments are noted. It should be
339 mentioned that in this paper, moisture flow is referred to both liquid water and water vapor flow
340 in the system. The reason we show these results is to demonstrate the observed thermal and
341 hydraulic behavior of different soils.

342 **3.1 Temperature behavior in soil**

343 The temperatures of the circulating fluid at the inlet and outlet of the heat exchanger (not
344 shown here) shows that the outlet temperature reaches steady state conditions within 2 days,
345 indicating a nearly constant thermal storage capacity of the test soil. Temperature profiles for
346 sensors installed in the soil showed that a steady state condition for soil temperature was
347 established faster compared to the outlet temperature (i.e. less than 2 days). Similar behavior was
348 observed in the other three experiments.

349 Profiles of temperature in the soil for EX-2 at steady state conditions are shown in Figure
350 3(a). Because of symmetry, the results from only half of the sensors are shown. The closer the
351 sensor is located to the heat plate at the edge of the container, the higher the observed
352 temperature. The thermal gradient dissipates towards the centerline of the tank, resulting in a
353 concavity of the temperature profile and decrease in soil temperature. This, in part, is due to heat
354 loss out the sides of the tank as well as heat loss due to the energy required to change liquid
355 water to water vapor, i.e., evaporation (discussed later). Temperature trends throughout the depth
356 of the tank can also be inferred from the figure; the temperature increases with depth in the tank.
357 This can be explained by the relationship between λ and S. The bottom row of sensors is located
358 in the saturated region ($S \approx 1$) while the degree of saturation decreases with height above the
359 saturated region. Typically, as degree of saturation increases, the apparent thermal conductivity
360 also increases according to the relationships shown in Figure 1. Partially wet soil can be
361 considered as a composite mixture of water, air and soil grains (quartz mineral for the sands
362 under investigation). Thermal conductivity of water, dry air, and quartz mineral are typically

363 0.58 (at 20°C), 0.024 (at 20°C), and 6.15-11.3 W.m⁻¹K⁻¹ (Bristow 2002), respectively.
364 Therefore, the λ of partially wet soil as a mixture is a function of water and air content. The
365 results suggest that availability of moisture and distance from the heat source are two important
366 factors, contributing to the temperature variation in the soil. Figure 3(b) also shows the
367 temperature variation with time in sensors located along transects A and B. As shown in the
368 figure, steady state temperature is reached after about 1 day.

369 Similar to the results from EX-2 shown in Figure 3(b), the temperatures for EX1, 3 and 4
370 also reached steady state condition in approximately less than 2 days (not shown here). Trends
371 for temperature change throughout the soil profile as well as with distance from the heat plates
372 were consistent for all experiments. Nonetheless, the observed steady state values of temperature
373 were different for each soil type, although the temperature of the inlet fluid was maintained equal
374 to 60°C. It is difficult to compare the temperature distribution in all experiments since the
375 ambient condition was slightly different for each experiment specifically in EX-2. However, it is
376 obvious from the data that a higher temperature for EX4 was observed throughout the soil tank.
377 The increase in temperature for EX4 compared to that of other three experiments is most notably
378 due to differences in soil porosity which can play an important role in thermal conduction
379 through increasing direct inter-particle contact. The C7F3 soil type has a lower porosity
380 compared to the other soils ($\phi = 0.245$ to 0.318, 0.317 and 0.327) resulting in more soil grain
381 contacts and hence a higher thermal conductivity for all saturation conditions. It should be
382 mentioned that it is quite impossible to quantify the contribution of different heat transfer
383 processes (i.e., conduction, convection and latent heat) for current experiment using the
384 experimental data. Final steady state temperature distributions for all the experiments represent a
385 non-linear trend (not shown here) similar to Figure 3(a). This non-linear behavior is in general
386 agreement with previous studies (e.g. Cassel et al., 1969). One possible reason for this behavior
387 can be the heat loss through the surface of the tank.

388 [Figure 3 here]

389 3.2 Saturation behavior

390 Experimental measurements of the degree of saturation as a function of time for EX-2 on
391 two vertical transects (Transects A and B in Figure 2) are plotted in Figure 4. In general, the
392 degree of saturation appears to exhibit more dynamic behavior compared to the temperature data

393 shown in Figure 3(b). A drying effect can be easily seen in the data shown in Figure 4 at the
394 locations of the sensors located close to the heat plate (transect B or sensor locations 1, 8, and
395 15). Along transect B, the drying rate decreases with distance from soil surface (i.e. in the
396 saturated region where moisture availability increases). Dependency of the moisture distribution
397 pattern on initial water conditions is highlighted in Bear et al. (1991). They showed that the
398 distribution in volumetric water content in unsaturated soils subject to high heat gradients is
399 dependent on the initial conditions. They mentioned that for each soil type, there is a critical
400 value for initial degree of saturation, such that for the initial degree of saturations below this
401 value, a significant drying will occur in the vicinity of hot boundaries. It can be theoretically
402 shown that for sufficient water contents, the liquid water and water vapor transfer processes in
403 presence of thermal and hydraulic head gradients in the system are less likely to reach
404 equilibrium and consequently a continuous circulation of the moisture is expected (Gurr et al.,
405 1952). However, in this experiment, the initial water content is not high enough to establish a
406 continuous moisture circulation and therefore, a steady state moisture distribution pattern was
407 established as seen in the nearly constant drying front close to the heat plates (Transect B).

408 [Figure 4 here]

409 Based on the theory of coupled heat and mass transfer, it is expected that the liquid water
410 would move from bottom part of the tank (lower capillary pressure) towards the soil surface
411 (higher capillary pressure) due to suction and from top to bottom due to gravity. It would also
412 move from middle parts of the tank towards the heat plates in horizontal direction. Moreover, it
413 is expected that water vapor would transfer from the soil closer to the heat plates to the middle of
414 the tank. The vapor transfer could also occur from the bottom part of the tank toward soil surface
415 since the temperature increases as distance from soil surface increases. In the experiments, a
416 drying effect was observed on both sides of the container, and the degree of saturation increased
417 in the middle of the tank. The results for the changes in degree of saturation along transect A
418 provide experimental evidence for thermally induced flow in the system. An increasing trend in
419 degree of saturation over time for the middle and top sensor (sensor #11 and #4) is an indication
420 of moisture flow towards middle region of the tank. The combined effect of abovementioned
421 transfer processes shows that a greater amount of moisture flow occurs most likely due to vapor

422 transfer in both directions than liquid water transfer which is later confirmed by modeling results
423 (see section 5.2).

424 The rate of moisture flow decreases closer to the soil surface, as reflected in the slightly
425 steeper change in sensor #11 readings compared to sensor #4 throughout the experiment. The
426 bottom sensor (sensor #18) along transect A shows a decreasing trend in the degree of saturation.
427 Since the tank is connected to the constant head devices at the sides of the container, the
428 moisture loss due to thermally induced flow should be compensated with water supplied by the
429 constant head devices. Nevertheless, the rates of water loss and supply are not equal, potentially
430 due to poor hydraulic connection in fine-grained soils such as #30/40 or #50/70 which led to
431 have a decreasing trend of moisture profile in vicinity of sensor #18. This trend for sensor #18 is
432 not seen in EX-1 (coarser #12/20 sand) where the hydraulic connection was better established.

433 An increase in the degree of saturation along transect A occurred in all of the experiments
434 (not shown here). However, the rate of increase is different in each experiment due to the
435 different hydraulic and thermal properties of the sands. In EX-1 and EX-2 in which relatively
436 coarse-grained soils were used in the test tank, the rate of increase in the degree of saturation is
437 similar. The lowest increase in degree of saturation was observed in EX-3 in which a uniform,
438 fine sand was used. The greatest increase in the degree of saturation occurred in EX-4, which
439 included a mixed sand. This is in part due to higher thermal gradients which results in higher
440 moisture flow in the system as will be further discussed in section 5.4. This may indicate that
441 mixed sand provides better conditions for moisture flow. Degree of saturation at the locations of
442 sensors 7 and 14 along with the heat plate and visual observations of the drying front propagation
443 reveal that a drying front was less prominent in EX-3 and EX-4 than in the EX-1 and EX-2,
444 which involved coarse-grained soils. This observation is in agreement with the findings of Bear
445 et al. (1991).

446 **3.3 Thermal properties**

447 In-situ measurements of thermal properties of soil permit comparison between the results
448 from the experiments with the λ -S-T relationship to that of separate Tempe cell experiments
449 using the same soils and packing conditions (Smits et al., 2010, 2013). In addition, in-situ
450 measurements allowed us to experimentally capture the effects of coupled mass and heat transfer
451 on thermal properties. The SH-1 sensor location was selected to allow for variation in degree of
452 saturation and temperature over time.

453 Time series of the measured values of λ and α are shown in Figure 5, along with the
454 values of temperature and degree of saturation in the vicinity of SH-1 sensor. After an initial

455 decrease which is possibly due to a small amount of drainage of the system in initial stages of the
456 experiment, λ and α both increased over the course of the experiment. This behavior is mainly
457 due to the increase in degree of saturation at the same location. Although temperature also
458 increased at the location over time, the rise in temperature had a minimal effect on the increase in
459 soil thermal properties.

460 Previous studies demonstrated that an increase in S results in an increase in λ and α (e.g.,
461 Smits et al., 2013). In addition, λ and α increase with an increase in temperature, mainly due to
462 the transfer of latent heat in soil, thus increasing the apparent thermal conductivity (e.g. Philip
463 and de Vries, 1957; Momose and Kasubuchi, 2002; Smits et al., 2013). According to the
464 experimental studies by Smits et al. (2013) on the same #30/40 sand, at intermediate saturations
465 ($\sim 0.1-0.6$), λ and α increase at temperatures above 50 °C, with the maximum enhancement near
466 the residual degree of saturation for each sand ($S = 9\%$). For high and near-zero degree of
467 saturation, such enhancement was insignificant. At temperatures below 50 °C, Smits et al. (2013)
468 found that there was not a measurable difference in λ with changes in temperature. For the
469 experiment presented here, S values at the SH-1 sensor location varied between 7-11% while the
470 temperature varied between 20-30 °C, far too low values of temperature to have a measurable
471 effect on the thermal properties. Therefore, it seems that the effect of temperature on λ is not
472 considerable in the experimental conditions discussed here. On the other hand, as illustrated in
473 Figure 5(b), the increasing trend for moisture in the vicinity of SH-1 sensor (both #3 and #4
474 sensors) seems to be the main cause of thermal conductivity enhancement over time. Comparing
475 values of λ and $\alpha-S$ with those obtained in separate Tempe cell experiments conducted by Smits
476 et al. (2013) show that the values match very well. This verification was needed to properly
477 select the thermal property relationships for the numerical modeling (e.g. Campbell et al.
478 relationship and parameters). The value of α shows similar behavior to λ , which implies that the
479 volumetric heat capacity is not changing during the test because it is related to the thermal
480 diffusivity as $\alpha = \lambda / C$. Specifically, a nearly constant value of volumetric heat capacity of about
481 1.8 MJ.m⁻³.K was observed throughout the experiment.

