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## Secondary Organic Aerosol Formation and Organic Nitrate Yield from NO<sub>3</sub> Oxidation of Biogenic Hydrocarbons

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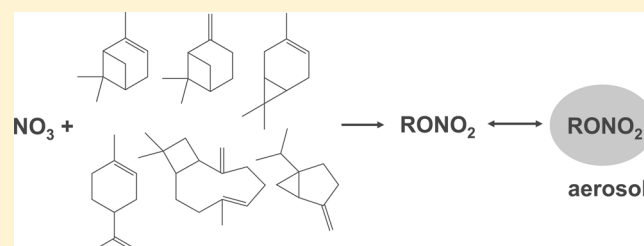
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### Supporting Information

**ABSTRACT:** The secondary organic aerosol (SOA) mass yields from NO<sub>3</sub> oxidation of a series of biogenic volatile organic compounds (BVOCs), consisting of five monoterpenes and one sesquiterpene ( $\alpha$ -pinene,  $\beta$ -pinene,  $\Delta$ -3-carene, limonene, sabinene, and  $\beta$ -caryophyllene), were investigated in a series of continuous flow experiments in a 10 m<sup>3</sup> indoor Teflon chamber. By making in situ measurements of the nitrate radical and employing a kinetics box model, we generate time-dependent yield curves as a function of reacted BVOC. SOA yields varied dramatically among the different BVOCs, from zero for  $\alpha$ -pinene to 38–65% for  $\Delta$ -3-carene and 86% for  $\beta$ -caryophyllene at mass loading of 10  $\mu\text{g m}^{-3}$ , suggesting that model mechanisms that treat all NO<sub>3</sub> + monoterpene reactions equally will lead to errors in predicted SOA depending on each location's mix of BVOC emissions. In most cases, organonitrate is a dominant component of the aerosol produced, but in the case of  $\alpha$ -pinene, little organonitrate and no aerosol is formed.



## INTRODUCTION

Secondary organic aerosol (SOA), formed in situ from the conversion of gas-phase volatile organic compounds (VOCs) to oxidized products that partition preferentially to the particle phase, is an important source of aerosol mass both regionally and globally. It is estimated that approximately 70% of total global organic aerosol production is secondary (~150 TgC/yr),<sup>1</sup> but formation mechanisms remain uncertain.

A large fraction of total organic aerosol is thought to originate from the oxidation products of *biogenic* VOC emissions.<sup>1,2</sup> These naturally emitted compounds constitute the majority of VOC emissions to the atmosphere globally,<sup>3–5</sup> with a diverse and regionally varied mixture of isoprenoid chemical structures, depending on regional plant species distributions. The gas-phase oxidation of VOCs to condensable products is initiated by reaction with O<sub>3</sub> or the OH or NO<sub>3</sub> radicals. The relative importance of each competing oxidant depends on the relevant rate constants (which depends on the VOC molecular structure) and ambient concentrations. For example, NO<sub>3</sub>-initiated reactions with biogenic alkenes have large rate constants,<sup>6</sup> and will be most important at night (when photolysis and NO reaction sinks for NO<sub>3</sub> radical are

minimized), and in regions that contain both high biogenic emissions and elevated NO<sub>x</sub> such as downwind of urban areas or industrial point sources. SOA yields from OH and O<sub>3</sub> oxidation of BVOC have been studied extensively,<sup>7</sup> but less is known about reactions involving NO<sub>3</sub>-induced oxidation.

Because partitioning to the aerosol phase depends on molecular weight and polarity,<sup>8</sup> the precursor VOC generally needs to contain a minimum number of carbon atoms (or undergo condensed phase oligomerization reactions) to produce condensable oxidation products and thus form SOA. Isoprene (C<sub>5</sub>H<sub>8</sub>) is the globally dominant BVOC, comprising ~50% of total global nonmethane VOC emissions by mass<sup>5</sup> with total emissions estimated at approximately 500 Tg yr<sup>-1</sup>. However, isoprene and its NO<sub>3</sub>-induced oxidation products are quite volatile, and thus have relatively low NO<sub>3</sub> SOA yields of 4–24%.<sup>9</sup> The larger monoterpenes (C<sub>10</sub>H<sub>16</sub>) and sesquiterpenes (C<sub>15</sub>H<sub>24</sub>), which are much more prevalent in coniferous

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forests, are more efficient SOA precursors via their production of extremely low-volatility organic compounds.<sup>10</sup>

The NO<sub>3</sub> oxidation of some terpenes has been studied in laboratory experiments, summarized in Table 1. Wängberg et al.,<sup>11</sup> Hallquist et al.,<sup>12</sup> and Spittler et al.<sup>13</sup> all observed substantially higher ketone yields and lower organonitrate yields for  $\alpha$ -pinene than for the other terpenes; where SOA yield measurements are available they roughly correlate with organonitrate yields, showing lower yield for  $\alpha$ -pinene. We note that these chamber experiments may preclude further oxidation of initial products, which could produce additional SOA in the real atmosphere (e.g., photo-oxidation of pinonaldehyde<sup>14</sup>).