482 The thermal properties of test soils at a single location (same as EX-2) with time were
483 measured for all experiments (not shown here). The results for thermal properties and
484 temperature change are similar in all of the experiments to those shown in detail for EX-2.
485 Therefore, it appears that increase in degree of saturation is the main reason for enhancement of

486 thermal properties for other experiments as well whereas temperature has minimal effect. In EX-
 487 4 with the mixed soil type, thermal conductivity and diffusivity are considerably higher than
 488 other soil types which are due to lower porosity and higher particle contacts. Although the rate of
 489 change is different for each experiment, an overall increasing trend was observed. Results also
 490 show similar trends for the thermal diffusivity as a function of time for all experiments at the
 491 same location. The similar trends for thermal conductivity and thermal diffusivity are due to
 492 nearly constant volumetric heat capacity observed for all experiments.

493 [Figure 5 here]

494 **4 Numerical Model Formulations**

495 The model used in this study is a modified version of the model described by Smits et al.
 496 (2011, 2012) which solves for heat, liquid water and water vapor flux and allows for non-
 497 equilibrium liquid/gas phase change. A detailed description of the model can be found in Smits
 498 et al. (2011); however, governing equations for mass and energy transport mechanisms as well as
 499 phase change are presented here.

500 **4.1 Mass transport in porous medium**

501 Darcy's law is used to model the non-isothermal, non-equilibrium, two phase flow in
 502 porous medium. In this regard, two different equations are defined for both the liquid and gas
 503 phases. The total gas phase is assumed to be ideal and a binary mixture of water vapor and air.
 504 These two equations are related by capillary pressure to form the following coupled differential
 505 equations (Bear, 1972):

$$506 \quad \emptyset \frac{dS_w}{dP_c} \frac{\partial \rho_w P_c}{\partial t} + \nabla \cdot \left(\frac{-\rho_w k_{rw} k_{int}}{\mu_w} (\nabla P_w + \rho_w g) \right) = -f_{vw} \quad (1)$$

$$507 \quad \emptyset \frac{dS_a}{dP_c} \frac{\partial \rho_a P_c}{\partial t} + \nabla \cdot \left(\frac{-\rho_a k_{ra} k_{int}}{\mu_a} (\nabla P_g + \rho_a g) \right) = f_{vw} \quad (2)$$

508 Where \emptyset is the total porosity of soil, S_w and S_a are water and air degree of saturation
 509 (dimensionless), ρ_w ($\text{kg} \cdot \text{m}^{-3}$), μ_w ($\text{Pa} \cdot \text{s}$), ρ_a , μ_a are the density and dynamic viscosity of water
 510 and air respectively, P_c (Pa) is the capillary pressure in porous medium ($P_c = P_g - P_w$), k_{int} is the
 511 intrinsic permeability of soil (m^2), k_{rw} (dimensionless) and k_{ra} are the relative permeability of
 water and air respectively, g is the gravitational acceleration ($\text{m}^2 \cdot \text{s}^{-1}$) and f_{vw} ($\text{kg} \cdot \text{m}^{-3} \cdot \text{s}^{-1}$) is the
 non-equilibrium phase change rate between water and its vapor which is a result of evaporation

512 or condensation in the system. To calculate the unknown water and gas phase pressure (P_w, P_g),
513 equations (1) and (2) are solved simultaneously. The model of van Genuchten (1980) is used to
514 describe the WRC in this study and the relative permeability values for water and gas (k_{rw} and
515 k_{ra}) were obtained by utilizing the van Genuchten-Mualem model (van Genuchten, 1980). Since
516 the temperature considerably changes in the system, the P_c - S_w relationship requires modifications
517 to account for the effect of temperature changes. Changes in the temperature can cause
518 fluctuations in the surface tension (Assouline, 2006). Therefore, the P_c - S_w relationship measured
519 in the room temperature can be modified by substituting the relationship $P_c(T) = P_c(T_{ref})\sigma(T)/$
520 $\sigma(T_{ref})$ in the P_c - S_w relationship where T_{ref} is the reference temperature at which the original P_c -
521 S_w relationship was measured. Previous studies have shown that classical models for WRC as
522 the van Genuchten model commonly fails to describe the WRC well enough at low water
523 contents (e.g., Ross et al., 1991). This inaccuracy can be even amplified at higher temperatures
524 when water content is less than residual water content. Based on the work of She and Sleep
525 (1998), the residual water content is assumed to change linearly as a function of temperature, as
526 follows:

$$\theta_r(T) = \theta_r(293 \text{ K})[1 - c(T - 293 \text{ K})] \quad (3)$$

527 where c is a fitting parameter (She and Sleep, 1998).

528 **4.2 Phase change under non-equilibrium conditions**

529 In traditional liquid-gas phase change models, phase change between the liquid and vapor
530 phases is often evaluated based on the assumption of equilibrium; evaporation or condensation
531 behavior is often considered as an instantaneous process (e.g. Philips and de Vries, 1957; Bear et
532 al., 1991). In modeling efforts based on the equilibrium assumption, the equilibrium vapor
533 density is determined by Kelvin's equation. Kelvin's equation can describe the equilibrium
534 condition between the relative humidity and capillary pressure in pore space (e.g., Lu and Likos,
535 2004):

$$\ln\left(\frac{\rho_{veq}}{\rho_{vs}}\right) = \frac{P_c V_m}{RT} \quad (4)$$

536 where ρ_{vs} ($\text{kg} \cdot \text{m}^{-3}$) is the saturated vapor density, V_m is the molar volume of water (M_w / ρ_w), R
537 is the universal gas constant ($\text{J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$) and T (K) is the temperature. Using Kelvin's
538 equation, one can readily find the relationship between vapor densities for both equilibrium and

539 saturated conditions. The saturated vapor density changes with temperature and can be estimated
 540 using the empirical relationship of Campbell (1985), given as follows:

$$\rho_{vs} = \exp(31.37 - 6014.79T^{-1} - 7.92 \times 10^{-3}T) / T \times 10^{-3} \quad (5)$$

541 Therefore, the equilibrium vapor density can be calculated by rearranging (4) and incorporating
 542 the value of ρ_{vs} from Equation 5:

$$\rho_{veq} = \rho_{vs} \exp\left(\frac{P_c V_m}{RT}\right) \quad (6)$$

543 In several studies, the assumption of equilibrium phase change is called into question
 544 (e.g., Bénet et al., 2009). The study carried out by Bénet et al. (2009) showed that the
 545 characteristic time associated with thermal equilibrium is much lower than the characteristic time
 546 associated with mass transfer. In a macroscopic model for liquid-gas phase change in
 547 hygroscopic porous media such as soil, phase change velocity is considerably influenced by
 548 hygroscopic effects of porous media (Cherblane et al., 2007). Since limited experimental data are
 549 available on the soil types that were used in our work, a method based on the difference between
 550 the vapor pressure in air and the equilibrium pressure at the water-gas interface was used (Zhang
 551 and Datta, 2004). In this approach the phase change rate is defined as:

$$f_{vw} = \frac{b(\theta_w - \theta_r)RT}{M_w} (\rho_{veq} - \rho_v) \quad (7)$$

552 where ρ_v ($\text{kg} \cdot \text{m}^{-3}$) is the vapor density and b is defined as a fitting parameter that is assumed to
 553 be a function of soil properties. The value of b was fitted using experimental data obtained in this
 554 study for each soil type.

555 **4.3 Heat transfer in porous medium**

556 Conduction, convection and later heat transfer due to phase change are considered as
 557 three main heat transfer mechanisms in soil. We assumed local thermal equilibrium between the
 558 gas, liquid and solid phases. By taking averages at the scale of a representative elementary
 559 volume (REV), the energy equation can be applied for each phase separately. Under the
 560 assumption of local thermal equilibrium, energy equations for each phase are then combined to
 561 yield a general form of heat transfer equation for porous media, given as follows:

$$(\rho c_p)^* \frac{\partial T}{\partial t} + \nabla \cdot ((\rho c_p)_w u_w T) + (\rho c_p)_g u_g T) - \nabla \cdot (\lambda_t \nabla T) = -L f_{vw} - Q_s \quad (8)$$

562 where c_p ($\text{J} \cdot \text{kg}^{-1} \cdot \text{K}^{-1}$) is the heat capacity for the phase, u_w (ms^{-1}) and u_g are the liquid and gas
 563 velocities respectively, $L f_{vw}$ is the latent heat due to phase change, λ_t is the apparent thermal

564 conductivity ($W \cdot m^{-1}K^{-1}$) and $Q_s(J \cdot m^{-3} \cdot s^{-1})$ is the heat loss from the system. The value of Q_s
565 can be estimated by incorporating Newton's law of cooling. The heat loss coefficient was
566 defined based on knowledge of the thermal properties of the soil tank and surrounding air and the
567 difference between the ambient room temperature and temperature of the soil tank (i.e.,
568 Plexiglas). The term $(\rho c_p)^*$ represents the effective heat capacity for all three phases and can be
569 described by assuming that surface porosity is equal to the total porosity of porous media:

$$(\rho c_p)^* = (1 - \phi)(\rho c_p)_s + \phi(\rho c_p)_w + \phi(\rho c_p)_g \quad (9)$$

570 The thermal conductivity model of Campbell et al. (1994) was used in this study to
571 estimate the apparent thermal conductivity (λ_t) as it considers the effect of changes in
572 temperature and degree of saturation on the thermal conductivity of the soil and has shown to be
573 effective compared to other models. In this model, the thermal conductivity of a mixture is
574 considered as a weighted sum of thermal conductivities of components. Furthermore, since the
575 system operating temperature is relatively high in the experiments, the physical properties of the
576 different phases can be affected by temperature. In order to take these effects into account, the
577 density and viscosity of water and air are treated as functions of the system temperature at each
578 point.

579 **5 Numerical simulation and comparison with experimental results**

580 In this section, numerical model results are compared to experimental results to better
581 understand any discrepancies between theory and experiments and the validity of the proposed
582 model. First, to validate the proposed two-dimensional, non-isothermal, non-equilibrium model,
583 numerical results for temperature and degree of saturation are compared with experimental
584 results from EX1-4. Secondly, the numerical model correspond to EX-2 was considered to
585 discuss effective processes and finally to perform several parametric studies in following
586 sections.

587 The boundary conditions applied for mass and energy transfer are depicted in Figure 6.
588 As seen from Figure 6(a), for liquid water and water vapor flow, Neumann boundary conditions
589 (no mass flux) were assumed for all boundaries. Figure 6(b) presents applied boundary
590 conditions for heat transfer in porous media. The Neumann boundary conditions were used in top
591 and bottom insulated boundaries. However, for right and left boundaries, since constant
592 temperature was applied, Dirichlet boundary conditions were chosen. Initial ambient temperature
593 was considered as an initial temperature for the entire domain which was slightly different for

594 each experiment. To establish the initial conditions of soil saturation, as mentioned earlier,
595 constant hydraulic devices were used to create variable degree of saturation conditions
596 throughout the domain.

597 To develop the numerical model, the porous media properties, initial and boundary
598 conditions of the experimental case were implemented. The system of differential equations was
599 then solved using the COMSOL Multiphysics software package. The domain was discretized by
600 using 8909 triangular elements. Smaller boundary elements were used in the boundaries with
601 constant temperature (heat plates) and bottom valves (connection to the constant hydraulic
602 devices) as well.