A systematic controlled chamber study of SOA production from six mono- and sesquiterpenes is the focus of the work presented here. We measured the SOA yield from NO<sub>3</sub> reacting with the individual monoterpenes  $\alpha$ -pinene,  $\beta$ -pinene,  $\Delta$ -3-carene, limonene, sabinene, and with the sesquiterpene  $\beta$ -caryophyllene (structures shown in Supporting Information (SI) Figure S6 and in the abstract). Since the nitrate-peroxy radicals produced from these terpenes are all tertiary, we expect no HO<sub>2</sub> production in the chamber. Hence, these experiments explore RO<sub>2</sub>—RO<sub>2</sub> and RO<sub>2</sub>—NO<sub>3</sub> chemistry only, omitting RO<sub>2</sub>—HO<sub>2</sub> chemistry that would contribute in the real nighttime atmosphere. These experiments were performed in continuous-flow mode in a dark chamber at the Atmospheric Chemistry Division of the National Center for Atmospheric Research (NCAR) in Fall 2011. We monitored particle size distributions and total alkyl nitrate concentrations to enable determination of SOA mass yields and alkyl nitrate yields. We interpreted key observations based on chemical structure and proposed mechanisms.

## EXPERIMENTAL AND THEORETICAL METHODS

**NCAR Chamber Facility.** A detailed description of the NCAR Chamber Facility instrumentation and cleaning and operating procedures for the experiments described herein are provided in the SI. Figure SI shows the chamber diagram, and Table SI the instrumentation employed in these experiments. Briefly, the 10 m<sup>3</sup> chamber<sup>18,19</sup> was run with all reagents input continuously under dark conditions, with an average chamber residence time of 4 h. The NO<sub>3</sub> and N<sub>2</sub>O<sub>5</sub> concentrations were alternately measured either before entering the chamber, or from the chamber itself. Flows were adjusted to give initial [N<sub>2</sub>O<sub>5</sub> + NO<sub>3</sub>] and [BVOC] of 10–100 ppb in dry zero air. SOA experiments were initiated by injecting BVOC (~50 ppm in N<sub>2</sub>) into the N<sub>2</sub>O<sub>5</sub> + NO<sub>3</sub> filled chamber, delivered from the standard cylinders using flow restrictors and added to the zero air flow to obtain the final desired mixing ratios (Table 2). This results in decay of chamber N<sub>2</sub>O<sub>5</sub> + NO<sub>3</sub> as the BVOC reacts away.

A series of 11 experiments were conducted with the six BVOC, in most cases with two levels of oxidant and BVOC concentrations: a nominally “high” (~50 ppb) and a “low” (~10 ppb) concentration of each (see Table 2). For the high concentration experiments only (Expts. 1, 2, 4, 6, and 9), organic nitrate measurements are available. In these experiments, total alkyl + peroxy nitrate mixing ratios ( $\Sigma$ ANs + PNs), subsequently referred to collectively as organonitrates, are determined in the gas and aerosol phases by sampling directly or through a charcoal denuder.<sup>20</sup>

**Instrumentation.** The following measurements were made during each experiment: (1) NO<sub>3</sub> and N<sub>2</sub>O<sub>5</sub> concentrations on both inlet and outlet flows by cavity ringdown spectroscopy

Table 1. Oxidation Products and SOA Yields Observed in Previous Studies of NO<sub>3</sub> + Terpenes

BVOC	ketone molar yield <sup>a</sup>	organonitrate molar yield	SOA mass yield
$\alpha$ -pinene	58–66% Wängberg et al. <sup>11</sup> 65–72% Hallquist et al. <sup>12</sup> 39–58% Spittler et al. <sup>13</sup>	14% Wängberg et al. <sup>11</sup> 18–25% Hallquist et al. <sup>12</sup> 11–29% Spittler et al. <sup>13</sup>	7% Hallquist et al. <sup>12</sup> 0.3–0.7% Moldanova and Ljungstrom <sup>15</sup> 4–16% Spittler et al. <sup>13</sup>
$\beta$ -pinene	0–2% Hallquist et al. <sup>12</sup>	51–74% Hallquist et al. <sup>12</sup> 40% Fry et al. <sup>16</sup>	>39% Hallquist et al. <sup>12</sup> 50% Fry et al. <sup>16</sup> 18–35% Moldanova and Ljungstrom <sup>15</sup>
$\Delta$ -carene	0–3% Hallquist et al. <sup>12</sup>	68–74% Hallquist et al. <sup>12</sup>	>15% Hallquist et al. <sup>12</sup> >13% Moldanova and Ljungstrom <sup>15</sup>
limonene	69% Hallquist et al. <sup>12</sup> 25–33% Spittler et al. <sup>13</sup>	48% Hallquist et al. <sup>12</sup> 63–72% Spittler et al. <sup>13</sup> 30% Fry et al. <sup>17</sup>	17% Hallquist et al. <sup>12</sup> 20–40% Spittler et al. <sup>13</sup> 18% Moldanova and Ljungstrom <sup>15</sup>

<sup>a</sup>In Hallquist et al.,<sup>12</sup> these ketone yields refer to the dominant single ketone product, e.g. in the case of  $\alpha$ -pinene, pinonaldehyde.