603 [Figure 6 here]

604 **5.1 Model verification with experimental results**

605 Figure 7 shows the simulated vertical profiles of both temperature and degree of
606 saturation compared with experimental data along transect A and B (see Figure 2) at times t=0
607 and 7 days. Although the numerical model captures the trends in the experimental data well,
608 some discrepancies exist between experimental and numerical results which are statistically
609 confirmed with the R^2 values (ranging from 0.660 to 0.907). Deviations between simulated and
610 measured degrees of saturation and temperatures may, in part, be due the accuracy and resolution
611 of the Dielectric sensors and thermistors compared to the model. The EC-5 soil moisture sensor,
612 for example, has a sampling volume (i.e. the volume of soil around the sensor, within which a
613 change in degree of saturation affects the sensor readings) of 18 cm^3 (Sakaki et al., 2008) while
614 the numerical model predicts a degree of saturation value at an exact point, rather than a volume
615 average. For the transect located close to the heat plate (transect B), the predicted and measured
616 residual degree of saturation at t=7days did not agree well. The observed degrees of saturation
617 at the location of sensors #1 and #15 were lower than the model predicted, demonstrating that the
618 tank dried faster than the model predicted for these times. As discussed in the theory section, the
619 effect of temperature on the WRC properties were accounted for using the She and Sleep (1998)
620 modification of the van Genuchten model; this model could not capture the drying behavior for
621 transect B where the temperature values were above $35 \text{ }^\circ\text{C}$. Poor estimation of residual water
622 content at the location of sensors #1 and #15 at t=7days could also be in part due to changes in
623 soil water retention properties with changes in bulk density within the soil column (Assouline,

624 2006) as will be discussed later in section 5.5 as the constitutive relationship selected for the
625 WRC.

626 A comparison between predicted and measured temperatures at different locations within
627 the test tank along transects A and B is shown in Figures 7(c) and 7(d). Although the observed
628 and modeled temperatures disagreed, the model captured the general trend (R^2 values ranging
629 from 0.660 to 0.907). The deviations between simulated and measured temperatures may be, due
630 to the accuracy and resolution of the temperature sensors compared to the model. The shape of
631 the temperature profile is associated with the nonlinear distribution of the thermal properties
632 associated with water redistribution in response to temperature gradients (Prunty and Horton,
633 1994), heat loss out of the sides of the soil tank, and differences in the degree of saturation
634 through the depth of the tank. The heat loss was accounted for in the model based on knowledge
635 of the temperature distribution out of the tank and thermal properties of the Plexiglas tank
636 material. The additional heat loss due to the latent heat of evaporation was also taken into
637 account in the model by the transfer of latent heat as a result of liquid water-water vapor phase
638 change. The latent heat transfer is responsible for the S-shape curve (blue line) by maximizing
639 the heat transfer close to the heat plates above the saturated zone. Errors associated with
640 prediction of numerical models for temperature and degree of saturation distribution under non-
641 isothermal conditions as opposed to isothermal conditions was also reported by Bach (1992).
642 Bach (1992) showed that adjusting the temperature coefficient of the matric potential resulted in
643 better agreement between measured and predicted values. Thus, a closer fit might be obtained by
644 implementing more realistic relationships of effective parameters in WRC. Possible sources of
645 error in both experimental data and modeling process will be further addressed in future studies.

646 [Figure 7 here]

647 To better understand the water vapor and liquid water movement throughout the domain
648 over time, a comparison was made between the initial and final degree of saturation distribution
649 in the domain. The simulated distribution of degree of saturation within the domain at the end of
650 the experiment ($t=7$ days) is shown in Figure 8(b). The gradient plot depicts the liquid water
651 distribution while the arrows represent the water vapor flow. As expected, saturation decreased
652 in the vicinity of the heat plates and a dry region developed at both sides of the tank, adjacent to
653 the heat plates, which is in agreement with experimental observations discussed in previous

654 sections. Water vapor flow is observed to flow from the sides of the tank toward the centerline,
655 as expected. To investigate the degree of saturation and temperature trends in the middle of the
656 tank, three points were considered, and the degree of saturation and temperature at these points
657 as a function of time are plotted in Figure 8(c) and (d). It should be mentioned that the
658 fluctuations in the temperature and degree of saturation plots are caused by ambient air
659 fluctuations which were implemented as an input function to the model to account for heat loss.
660 Consistent with the experimental results, the simulated degree of saturation profiles show a slight
661 increase in both temperature and degree of saturation at all three points, demonstrating that the
662 model captures the increasing degree of saturation trends well. Nonetheless, comparison of the
663 trends in the degree of saturation values from the experiment and simulation indicate that
664 although model captured the trends well, it underestimated the increasing rates.

665 The increase in degree of saturation in the middle regions of the tank as well as the trends
666 in the velocity field for gas phase (shown by the arrows in Figure 8(b)) demonstrate the
667 contribution of thermally induced vapor flow to the overall saturation movement as will be
668 further discussed in section 5.4. The water vapor movement is highest close to the heat plates and
669 decreases with distance from the centerline. This is because the water evaporates from the
670 regions close to the heat plates and condenses as it reaches the relatively colder regions towards
671 the centerline of the domain. This then results in an increase in soil degree of saturation toward
672 the centerline of the tank (hence the increase in degree of saturation for points 1-3). It is
673 important to note that although liquid water flow also contributes to overall moisture flow in the
674 domain; its magnitude is smaller compared to vapor flow which is in part due to smaller
675 percentage of saturated soil. Although degree of saturation increases in all three points, the rates
676 of increase are different. For point #1 which is closer to the saturated soil, the increase rate (slope
677 of gray trend-line) is slightly smaller compared to point #2 located above point #1 (hence a lower
678 degree of saturation). This could, in part, be due to better connectivity of air-filled pores in dryer
679 soil (point #2) which provides a better medium for vapor to flow. Since the water vapor transfers
680 from both sides toward centerline, the rate of degree of saturation increase for both points #1 and
681 #2 are larger than point #3.

682 The temperature trends for points 1-3 are shown in Figure 8(d). Consistent with
683 experimental results, since point #3 is closer to the heat plate; the temperature was higher
684 compared to points #1 and #2. In addition, point #1 has a higher temperature than point #2; this

685 is due, in part, to the difference in degree of saturation and consequently differences in thermal
686 properties (e.g. apparent thermal conductivities). For instance, the higher degree of saturation at
687 point #1 than point #2, resulted in a higher thermal conductivity, thus a higher temperature was
688 reached. As seen in the Figure 8(d), after an initial sharp increase in temperature, temperature
689 remains almost constant for all three points. Similar behavior was observed in experimental
690 results (Figure 5(b)).

691 [Figure 8 here]

692 **5.2 The importance of conductive and convective heat fluxes**

693 Surface plots of conductive and convective heat fluxes (i.e., heat transferred by liquid
694 water and water vapor flow) within the domain are shown in Figures 9(a) and 9(b), respectively.
695 The convective heat flux is considerably larger than conductive heat flux, demonstrating that the
696 liquid water and water vapor flow have more of a contribution to the overall heat flux than the
697 conductive fluxes. Cary (1965) also showed that most of the rise in net heat flux at higher
698 average temperatures was due to latent heat transfer of vaporization. Based on surface integration
699 values of the two components of the convective heat flux (i.e. liquid water and water vapor flux),
700 liquid water flow contributes less to the overall convective flux (about 10% of total convective
701 flux) as compared to the convective flux due to water vapor flow within the domain. This
702 contribution will vary of course with soil degree of saturation; the percentage of liquid water
703 flow is related to the percentage of saturated soil (around 25% of total soil volume for $t=7$ days).

704 Conductive heat flux is a function of the temperature gradient and apparent thermal
705 conductivity of the soil. Since the moisture flow within the domain alters the apparent thermal
706 conductivity, it is expected to indirectly affect the conductive heat transfer rate. The results in
707 Figure 9(a) indicate that a higher conductive flux is observed in the saturated soil than in the
708 unsaturated soil. This is partially due to the higher thermal conductivity of the saturated soil than
709 the unsaturated soil (e.g., λ_{dry} vs. λ_{sat} values).

710 It is evident from Figure 9(b) that convective heat fluxes are higher in unsaturated regions
711 close to the heat plates which are located just above saturated soil. This is likely due to the higher
712 phase change rate from liquid water to water vapor at these locations and can be explained by
713 relating the phase change rate to the degree of saturation of the soil. As discussed by Ruiz and
714 Benet (2001), at low degrees of saturation the liquid/gas interfacial area increases resulting in

715 more locations for phase change to occur and hence higher phase change rates. Close to the heat
716 plates above the saturated zone, at $t=7$ days, the soil is below the residual degree of saturation and
717 phase change can occur readily. Although the same degree of saturation conditions exist in the
718 middle of the tank and at same vertical distance, the regions with higher convective flux do not
719 extent to the middle part of the tank due to smaller evaporation rate. Since the evaporation is
720 directly related to the temperature, in colder regions in the middle of the tank the temperature is
721 not high enough to trigger evaporation. These findings clearly show that in SBTES systems
722 installed in vadose zone, depending on the initial and boundary conditions, the convective heat
723 flux can have major contribution to overall heat transfer. Therefore, it should be considered in
724 modeling and designing efforts.

725 [Figure 9 here]

726 **5.3 Effect of convective heat flux on saturation and temperature distribution**

727 The impact of convective heat flux on the temperature and degree of saturation was
728 evaluated by comparing model results with and without including convective heat flux. In the
729 case where convection was removed, conduction was the only mechanism for heat transfer. No
730 considerable change in degree of saturation is observed in Figure 10(a) when only the heat
731 transfer equation was modified. However, the impact of convective heat flux on temperature
732 shown in Figure 10(b) indicates a greater effect. A temperature difference of almost 2 °C was
733 observed in middle of the tank and the effect of convective heat flux on temperature rise
734 increases with distance towards the heat plate. The temperature difference between the cases
735 with and without convective heat flux highlights the importance of convective heat flux in
736 obtaining more realistic temperature distribution in SBTES systems.

737 [Figure 10 here]

738 **5.4 Effect of thermal and hydraulic gradients on moisture flow**

739 Temperature and total hydraulic head (i.e., suction and gravity) gradients are two main
740 driving mechanisms for coupled heat and mass flow in porous media. Thus, calculating the range
741 of variation for these gradients is necessary to draw conclusions on the effect of each individual
742 variable on heat and moisture movement. Simulated surface plots of temperature and hydraulic
743 head gradients at $t=7$ days are depicted in Figure 11(a) and (b), respectively. As seen from Figure

744 11(a), the temperature gradient is highest close to the heat plates and decreases with distance
745 towards the centerline. The decreasing trend is slightly different in the bottom region of tank
746 where the soil is mostly saturated. As illustrated in Figure 11(b), the total hydraulic head
747 gradient is considerably higher in the distinct boundary of the wetting front but it is negligible in
748 rest of the domain (about 0.15 cm H₂O/cm). Cary (1965) experimentally studied the contribution
749 of hydraulic head and thermal gradients to net moisture flow. Based on his studies with separate
750 liquid and vapor flow components as well as flow due to thermal gradient and pressure
751 difference, a temperature gradient of 0.5 °C cm⁻¹ at a soil suction of 5 cm Hg (about the total
752 hydraulic head range within wetting front in current study), caused a moisture movement as
753 much as a soil suction of 2 cm H₂O/cm. Therefore by considering the magnitude of each gradient
754 in this study, it appears that moisture flow is more influenced by thermal gradients than total
755 hydraulic head gradients. Although the moisture flow and distribution in the soil does not

756 It is important to note that the hydraulic gradients may be more important than the
757 thermal gradients at larger scales and at different initial degrees of saturation compared to this
758 experimental study. However, as far as findings of current numerical simulations reveal, the
759 thermal gradients should be taken into account to simulate moisture distribution when
760 implementing field scale SBTES systems. Thermal and hydraulic gradients are closely coupled
761 in SBTES systems; therefore it is critical to understand their relative importance for properly
762 determining SBTES system behavior.