Table 2. Experimental Conditions<sup>a</sup>

expt #	date	BVOC	[BVOC] <sub>i</sub> (ppb)	[N <sub>2</sub> O <sub>5</sub> ] <sub>i</sub> (ppb)	<i>k</i> <sub>NO<sub>3</sub>+BVOC</sub> @298 K (cm <sup>3</sup> molec <sup>-1</sup> s <sup>-1</sup> )	[N <sub>2</sub> O <sub>5</sub> ] <sub>i</sub> /[BVOC] <sub>i</sub>
1	9/15/11	α-pinene (seeded)	48	54	6.16 × 10 <sup>-12</sup>	1.1
2	9/28/11	β-pinene "high"	41	60	2.51 × 10 <sup>-12</sup>	1.5
3	10/18/11	β-pinene "low"	10	10	2.51 × 10 <sup>-12</sup>	1.0
4	9/19/11	Δ-3-carene "high"	16	42	9.1 × 10 <sup>-12</sup>	2.6
5	10/21/11	Δ-3-carene "low"	10	9	9.1 × 10 <sup>-12</sup>	0.9
6	10/3/11	limonene "high"	40	60	1.22 × 10 <sup>-11</sup>	1.5
7	10/11/11	limonene "low"	10	10	1.22 × 10 <sup>-11</sup>	1.0
8	10/15/11	limonene (+ O <sub>3</sub> + NO <sub>2</sub> )	10	[O <sub>3</sub> ] <sub>i</sub> = 12 ppb; [NO <sub>2</sub> ] <sub>i</sub> = 6.3 ppb	1.22 × 10 <sup>-11</sup>	1.2
9	9/22/11	β-caryophyllene "high"	109	40	1.9 × 10 <sup>-11</sup>	0.4
10	10/26/11	β-caryophyllene "low"	3	10	1.9 × 10 <sup>-11</sup>	3.0
11	11/11/11	sabinene	9	10	1 × 10 <sup>-11</sup>	1.1

<sup>a</sup>Except α-pinene, all experiments were conducted without seed aerosol. Rate constants at 298 K are taken from Calvert et al. (2000).<sup>21</sup> For the "low" experiments, the ratio of N<sub>2</sub>O<sub>5</sub> to BVOC in the inlet line was approximately 1:1; for the "high" experiments, the oxidant was generally in slight excess (with the exception of Expt # 9). The highest purity sabinene source available was 80%, and contained 20% β-pinene. No correction was applied for this, so sabinene SOA reflects this mixture.

(CRDS, Wagner et al.;<sup>22</sup> Dube et al.<sup>23</sup>), and on the outlet side only: (2) NO and NO<sub>2</sub> by chemiluminescence, (3) O<sub>3</sub> by absorption spectroscopy, (4) particle number and size distribution by a scanning mobility particle sizer (SMPS), and (5) organonitrates by thermal dissociation–laser-induced fluorescence (TD-LIF, Rollins et al.<sup>20</sup>). The specifications of each instrument used in these experiments are shown in Table S1 in the SI.

**Wall Losses.** In order to interpret observed aerosol formation, it is essential to understand the effect of chamber wall losses on measured aerosol size distributions. Following the methods of Van Reken et al.,<sup>24</sup> we measured the size-dependent wall loss of ammonium sulfate aerosol at steady-state flow. Results and additional analysis details are shown in the SI (Figure S2). Average input and output size distributions were analyzed to derive the first-order size-dependent wall loss coefficient, β(*d<sub>p</sub>*), with the chamber considered to behave as a continuously stirred tank reactor:<sup>25,26</sup>

$$\beta(d_p) = \frac{Q}{V} \left( \frac{n_{in}(d_p)}{n_{out}(d_p)} - 1 \right) \quad (1)$$

The losses are applied cumulatively, so that corrected aerosol mass timeseries include all particles lost since the start of the experiment, following the method of McMurry and Grosjean,<sup>27</sup> and we find values consistent with previous chamber studies.<sup>24</sup>

Recent work has shown that vapor-phase wall losses may also substantially contribute to underestimation of chamber SOA yields,<sup>28,29</sup> suggesting that the yields reported here may be lower limits. The implications of this unconstrained process for observed relative organonitrate yields is discussed in below.

## RESULTS

**Qualitative Differences in Aerosol Formation.** Particle formation and growth was observed for all BVOCs except α-pinene, although with widely varying yields. The observed time evolution of the particle size distribution function of a representative experiment (Experiment 3, β-pinene at low concentration) is shown in Figure 1, illustrating the new particle formation and growth that occurred in each experiment (except α-pinene).

Figure 2 shows the time evolution of aerosol number (*N*<sub>tot</sub>, Figure 2a) and volume concentration (*V*<sub>tot</sub>, Figure 2b,c). These

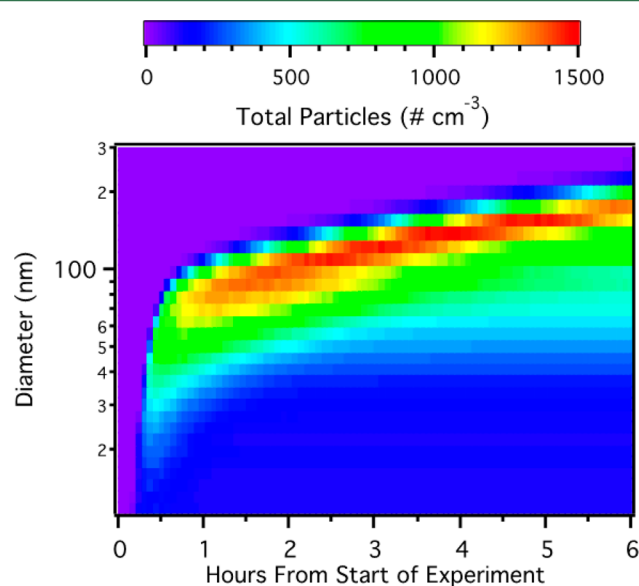
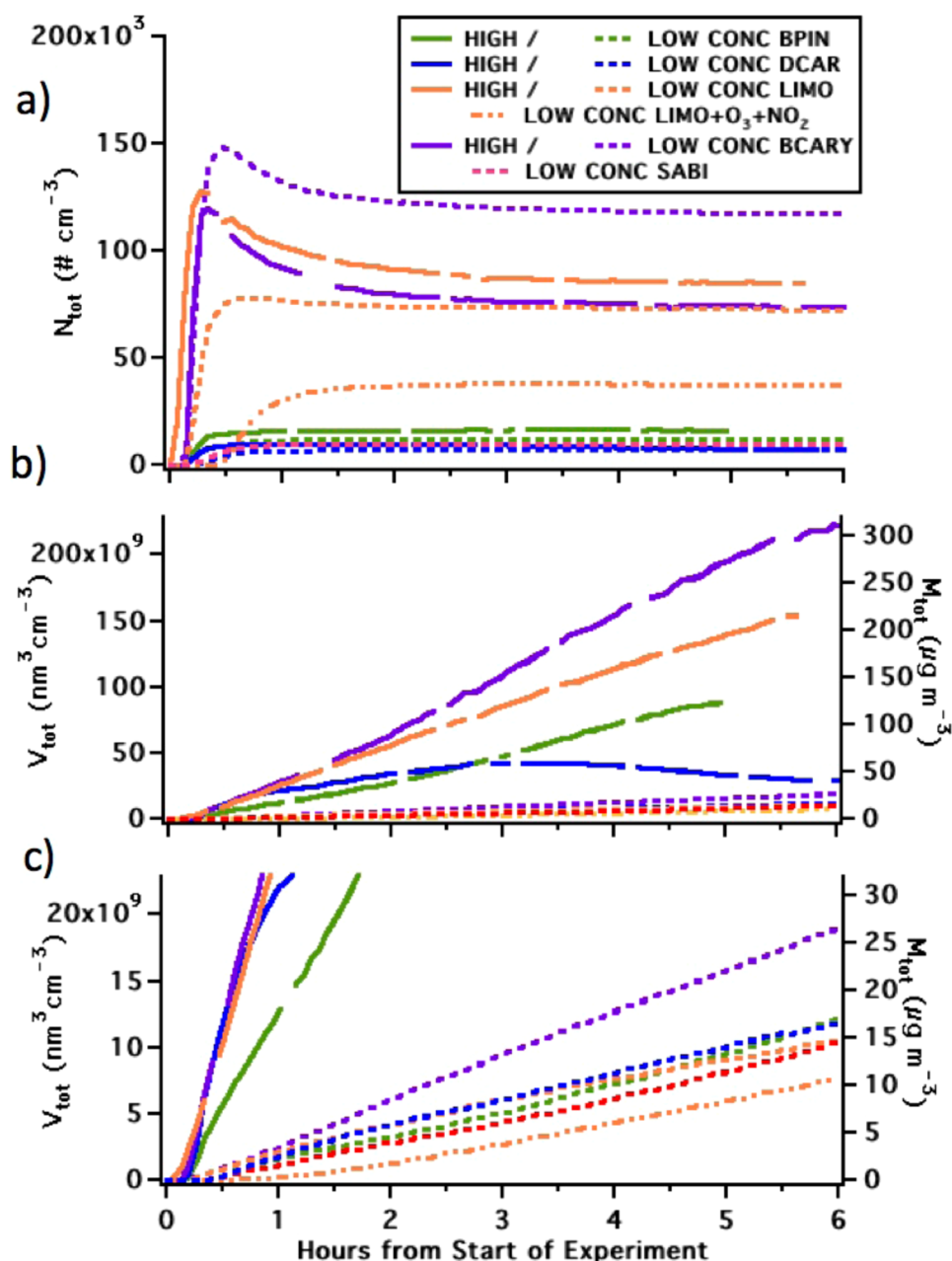


Figure 1. Wall loss corrected SOA growth curve for Experiment 3 (β-pinene low concentration).

plots show the comparison of SOA growth from different BVOC precursors, including both concentration conditions for each precursor (nominally 50 and 10 ppb for both NO<sub>3</sub> and BVOC). Generally, we observe the largest peaks in *N*<sub>tot</sub> from the oxidation of the BVOCs with two double bonds, β-caryophyllene and limonene, regardless of low or high concentration. Hence, for example, the peak *N*<sub>tot</sub> from limonene at 10 ppb initial concentration is larger than the peak *N*<sub>tot</sub> for all the monoterpenes with a single double bond, even at the higher concentration initial conditions. In contrast, the *V*<sub>tot</sub> curves grow fastest for the higher concentration experiments of all terpene precursors. In the case of β-caryophyllene, the faster volume growth at low loading may be due to differing chemical regime; higher NO<sub>3</sub>/BVOC ratio could lead to more second-generation products.

**Aerosol Yield Determination.** We determined the unitless time-dependent SOA mass yields over the course of the experiments, defined as *Y* = Δ*M*/Δ*V*OC, based on wall-loss corrected change in aerosol mass Δ*M* (μg m<sup>-3</sup>) divided by amount of VOC reacted Δ*V*OC (μg m<sup>-3</sup>), referenced to the



**Figure 2.** Time series of total wall-loss corrected aerosol (a) particle number concentration, and (b) volume and mass concentration, from all experiments producing SOA. Panel (c) repeats (b), zoomed in on the lowest  $30 \mu\text{g m}^{-3}$  of the y axis to show that the same pattern in volume growth is observed for the low-concentration series as for the high. LOW and HIGH indicate the nominal concentrations of BVOC and oxidant in each experiment; BPIN denotes  $\beta$ -pinene; DCAR,  $\Delta$ -3-carene, LIMO, limonene; BCARY,  $\beta$ -caryophyllene; and SABI, sabinene.

beginning of the experiment when both aerosol mass ( $M$ ) and VOC were zero.