763 [Figure 11 here]

764 **5.5 Effect of temperature correction on soil water retention**

765 As mentioned in section 4.3, the WRC can be corrected to account for effects of
766 temperature on the surface tension and residual degree of saturation (She and Sleep, 1998).
767 These corrections were applied to consider the effect of temperature on the soil water retention
768 function. To investigate the impact of these corrections on the model output, a simulation was
769 performed with and without applying the temperature corrections to the WRC; results were
770 compared to the base case scenario (EX-2) (with temperature corrections). The impact of the
771 temperature correction is observed by looking at degree of saturation and temperature as a
772 function of time in a sample point of the domain (point 2 in Figure 8(b) was selected here). As
773 depicted in Figure 12(a), the model predicted higher values for both degree of saturation and

774 temperature when no correction was applied to the WRC. For a constant capillary pressure,
775 including the effect of higher temperature will result in a lower degree of saturation. This could
776 be a main reason for the calculated degree of saturation level being lower when temperature is
777 taken into account. Furthermore, as evident from Figure 12(a) without using a temperature
778 correction for the WRC, fluctuations in ambient temperature do not affect the calculated degree
779 of saturation values, resulting in a more consistent trend. It is important to highlight that in the
780 original form of the van Genuchten model (i.e. no temperature correction); degree of saturation
781 does not drop below the residual degree of saturation value. For this reason, although not shown
782 here, the model failed to properly predict the drying behavior close to the heat plates when the
783 effect of temperature on the WRC was not considered. In most of previous SBTES modeling
784 efforts, there was no need to implement WRC in numerical models since the multiphase flow
785 within the soil was not considered. However, for the models that incorporate non-isothermal
786 multiphase flow, the proper correction for temperature in WRC should be considered.

787 [Figure 12 here]

788 **5.6 Effect of porosity and saturated hydraulic conductivity**

789 To examine the effect of porosity and hydraulic conductivity on degree of saturation and
790 temperature, two sets of simulations were performed. In both sets, porosity and hydraulic
791 conductivity values were changed by $\pm 10\%$ with respect to the base case values. Figure 13(a)
792 shows the effect of porosity on the degree of saturation trend. Figure 13(c) and (d) shows the
793 effect of saturated hydraulic conductivity on the degree of saturation and temperature
794 respectively. As seen from the figure, hydraulic conductivity does not have a measurable effect
795 on temperature and degree of saturation trends. At lower initial degree of saturations as in
796 present study, saturated hydraulic conductivity is not as influential as, for example, WRC and
797 relative permeability functions. The simulation clearly shows the importance of properly
798 assigning porosity values to get more realistic degree of saturation distribution especially in field
799 scale SBTES systems with nonhomogeneous domains (i.e., porosity can decrease with distance
800 from ground surface). Therefore, a proper approach should be applied to account for porosity
801 variability in the domain. On the other hand, in the SBTES systems installed in the vadose zone
802 with lower degrees of saturation, the hydraulic conductivity of soil would not considerably affect
803 the temperature and moisture distribution.

804

[Figure 13 here]

805 **5.7 Effect of thermal conductivity**

806 As discussed in the introduction, common practice in most previous studies related to
807 SBTES systems is to assume constant thermal properties for soil. Although this assumption can
808 be realistic in some cases, it is not accurate for modeling multiphase flow in unsaturated soil
809 under non-isothermal conditions. The impact of assigning constant values for thermal
810 conductivity in the numerical model was evaluated by running the model with two different
811 constant thermal conductivities (λ_{sat} and λ_{dry}). Figure 14 presents the results of degree of
812 saturation and temperature for each scenario as compared to the base case in which the Campbell
813 model was used to estimate λ as a function of degree of saturation. As seen from Figure 14(b),
814 higher temperatures were calculated when λ_{sat} was defined as a constant thermal conductivity
815 throughout the domain. This is due to the increase in conductive heat transfer as λ increases.
816 Inversely, λ_{dry} causes a decrease in conductive heat flux and consequently leads to lower
817 temperatures in the system. The effect of this temperature change is then reflected in the degree
818 of saturation profiles as seen in Figure 14(a). As discussed in section 5.5, the decrease in
819 temperature can alter the WRC and therefore change the calculated degree of saturation values.
820 For instance, as temperature decreases, degree of saturation increases for a constant capillary
821 pressure. This is in general agreement with the degree of saturation trends in Figure 14(a).
822 Results demonstrate the importance of properly assigning the thermal conductivity in designing
823 and implementing any SBTES systems in vadose zone as the effect of this property is much
824 larger than other thermal or hydraulic properties of the soil.

825

[Figure 14 here]

826 **5.8 Numerical results for a natural soil: Bonny silt**

827 Now that the model has been validated using experimental results, it is possible to
828 evaluate the physics of coupled heat and mass transfer in soil layers that will likely be
829 encountered in SBTES systems in the vadose zone. Accordingly, simulations with same
830 assumptions and formulations were performed using the thermal and hydraulic properties of a
831 natural soil named “Bonny Silt” (Dong et al., 2014). General properties of the soil are provided
832 in Table 1. The same geometry for soil domain was considered to simulate three cases with

833 different initial saturation conditions. In the first case, initial degree of saturation of
834 approximately 19% was considered while in the second case, the initial variable degree of
835 saturation was varied between 48% to about 51% and an almost saturated initial condition (89
836 $\% < S < 100\%$) was considered in the third case. These simulations were aimed at investigating the
837 effect of initial moisture condition on temperature and moisture transfer within the soil. The
838 variation in initial degree of saturation is due to the approach used to create initial condition. An
839 initial temperature of 21.3 °C was assumed for all simulations.

840 For all three cases, a vertical profile of initial and final values of degree of saturation and
841 temperature along transect A are illustrated in Figure 15. This figure clearly shows that
842 maximum change in degree of saturation and temperature occurs in case one ($S=19\%$), while
843 case three with higher initial degree of saturation level, exhibits minimum variation in both
844 temperature and degree of saturation. These results therefore reveal that heat and mass transfer
845 processes highly depend upon initial saturation conditions. To better illustrate the effect of
846 convective heat flux on temperature distributions, the final temperature profiles were plotted
847 with and without (green dotted line) taking the convective component of heat transfer into
848 account. Figure 15(b) shows that convective heat flux has more contribution in soil with lower
849 initial degree of saturation as opposed to higher initial degree of saturation (Figure 15(f)). As
850 illustrations of Figure 15 reveal, there is a correlation between moisture variation and convective
851 heat transfer. A comparison between temperature profiles for all three cases demonstrates that as
852 initial degree of saturation of the soil increases the effect of convective heat transfer on
853 temperature rise decreases while conduction becomes more significant. It can thus be suggested
854 that for each soil type, there might be a critical degree of saturation in which overall heat transfer
855 is maximum. Similarly as reported by Bear et al. (1991), there is also a critical degree of
856 saturation (which depends on the soil type) that causes no considerable drying at the hot
857 boundaries.

858 [Figure 15 here]

859 **6 Conclusions**

860 This paper reported a study where a two-dimensional, non-isothermal, non-equilibrium
861 model for coupled heat and mass transfer processes was developed and evaluated using
862 experimental data. The experimental and numerical results show that the hydraulic and thermal

863 processes in unsaturated soil are coupled and therefore, their effect should be simultaneously
864 analyzed in any SBTES system installed in vadose zone. Although limited, the experimental
865 results for different soil types indicate that mixed soils with minimal porosity and varying grain
866 size distribution would possibly lead to higher temperature gradients and consequently higher
867 moisture flow in the system; therefore are suitable for SBTES systems. Furthermore, constant
868 volumetric heat capacities for all studied sand types implies that non-isothermal conditions in
869 similar unsaturated conditions may lead to a rate of heat injection/extraction, but will not change
870 the overall amount of heat that can be stored.

871 For initial and boundary conditions assumed in this study, results indicate that convective
872 heat flux is considerably larger than conductive heat flux, demonstrating the importance of
873 including convective heat transfer in modeling of SBTES systems, especially in the unsaturated
874 soils when water vapor phase is present. Returning to the concerns presented at the beginning of
875 this study, it is possible to state that SBTES systems in vadose zone may have greater heat
876 transfer capabilities due to effect of convective heat fluxes.

877 Analysis of thermal and hydraulic head gradients reveal that for the soil types, boundary
878 conditions and initial conditions evaluated in this study, moisture flow (i.e., in terms of total flow
879 in liquid and vapor phases) is influenced more by thermal gradients rather than total hydraulic
880 head gradients. However this finding might not be valid for larger scales with different soil types
881 and initial moisture contents. In larger scales, hydraulic gradients will be more important
882 compared to smaller experimental scales such as current study.

883 The validated model provides a suitable tool to explore model sensitivity to different
884 inputs and assumptions, including apparent thermal conductivity, soil water retention properties
885 and porosity. It is therefore important to include more realistic equations/assumptions in defining
886 apparent thermal conductivity (e.g. the effect of degree of saturation and temperature on soil
887 thermal conductivity), the WRC (e.g., temperature effects) and porosity variation when modeling
888 SBTES systems in unsaturated soils. The sensitivity analysis of validated model showed that
889 traditional Van Genuchten model is not applicable in presence of high thermal gradient.
890 Therefore, in order to consider the coupled hydraulic and thermal processes in SBTES systems,
891 the effect of temperature should be considered in WRC. An implication of these findings is that
892 SBTES systems in the vadose zone where unsaturated conditions are present should include
893 variable thermal and hydraulic properties.

894 Numerical simulation of Bonny silt revealed that convective heat flux is not as
895 pronounced in saturated soils than unsaturated soils, which indicates that SBTES systems in
896 saturated soil will not have a change in the rate of heat injection/extraction during the
897 inject/extraction process. Nonetheless, they may still be affected by buoyancy changes due to
898 changes in temperature of the fluid. Furthermore, the simulations for Bonny silt highlight the
899 importance of initial degree of saturation on convective heat flux. In general, for any specific
900 SBTES system, there is possibly an initial degree of saturation in which convective heat transfer
901 and consequently overall heat transfer is maximized.

902 This research demonstrates the need for further experimental and theoretical study on
903 SBTES system behavior in three dimensional and field scales, the effect of boundary conditions
904 (e.g. heat source temperature, distance of constant temperature boundaries), initial moisture
905 conditions and incorporating different formulations/assumptions to define soil thermal and
906 hydraulic properties. The findings of this study also indicate that SBTES system efficiency can
907 be affected in different ways by coupled heat and mass transfer processes in the vadose zone.
908 Further research is needed to evaluate how these processes can be exploited, specifically
909 focusing on the impact of these mechanisms on the injection/extraction schemes and the long-
910 term efficiency. It is also important to note that in natural soils, solute transport effects may
911 impact the heat transfer process at hot boundaries. Drying out effect can increase the solute
912 concentration close to the hot boundaries leading to lower equilibrium vapor pressure.
913 Convective, dispersive and diffusive solute transport as well as osmotic effects can then develop
914 as a result of variation in equilibrium vapor pressure (Bear et al., 1991). Hence, more
915 experimental and theoretical investigations are required to better understand the effect of more
916 complex processes such as solute transport on coupled heat and moisture transfer in natural soil
917 under non-isothermal conditions.