Since each experiment was initiated with VOC injection into a chamber already filled with oxidant, the VOC began to react immediately, preventing measurement of its concentration during initial reaction. Therefore, the  $\Delta\text{VOC}$  in each experiment must be calculated. Since there are uncertainties in both the reaction kinetics and chamber mixing, we employ two separate strategies to bracket the possible range of  $\Delta\text{VOC}$ : (1) a simple observationally constrained method that more accurately captures mixing dynamics due to the high precision and time resolution measurement of  $[\text{NO}_3]$ , and (2) a free-running kinetics box model assuming a well-mixed chamber, that may more accurately capture subsequent  $\text{RO}_2$  chemistry,

but is subject to large uncertainties in  $\text{RO}_2$  rate constants for these systems and cannot capture mixing.

For the first method, we use the known amount of VOC injected and the observed  $[\text{NO}_3]$  in each time step ( $\Delta t$ ) to determine the amount of VOC consumed via eq 2:

$$\Delta\text{VOC}_i = k[\text{NO}_3][\text{VOC}]\Delta t_i \quad (2)$$

where rate constants  $k$  are taken from Calvert et al. (2000),<sup>21</sup>  $[\text{NO}_3]$  is the instantaneous observed concentration (and hence includes  $\text{NO}_3$  produced from  $\text{N}_2\text{O}_5$  added at each time step), and  $[\text{VOC}]$  is the sum of concentration added to the chamber and the unreacted concentration in the chamber from the previous time step. If this calculation of  $\Delta\text{VOC}$  results in a reacted amount less than the VOC injected during that time

step, then the residual VOC builds up in the chamber and contributes to the instantaneous rate calculation for the next timestep. In this way, a  $\Delta\text{VOC}$  ( $=\sum_{i=0}^t \Delta\text{VOC}_i$ ) timeseries is derived that depends only on observed  $\text{NO}_3$  consumption, assuming a one-to-one  $\text{NO}_3$  to VOC stoichiometry. This method ignores any reactions of  $\text{NO}_3$  with first-generation oxidation products ( $\text{NO}_3 + \text{RO}_2$  reactions), thus rendering it an upper limit on the amount of VOC reacted, which leads to lower limit SOA yields. However, it has the advantage of allowing our most precise, highest time-resolution measurement to directly incorporate the time scale of chamber mixing into the calculation of  $\Delta\text{VOC}$ . Thus, for each experiment we determine a complete  $\Delta\text{VOC}$  time series that is constrained until  $\text{NO}_3$  concentration decreases to zero, as shown in the SI (Figure S3). Often, the usable SMPS data is truncated before this occurs, because the aerosol size distribution grows to diameters beyond the measurement range ( $\sim 350$  nm).

In the second method of  $\Delta\text{VOC}$  calculation, we employ a free-running kinetics box model constrained only by the known addition rates of  $\text{N}_2\text{O}_5$  and VOC. The cumulative VOC reacted over time is determined, by iterative solution of coupled kinetic equations for all X molecules:

$$\frac{d[X]}{dt} = ([X]_{\text{in}} - [X]_{\text{ch}}) \times \frac{Q}{V} - \sum_Y k_Y [X]_{\text{ch}} [Y]_{\text{ch}} + \sum_Z k_Z [Z]_{\text{ch}} - k_{\text{wall},X} [X]_{\text{ch}} \quad (3)$$

where  $[X]_{\text{in}}$  is the concentration of X in the inlet flow (only  $\text{N}_2\text{O}_5$  and VOC are added, at known concentrations shown in Table 2),  $[X]_{\text{ch}}$  is the concentration in the chamber, Q is the flow rate through the chamber (40 lpm), and V the chamber volume (10 000 L), Y are all chemical losses (for  $\text{NO}_3$ , reactions with VOC,  $\text{RO}_2$ , and  $\text{NO}_2$ ; for VOC, only reaction with  $\text{NO}_3$ ), Z are all chemical sources ( $\text{N}_2\text{O}_5$  decomposition for  $\text{NO}_3$ ; none for VOC), and  $k_{\text{wall},X}$  is the rate of loss of X to chamber walls. The complete set of reactions and rate constants used are described in the SI Figure S4 and Table S2. The cumulative  $\Delta\text{VOC}$  is obtained by summing cumulative reacted VOC in this model.

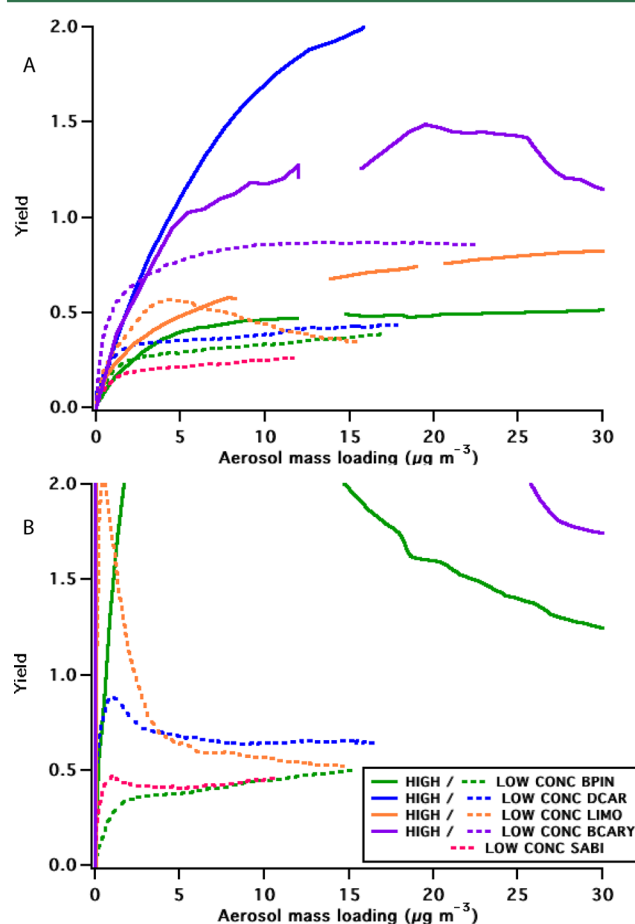
This method is superior in its chemical complexity, explicitly including  $\text{RO}_2 + \text{NO}_3$ ,  $\text{RO}_2 + \text{RO}_2$ , and  $\text{RO}_2 + \text{NO}_2$  reactions after the initial  $\text{NO}_3 + \text{VOC} \rightarrow \text{RO}_2$ . However, because these reaction rates are poorly known for monoterpene nitrate- $\text{RO}_2$ , this introduces some uncertainty. Further, since we are no longer constrained by  $\text{NO}_3$  data, we must invoke wall losses for  $\text{NO}_3$  and  $\text{N}_2\text{O}_5$ . In order to run this model consistently across experiments and with the minimum number of arbitrarily tunable variables, we “spun up” the model with continuous  $\text{N}_2\text{O}_5$  addition to the initial conditions of each chamber experiment, determining  $\text{NO}_3$  and  $\text{N}_2\text{O}_5$  wall loss rate constants that best fit all available data. Each experiment then proceeds by continuous addition of VOC and  $\text{N}_2\text{O}_5$  at the known injection rates, which we model free-running, with no tuning to match observed  $\text{NO}_3$  decay. This model assumes a well-mixed chamber at all times, so we interpret discrepancies with observed  $\text{NO}_3$  decay to be due to mixing inhomogeneity or uncertainties in  $\text{RO}_2$  rate constants (see SI Figure S5 for an exemplary model fit of  $\text{NO}_3$  decay). Because this method incorporates additional losses of  $\text{NO}_3$ , resulting VOC consumption is slower, leading to higher apparent SOA yields.

Both methods of  $\Delta\text{VOC}$  determination ignore reaction with the second double bonds in limonene or  $\beta$ -caryophyllene,

which would deplete  $\text{NO}_3$  further and enhance SOA yields.<sup>30</sup> The rate of  $\text{NO}_3$  reaction at the second, exocyclic double bond is predicted to be 30-fold slower in the case of limonene, so this is not expected to be a large effect,<sup>17</sup> although it may be more competitive in the low  $\beta$ -caryophyllene experiment, where  $\text{N}_2\text{O}_5$  concentration greatly exceeded BVOC.

Each wall-loss corrected SMPS size distribution in the time series was converted to  $\Delta M$  as follows. First, we iteratively applied the size-dependent wall loss corrections to the full SMPS time series to derive a complete time series of the size distributions that would have been observed had no particles been lost the walls. Then, number concentration data from each size bin were converted to SOA mass concentration in  $\mu\text{g m}^{-3}$  using the mean bin diameter and assumed organic aerosol density of  $1.4 \text{ g cm}^{-3}$ .<sup>7</sup> Since no seed particles were used, all observed aerosol is organic, and the wall-loss corrected aerosol mass gives cumulative  $\Delta M$ . The ratio of this  $\Delta M$  to cumulative VOC consumed is the unitless mass yield, ( $Y = \Delta M / \Delta\text{VOC}$ ).

We observe differences between high and low concentration mass yield curves (Figure 3) that vary with BVOC, suggesting



**Figure 3.** Yield curves for high and low  $\text{NO}_3 + \text{BVOC}$  SOA experiments, using (a) observed  $\text{NO}_3$  decay, or (b) complete kinetics model to determine reacted BVOC. BVOC labeling is as in Figure 2.

that the experiments differ in more than simply the total aerosol mass loading. We note from the kinetics modeling that in all experiments, the ratio of  $\text{RO}_2\text{—NO}_3$  to  $\text{RO}_2\text{—RO}_2$  rates is highest initially and decreases, in the case of the low concentration experiments crossing over so that after several hours of reaction,  $\text{RO}_2\text{—RO}_2$  reactions are predicted to be

dominant, while in the high concentration experiments, RO<sub>2</sub>—NO<sub>3</sub> reactions dominate throughout. Because these rate constants are quite uncertain and not known for specific BVOC precursors, we simply conclude that some of the explanation of the higher yields for the high concentration experiments may lie in the differences in RO<sub>2</sub> radical fate. We note here again an important difference between these experiments and what would be observed in the atmosphere: HO<sub>2</sub> radicals were nonexistent in these chamber experiments, but are expected to be a significant reaction partner for RO<sub>2</sub> in the real atmosphere.

In all low concentration experiments, due to the slower reaction, the ΔVOC is better constrained for longer periods, and the mixing time scale is faster relative to reactions, resulting in yield curves with less uncertainty but with the same inter-BVOC trend observed at both concentration conditions. Due to these differences, subsequent discussion will focus only on these low concentration experiments. As is apparent in Figure 3, the high concentration experiments (and early stages of some low concentration experiments) produce unrealistically high yields, especially in the full kinetics model, suggesting that in these cases, reactions were faster than chamber mixing and that this box model may be inaccurate. According to absorptive partitioning theory,<sup>31–34</sup> yields should increase with aerosol mass loading, assuming a constant product distribution over time. If, however, the product distribution is changing over time as RO<sub>2</sub> reactive fate changes, then mass yields could appear to decrease as an artifact of a shift from early high molecular weight products to later lower molecular weight products. As a result of these uncertainties at early times, we do not fit the mass-dependent yield for these experiments, but rather report yields at 10 μg m<sup>-3</sup> for each low concentration experiment (Table 3). We choose 10 μg m<sup>-3</sup> because it is sufficiently late in the low concentration experiments (generally ~1.5 h) that irregularities in the yield curve have subsided.