918

919 **Acknowledgments**

920 This research was funded by National Science Foundation (NSF) Sustainable Energy Pathways
921 (SEP) Collaborative, Award Number CMMI-1230544. The content is solely the responsibility of
922 the authors and does not necessarily represent the official views of the National Science
923 Foundation (NSF).

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1086

1087 Table 1. Selected properties of test sands used in experiments

1088

Experiments	Sand	d ₅₀ (mm)	Porosity	Residual Volumetric Water Content (m/m)	Saturated Hydraulic Conductivity, Ks, (m s ⁻¹)	van Genuchten (1980) WRC Model Parameters	
						Alpha (kPa ⁻¹)	n
EX-1	12/20	1.040	0.318	0.017	3.76×10 ⁻³	0.00816	12.69
EX-2	30/40	0.524	0.317	0.022	1.06×10 ⁻³	0.0060	17.81
EX-3	50/70	0.27	0.327	0.075	2.90×10 ⁻⁴	0.0026	29.76
EX-4	C7F3	-	0.245	0.010	3.97×10 ⁻⁴	0.0029	6.75
	Bonny silt	0.039	0.430	0.030	1.3E-6	0.0863	1.58

1089

1090 **List of Figures**

1091 **Figure 1.** Thermal conductivity-degree of saturation and primary drainage capillary pressure- degree of
1092 saturation relationships measured at room temperature for all test soils.

1093 **Figure 2.** Schematic of the test tank apparatus used in experiments discussed here (not to scale).

1094 **Figure 3.** Steady state temperature (time = 7days) measured vertically from the middle of the soil tank
1095 toward the heat plate and (a) temperature variation with time along transects A and B for EX-2 (b).

1096 **Figure 4.** Degree of Saturation with time for sensors located along transects A and B (EX-2).

1097 **Figure 5.** Thermal properties of soil at the location of SH-1 sensor (a) in EX-2. Degree of Saturation and
1098 temperature profiles as a function of time for two adjacent sensors #4 and #3 for the same experiment (b).
1099 (M: Dielectric sensor, T: Temperature sensor)

1100 **Figure 6.** Boundary conditions for two-dimensional configuration where T is temperature, P_w is water
1101 pressure, J_c is mass flux (liquid water or water vapor) and J_T is heat flux in the domain.

1102 **Figure 7.** Simulated and observed degree of saturation and temperature profiles along transects A and B
1103 at 0 and 7 days. (a), (b) initial and final degree of saturation values and (c), (d) initial and final
1104 temperatures along transects A and B.

1105 **Figure 8.** Simulated soil degree of saturation distribution (a) at $t=0$ and (b) $t=7$ days (arrows representing
1106 velocity field) within the tank. The lower part of the tank (white portion) with almost saturated soil is
1107 excluded from Figure 8 (a), 8(b) to better illustrate the soil degree of saturation differences throughout the
1108 unsaturated region. Points 1-3 were selected corresponding to locations for three points depicted in 8(b) to
1109 better illustrate the change in (c) degree of saturation and (d) temperature with time.

1110 **Figure 9.** Surface plot of simulated conductive (a) and convective (b) heat flux. Arrows in Figure 9(b)
1111 show the velocity field for gas phase. (Units: W/m^2)

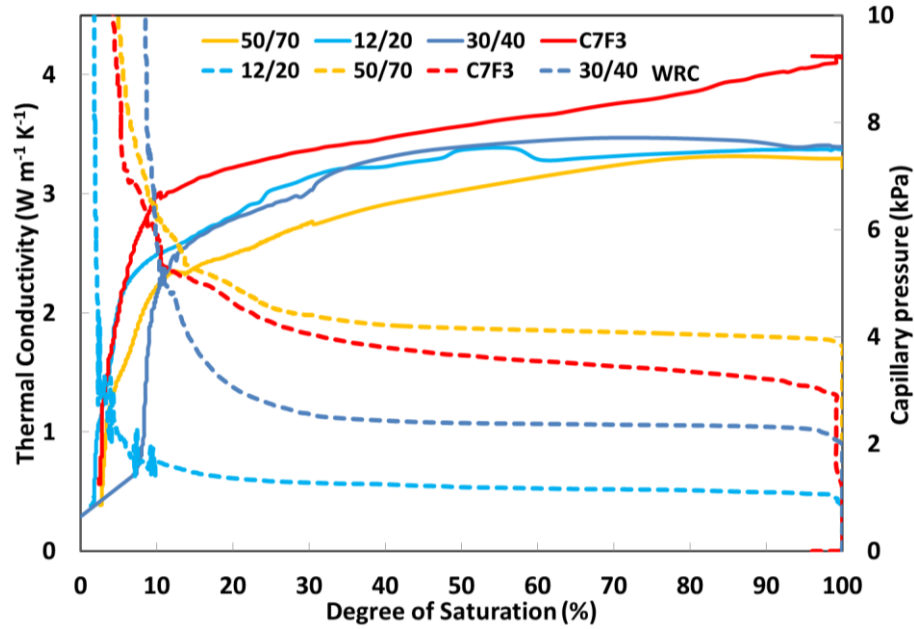
1112 **Figure 10.** Effect of convective heat flux in (a) degree of saturation (b) temperature profile with time at
1113 point #2 as shown in Figure 8(b).

1114 **Figure 11.** Simulated surface plots of (a) temperature gradient ($^{\circ}C/cm$) and (b) hydraulic head gradient
1115 ($cm H_2O/cm$) within the domain. Analysis of results demonstrates that thermal gradients have more
1116 contribution in moisture flow than total hydraulic head gradients.

1117 **Figure 12.** Effect of temperature correction of the WRC on the predicted trends at point 2 in Figure 8(b):
1118 (a) degree of saturation (b) Temperature.

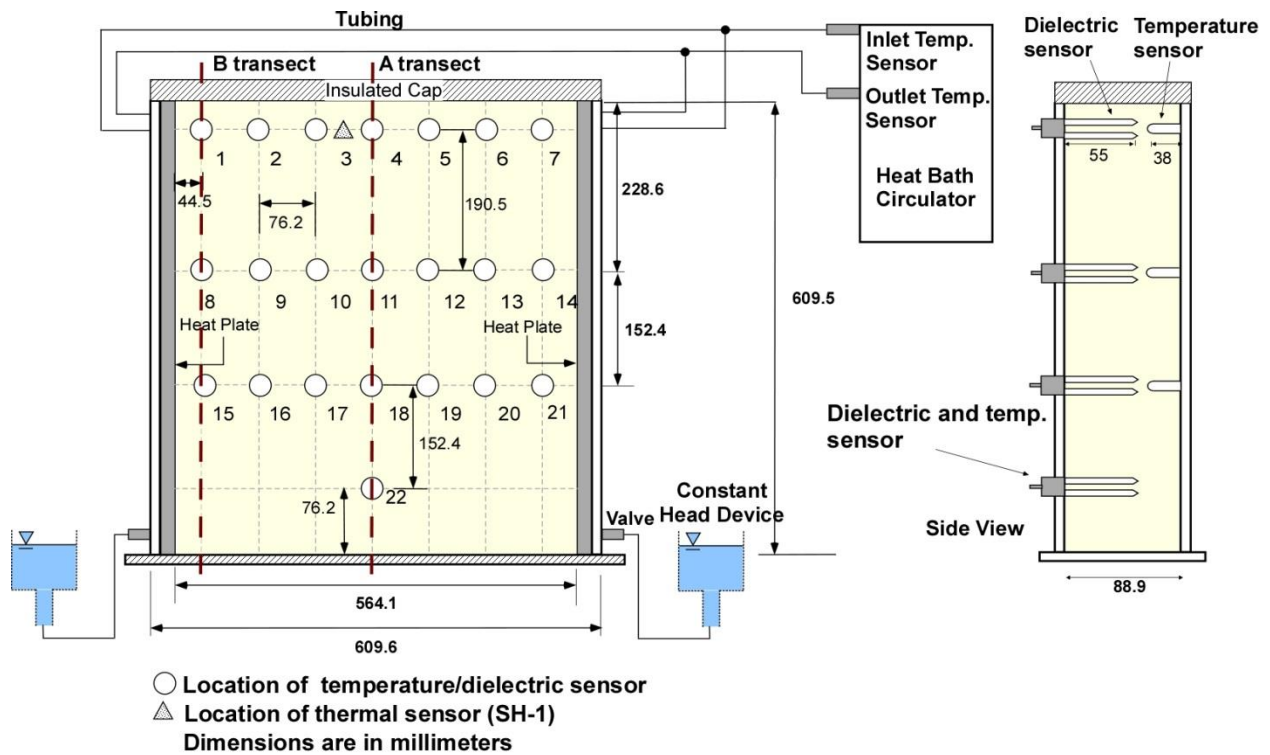
1119 **Figure 13.** Effect of soil porosity (\emptyset) in (a) degree of saturation (b) temperature with time and effect of
1120 saturated hydraulic conductivity (KH) in (c) degree of saturation (d) temperature at point #2 as shown in
1121 figure 8(b).

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1123 time at point #2 as shown in Figure 8(b).
1124 **Figure 15.** Vertical profile of initial and final values for degree of saturation (a, c, e) and temperature (b,
1125 d, f) along transect A (Figure 2) for all three cases. Case 1: initial degree of saturation of approximately
1126 19%, Case 2: $48 \% < S < 51\%$, Case 3: $89 \% < S < 100\%$



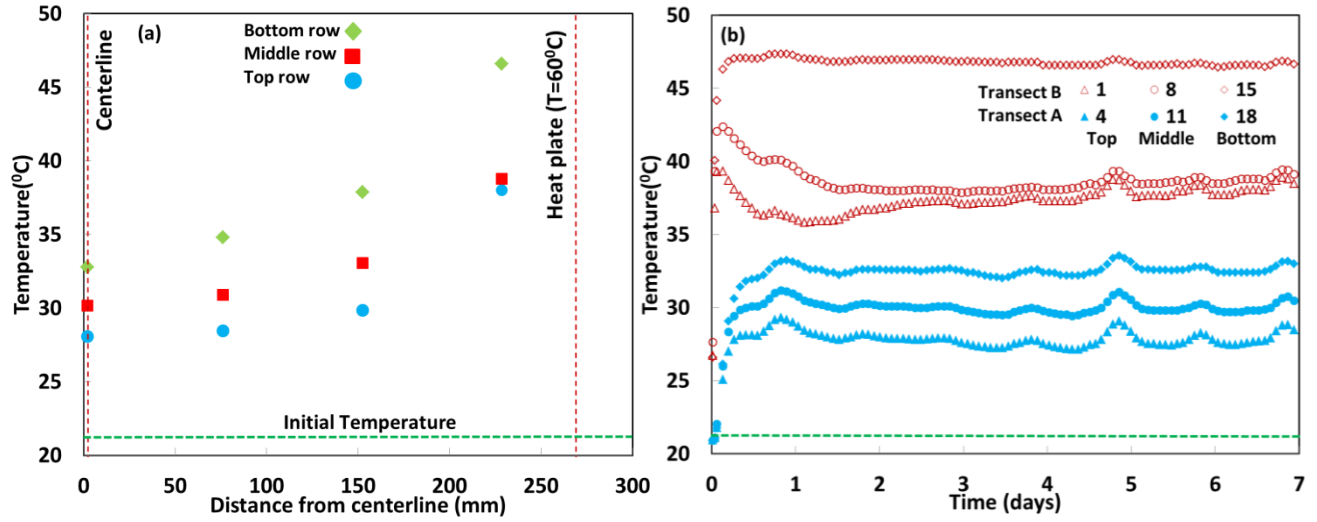
1127

1128 Figure 1. Thermal conductivity-degree of saturation and primary drainage capillary pressure- degree of
 1129 saturation relationships measured at room temperature for all test soils.