**Mechanistic Hypotheses for Observed Differences in SOA Formation.** Although we observe different yields for the high and low concentration experiments for each BVOC

**Table 3. Aerosol Yields (=ΔM/ΔVOC) Observed at 10 μg m<sup>-3</sup> in the Low-Concentration NO<sub>3</sub> Oxidation Experiments, Using Two Alternative Methods of Determining ΔVOC to Bracket Uncertainties Due to Mixing and RO<sub>2</sub> Fate<sup>a</sup>**

BVOC	yield @ 10 μg m <sup>-3</sup> ΔVOC calculated from NO <sub>3</sub> loss alone (Method 1)	yield @ 10 μg m <sup>-3</sup> ΔVOC calculated by complete kinetics model with RO <sub>2</sub> reactions (Method 2)
β-pinene	0.33	0.44
Δ-3-carene	0.38	0.65
limonene	0.44	0.57
sabinene	0.25	0.45
β-caryophyllene	0.86	n/a <sup>b</sup>
α-pinene	0	0

<sup>a</sup>Method 1 represents a lower limit yield, since no other RO<sub>2</sub> reactions are included, while Method 2's uncertainty lies in the uncertainty of rate constants (see SI discussion around Figures S3–S6). <sup>b</sup>For β-caryophyllene, extremely rapid modeled RO<sub>2</sub> + NO<sub>3</sub> reactions result in predicted very slow BVOC consumption and thus unreasonably high yields. This may be indicative of the rate constants being different for sesquiterpene RO<sub>2</sub>. Because the predicted relative excess of RO<sub>2</sub> + NO<sub>3</sub> reactions is greatest for β-caryophyllene, it is likely that the reported yield from the first method (which neglects these pathways entirely) is an underestimate.

(Figure 3), the inter-BVOC trend of volume growth observed at the higher oxidant + BVOC concentrations follows a similar pattern seen in the lower concentration experiments (Figure 2). This suggests that the mechanism responsible for this behavior corresponds to the chemical nature of each individual BVOC. Among the monoterpenes with one double bond, Δ-3-carene's initial volume growth (Figure 2b) exceeds both β-pinene and sabinene for both high and low concentration experiments, not matching the trend in reaction rate constants (sabinene's rate of reaction with NO<sub>3</sub> is faster than Δ-3-carene's). Sabinene was included in these experiments to assess whether the instability of the three-membered ring was responsible for Δ-3-carene's high SOA yield; sabinene's relatively low yield suggests that this is not the explanatory difference.

A possible mechanism for the observed SOA formation trends emerges when examining the structural differences of these monoterpenes. The NO<sub>3</sub> radical preferentially adds to the double bond in such a way as to make the more substituted alkyl radical, which will quickly react with O<sub>2</sub> to become an alkyl peroxy radical, and then upon reaction with another NO<sub>3</sub> or RO<sub>2</sub>, will produce the alkoxy radical (mechanism shown the SI Figure S6). In the subsequent reaction forming a ketone, the bond that is broken can be predicted via structure activity relationships (e.g., Table 3 in Vereecken and Peeters,<sup>35</sup> shown in black in SI Figure S6). Because a β-alkyl substitution destabilizes the adjacent bond more than a β-nitrate, the ketones predicted to be formed from breaking the weakest C—C bond in α-pinene and Δ-3-carene are structurally very different. In α-pinene, the predicted product has the radical at the opposite end of the molecule from a terminal nitrate. In Δ-3-carene, limonene, and β-caryophyllene, the radical ends up adjacent to the nitrate group, a structure which will stabilize the radical, possibly making it more likely to undergo subsequent radical-initiated oligomer formation rather than decomposition, and explaining high organonitrate and aerosol yields. However, we note that the predicted pathway of α-pinene bond scission is inconsistent with the observed dominant product channel of pinonaldehyde (Table 1), which is consistent with our observed low nitrate yield from α-pinene and potentially explanatory of low aerosol yield. Additional observations of NO<sub>y</sub> balance relevant to the understanding this subsequent radical chemistry are discussed below.

The importance of the nitrate radical in initiating rapid SOA growth was tested by conducting another limonene experiment (Expt. 8), where NO<sub>3</sub> was generated by O<sub>3</sub> + NO<sub>2</sub> (more typical in the atmosphere) rather than N<sub>2</sub>O<sub>5</sub> dissociation. In this case, limonene was oxidized by a mixture of O<sub>3</sub> and NO<sub>3</sub>, rather than only the NO<sub>3</sub> radical. No OH scrubber was used, so OH recycling may have also contributed to oxidative chemistry in this case, given the 86% OH yield from ozonolysis of limonene.<sup>36</sup> We observed in this mixed-oxidant case both a 3-fold lower peak number concentration and slower initial volume growth than in the case of NO<sub>3</sub> alone at nominally the same initial oxidant concentration ([N<sub>2</sub>O<sub>5</sub>]<sub>i</sub> = 10 ppb vs [O<sub>3</sub>]<sub>i</sub> = 12 ppb and [NO<sub>2</sub>]<sub>i</sub> = 6.3 ppb, in both cases with [limonene]<sub>i</sub> = 10 ppb). These nominally similar concentrations do not imply similar rates—the rate constant of O<sub>3</sub> + limonene is 2.1 × 10<sup>-16</sup> cm<sup>3</sup> molec<sup>-1</sup> s<sup>-1</sup>,<sup>6</sup> in contrast to NO<sub>3</sub> + limonene's 1.22 × 10<sup>-11</sup> cm<sup>3</sup> molec<sup>-1</sup> s<sup>-1</sup>.<sup>21</sup> In the observed volume growth curves, later in the experiment the total SOA volume in the mixed-oxidant case “catches up” to the NO<sub>3</sub>-only experiment. Hence, limonene ozonolysis and nitrate oxidation produce similar eventual SOA mass yields at comparable initial concentrations,