1130

1131 Figure 2. Schematic of the test tank apparatus used in experiments discussed here (not to scale).

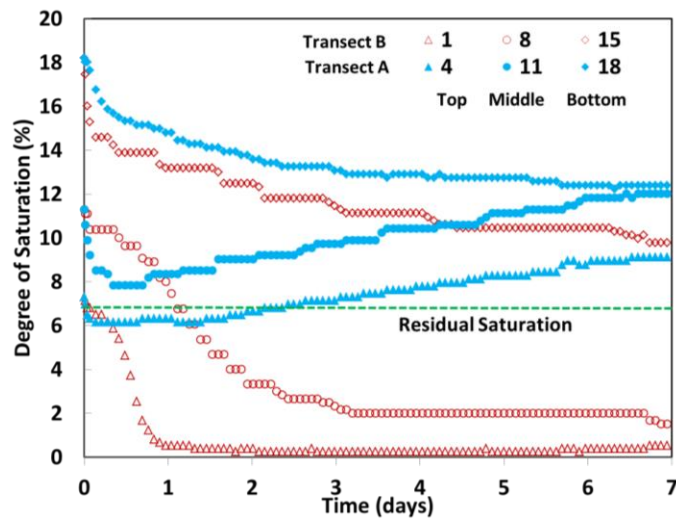


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1133 Figure 3. Steady state temperature (time = 7days) measured vertically from the middle of the soil tank

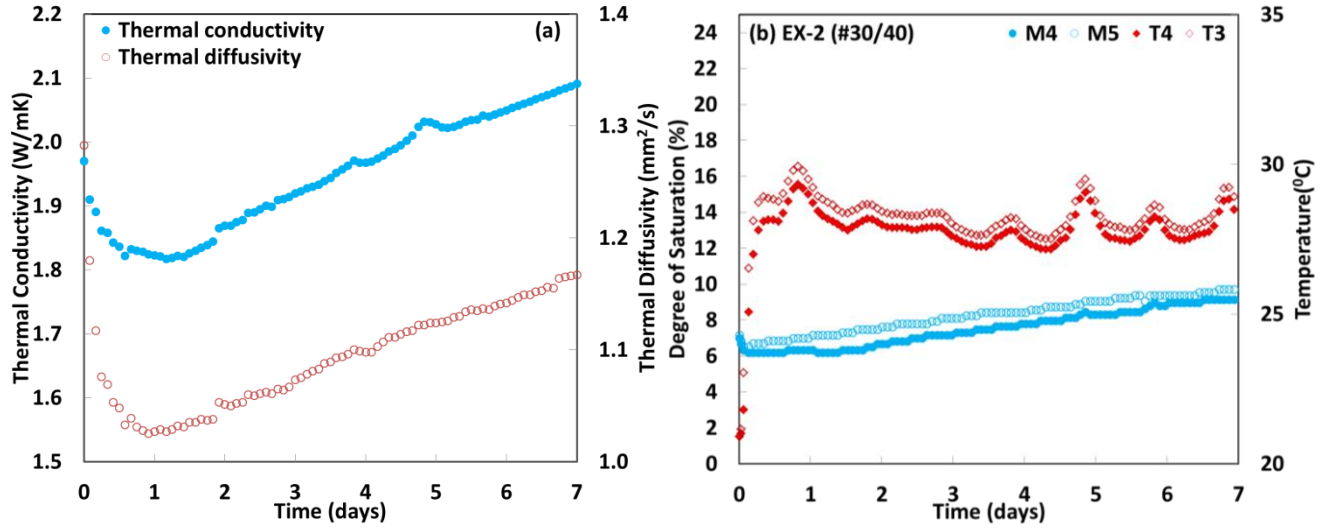
1134 toward the heat plate and (a) temperature variation with time along transects A and B for EX-2 (b).

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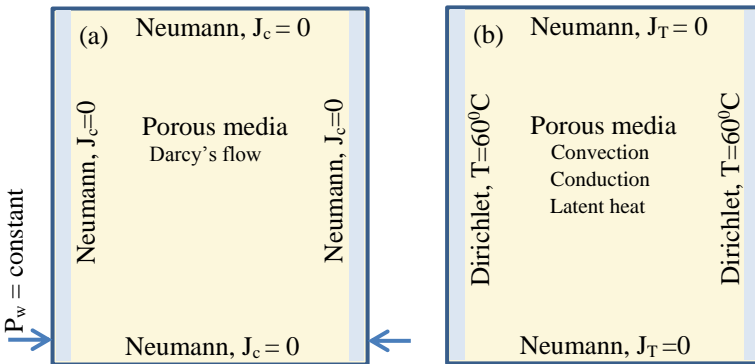
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1137 Figure 4. Degree of Saturation with time for sensors located along transects A and B (EX-2).

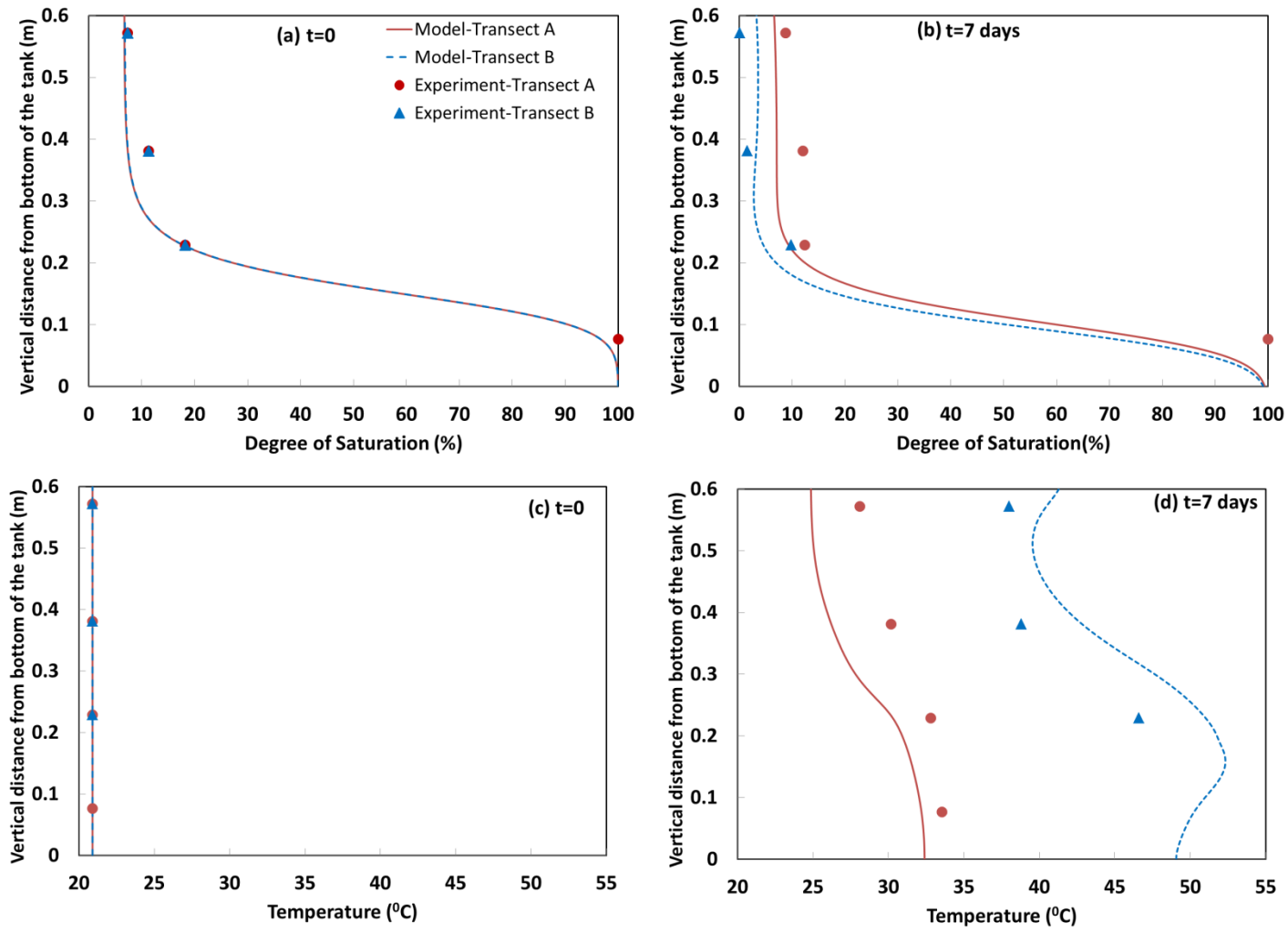


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 1139 Figure 5. Thermal properties of soil at the location of SH-1 sensor (a) in EX-2. Degree of Saturation and
 1140 temperature profiles as a function of time for two adjacent sensors #4 and #3 for the same experiment (b).
 1141 (M: Dielectric sensor, T: Temperature sensor)

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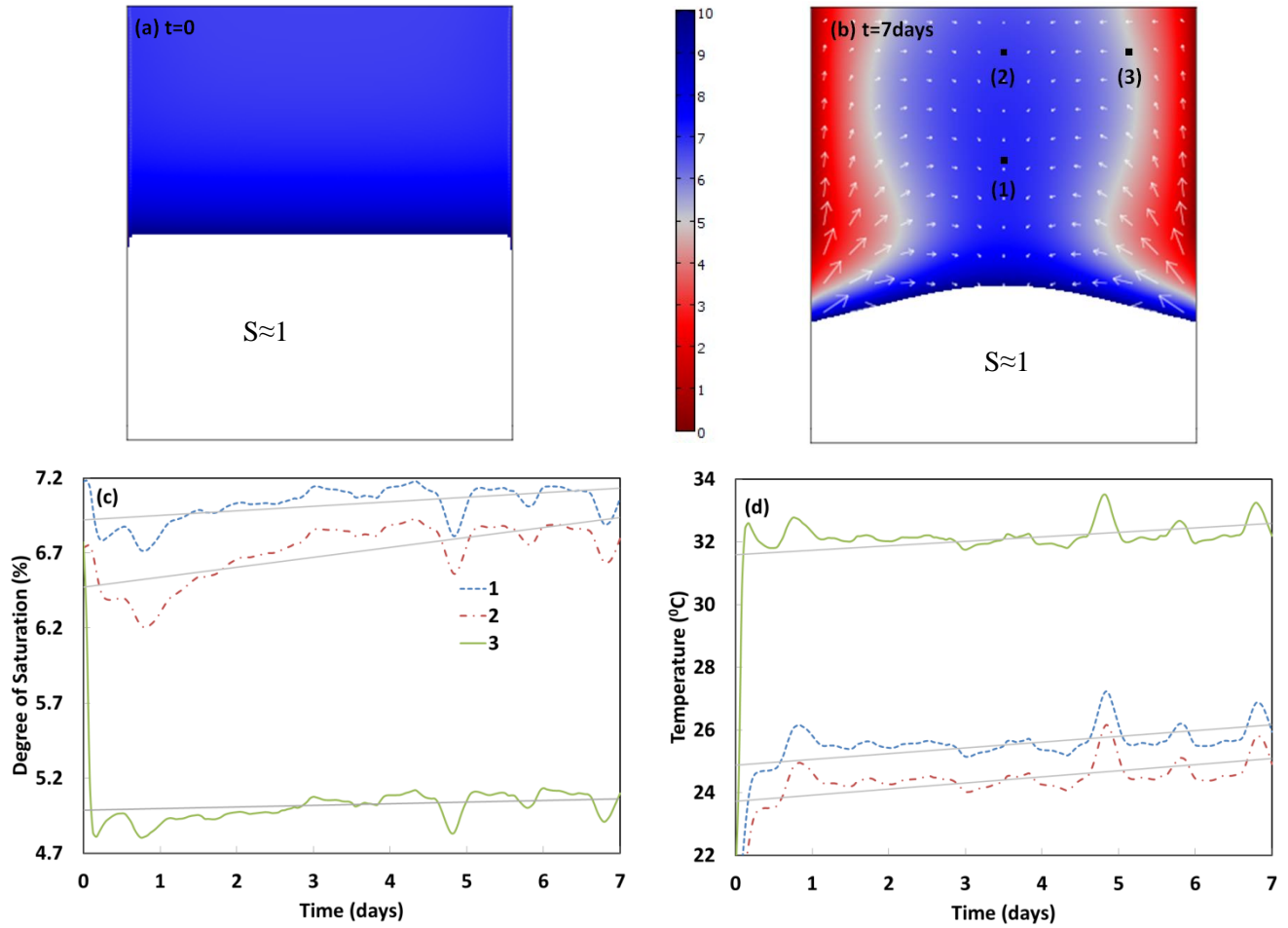


1143
 1144 Figure 6. Boundary conditions for two-dimensional configuration where T is temperature, P_w is water
 1145 pressure, J_c is mass flux (liquid water or water vapor) and J_T is heat flux in the domain.



1146 Figure 7. Simulated and observed degree of saturation and temperature profiles along transects A and B at
 1147 0 and 7 days. (a), (b) initial and final degree of saturation values and (c), (d) initial and final temperatures
 1148 along transects A and B.

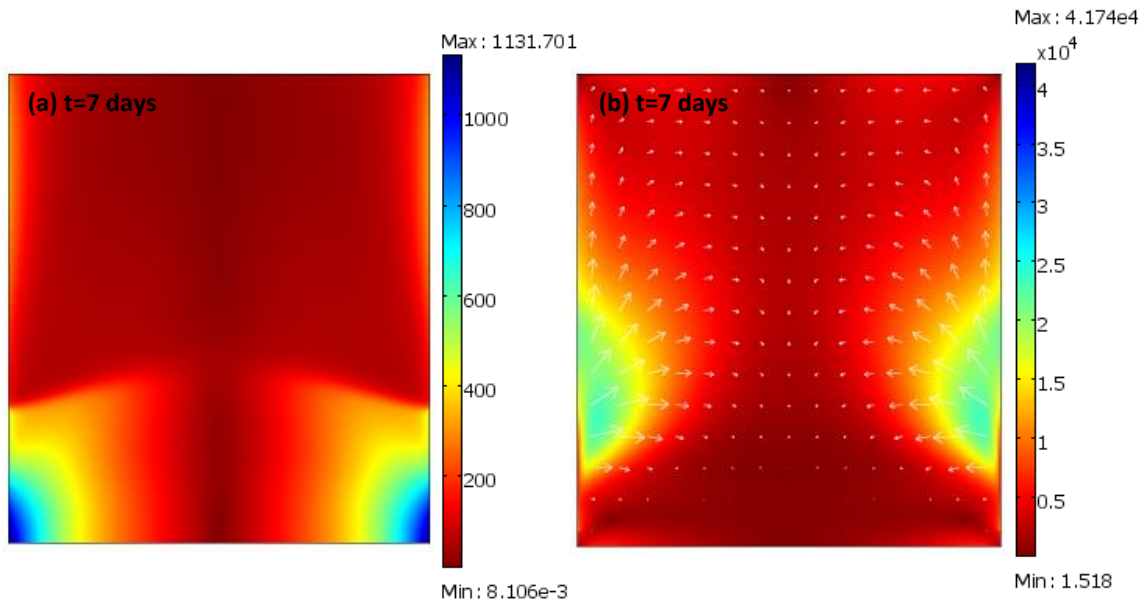
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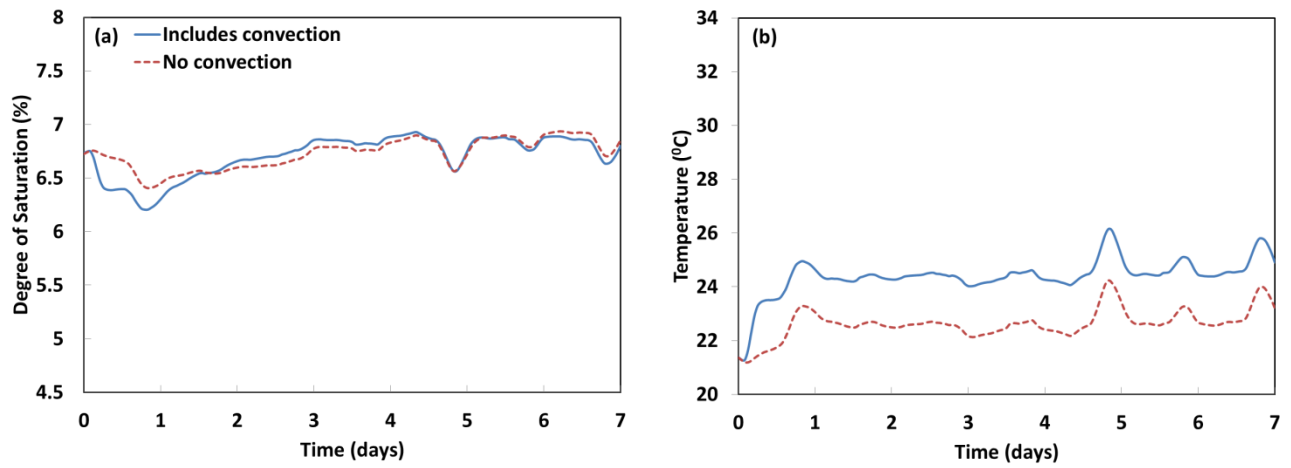
1153 Figure 8. Simulated soil degree of saturation distribution (a) at $t=0$ and (b) $t=7$ days (arrows representing
 1154 velocity field) within the tank. The lower part of the tank (white portion) with almost saturated soil is
 1155 excluded from Figure 8 (a), 8(b) to better illustrate the soil degree of saturation differences throughout the
 1156 unsaturated region. Points 1-3 were selected corresponding to locations for three points depicted in 8(b) to
 1157 better illustrate the change in (c) degree of saturation and (d) temperature with time.

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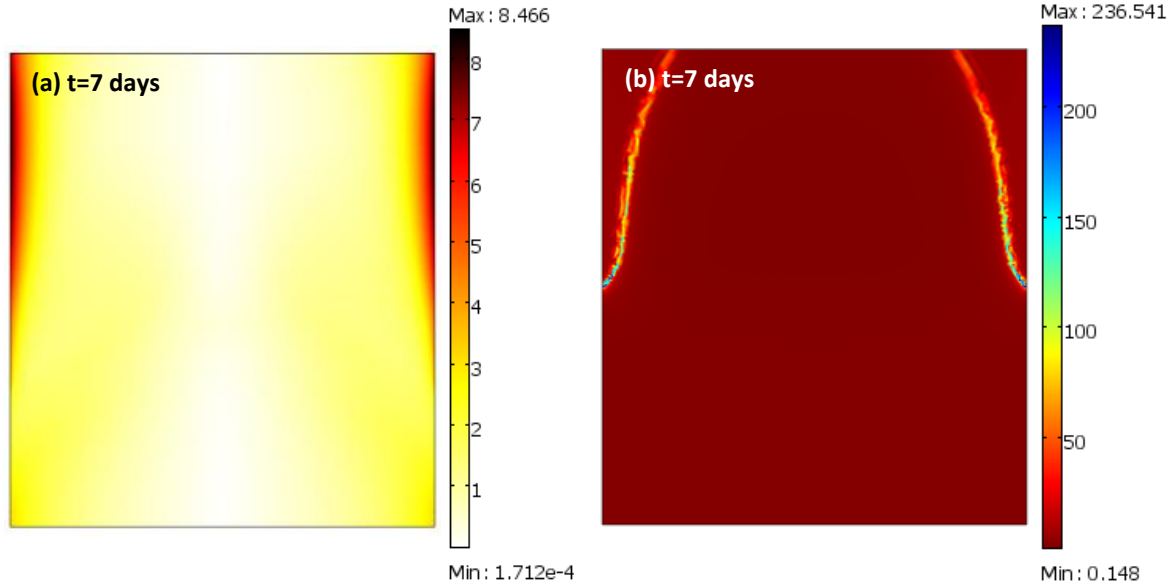
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1160
 1161 Figure 9. Surface plot of simulated conductive (a) and convective (b) heat flux. Arrows in Figure 9(b)
 1162 show the velocity field for gas phase. (Units: W/m^2)
 1163

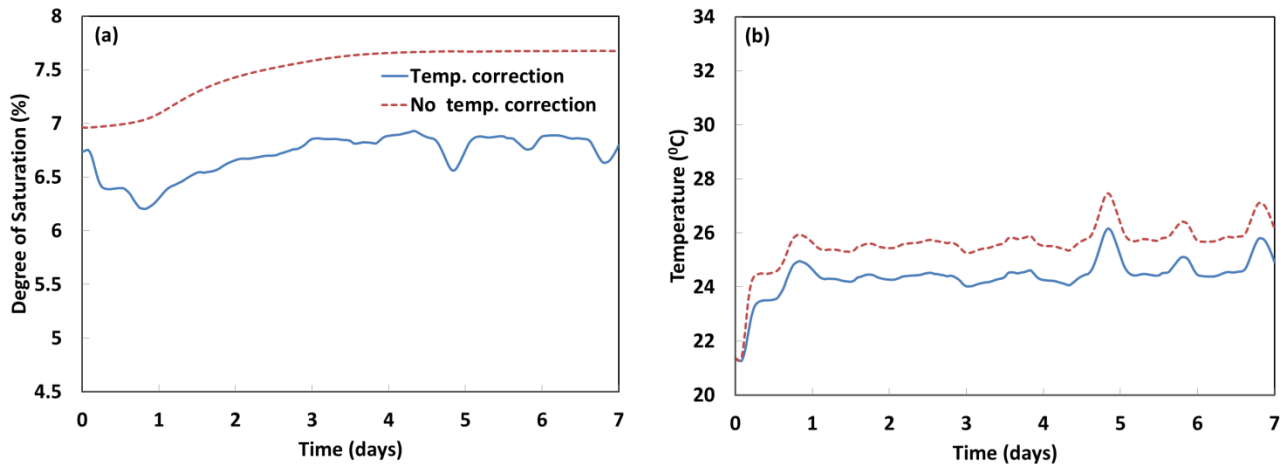


1164 Figure 10. Effect of convective heat flux in (a) degree of saturation (b) temperature profile with time at
 1165 point #2 as shown in Figure 8(b).
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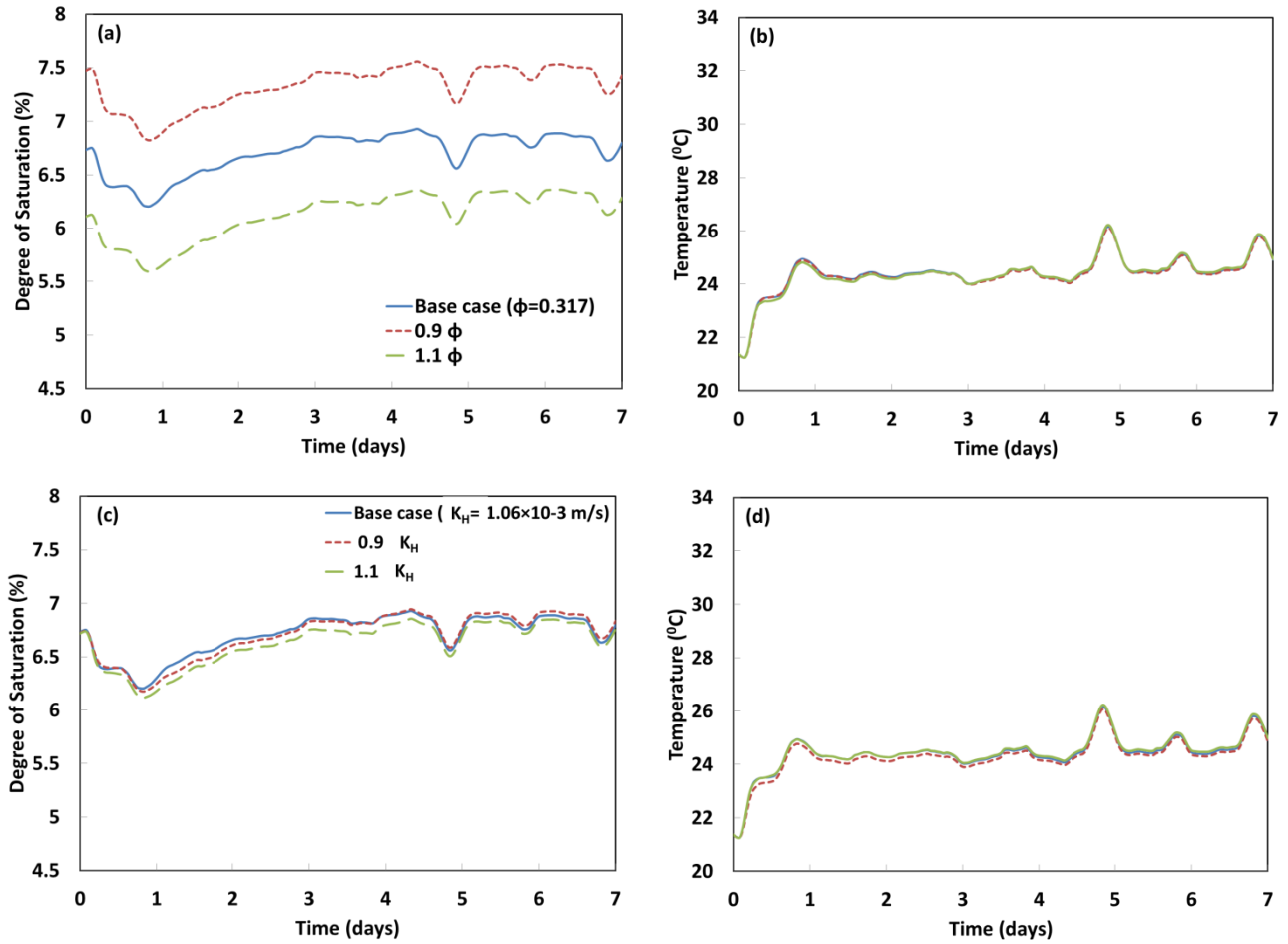


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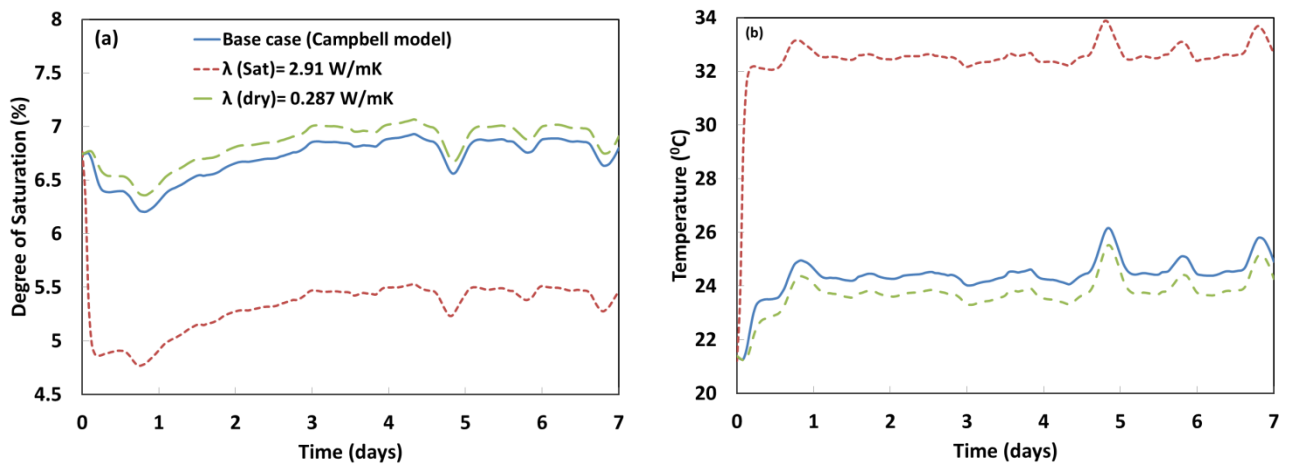
Figure 11. Simulated surface plots of (a) temperature gradient ($^{\circ}\text{C}/\text{cm}$) and (b) hydraulic head gradient ($\text{cm H}_2\text{O}/\text{cm}$) within the domain. Analysis of results demonstrates that thermal gradients have more contribution in moisture flow than total hydraulic head gradients.



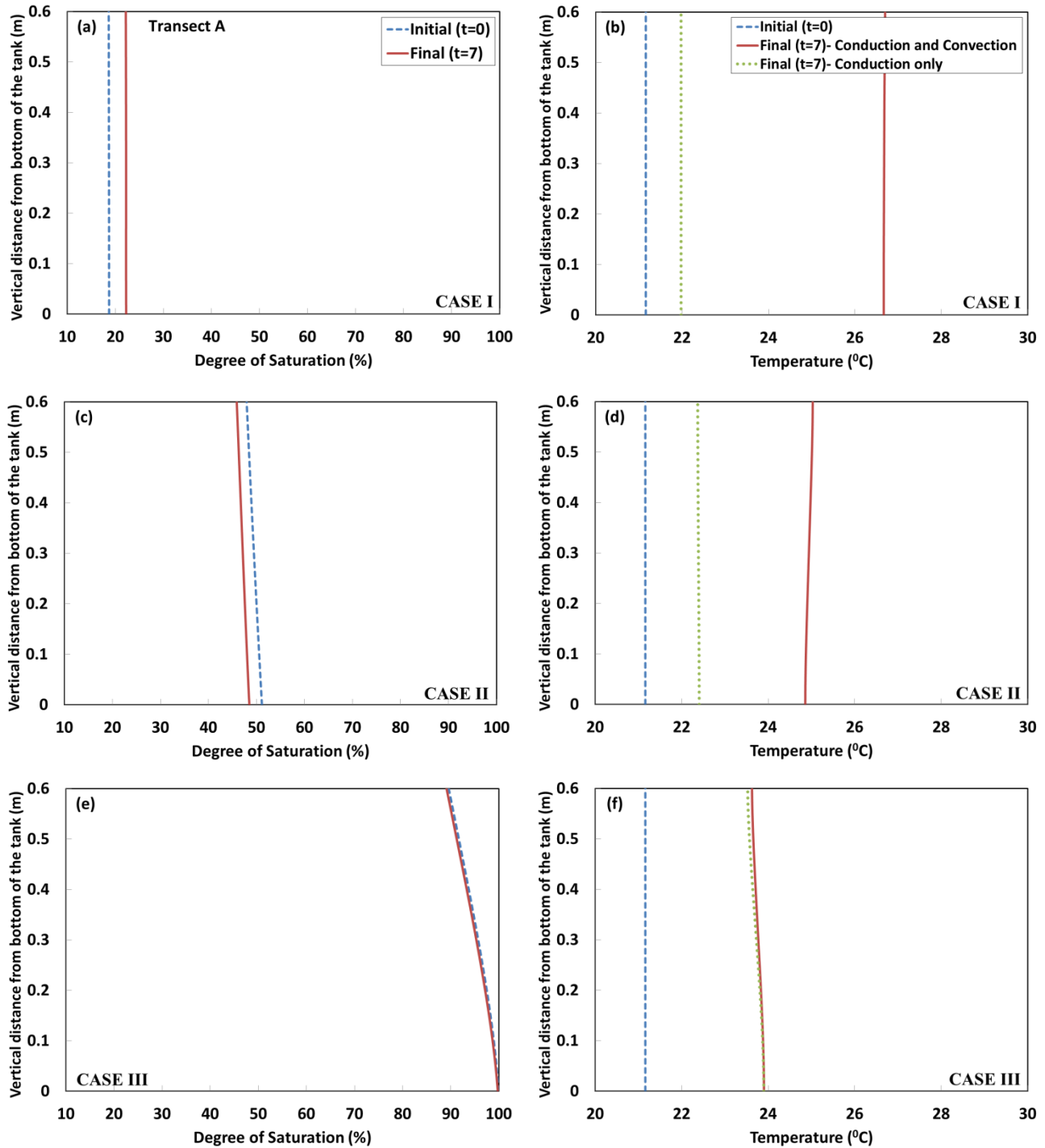
1173 Figure 12. Effect of temperature correction of the WRC on the predicted trends at point 2 in Figure 8(b):
 1174 (a) degree of saturation (b) Temperature.
 1175



1176 Figure 13. Effect of soil porosity (ϕ) in (a) degree of saturation (b) temperature with time and effect of
 1177 saturated hydraulic conductivity (K_H) in (c) degree of saturation (d) temperature at point #2 as shown in
 1178 figure 8(b).



1179 Figure 14. Effect of constant thermal conductivity in (a) degree of saturation (b) temperature profile with
 1180 time at point #2 as shown in Figure 8(b).



1181 Figure 15. Vertical profile of initial and final values for degree of saturation (a, c, e) and temperature (b,
 1182 d, f) along transect A (Figure 2) for all three cases. Case 1: initial degree of saturation of approximately
 1183 19%, Case 2: $48\% < S < 51\%$, Case 3: $89\% < S < 100\%$

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