Table 4. Observed Organic Nitrate and Gas/Aerosol Partitioning, and Nitrogen Balance<sup>a</sup>

BVOC	molar organic nitrate yield ( $\Delta[\text{ANs} + \text{PNs}]/\Delta[\text{VOC}]$ )	fraction of organonitrates in aerosol phase ( $\Delta[\text{ANs} + \text{PNs}]_{\text{aero}}/\Delta[\text{ANs} + \text{PNs}]$ )	organonitrate fraction of total aerosol mass ( $M_{\text{ANs,aero}}/M_{\text{o}}$ )	N-balance: $\text{NO}_2$ release ( $\Delta[\text{NO}_2]/-\Delta[\text{N}_2\text{O}_5]$ )	N-balance: organonitrate formation ( $\Delta[\text{ANs} + \text{PNs}]/-\Delta[\text{N}_2\text{O}_5]$ )
$\beta$ -pinene	0.22	0.76	0.56	1.04 1.15	0.08 0.23
$\Delta$ -3-carene	0.77	0.50	0.56	1.14	0.22
limonene	0.54	0.83	0.82	0.76 0.96	0.31 0.41
$\beta$ -caryophyllene	n/a	1	0.80	n/a <sup>b</sup>	n/a <sup>b</sup>
$\alpha$ -pinene	0.10	0	0	1.54 1.75	0.03 0.10

<sup>a</sup>BVOC-based molar organic nitrate yield, aerosol fraction of organonitrates, and organonitrate fraction of total aerosol mass are all evaluated at 2 h after chamber experiment initiation (data are all from the high-concentration experiments, when the TD-LIF instrument was available);  $\text{N}_2\text{O}_5$ -based  $\text{NO}_2$  and ANs + PNs production are evaluated at 30 min after chamber experiment initiation. For  $\beta$ -pinene, limonene, and  $\alpha$ -pinene,  $\text{NO}_3$  decays slowly enough that this N balance analysis can be reliably repeated at 2 h. These are the numbers reported in italics. <sup>b</sup>Several parameters are not available for  $\beta$ -caryophyllene, because the  $\text{N}_2\text{O}_5$  decay was very rapid and not well-characterized.

but  $\text{NO}_3$ -initiated chemistry appears more effective at nucleating new particles. This is consistent with the initial nitrate oxidation products being higher mass and lower-volatility than their ozone and OH counterparts under dry conditions, but both reactions producing substantial yields of products of intermediate volatility that begin to condense as aerosol loading increases.

**The Exceptional BVOC:  $\alpha$ -Pinene Forms No Aerosol upon  $\text{NO}_3$  Oxidation.** The wide range of observed SOA yields from  $\text{NO}_3$  oxidation of various BVOC is provocative, but perhaps most surprising is the observation that  $\alpha$ -pinene reacting with  $\text{NO}_3$  produced *no* SOA. Because  $\alpha$ -pinene is frequently used as a model monoterpene in chamber studies, this exceptional behavior relative to all other monoterpenes tested is particularly important. We seek an explanation in the initial oxidation steps of this reaction, and note that  $\alpha$ -pinene could be expected to produce an internal nitrate rather than a terminal nitrate, such as would be expected in  $\beta$ -pinene,  $\Delta$ -3-carene, or sabinene (see SI Figure S6). It has been shown that terminal functional groups result in lower vapor pressure than internal, but this observation would seem to be a very extreme manifestation of that trend. We note that the  $\text{NO}_3$  +  $\alpha$ -pinene reaction forms little organonitrate (Table 4), and this organonitrate was not observed to partition to the aerosol phase. Most of the  $\text{NO}_3$  returns to the gas phase as  $\text{NO}_2$ , consistent with previous observations that  $\alpha$ -pinene chemistry instead produces the diketone pinonaldehyde (SI Figure S6, red pathway), which is expected to be more volatile than the organonitrate alternatives.<sup>37</sup>

**Organonitrate Yields for Various BVOC.** An example of observed gas- and aerosol-phase organonitrate production is shown in the SI (Figure S7). The nitrogen balance of all high concentration experiments, for which organonitrate measurements were available, are reported in Table 4 and described below.

We determined molar organonitrate yields from BVOC ( $\Delta[\text{ANs} + \text{PNs}]/\Delta[\text{VOC}]$  in ppb units, using “method 1”  $\Delta\text{VOC}$ ), fraction of total organonitrates in the aerosol phase ( $\Delta[\text{ANs} + \text{PNs}]_{\text{aero}}/\Delta[\text{ANs} + \text{PNs}]$  in ppb units), and the fraction of total aerosol mass that is due to organonitrates ( $M_{\text{ANs,aero}}/M_{\text{o}}$  in  $\mu\text{g m}^{-3}$ ), all evaluated at 2 h into the experiment to capture longer-term trends. The calculation of total organonitrates requires subtraction from the total TD-LIF ANs + PNs signal the fraction of chamber  $\text{N}_2\text{O}_5$  that is detected in this channel (empirically determined by comparison to CRDS to be 11%), and if dinitrates are present, then they would appear as 2 nitrates. The calculation of total and

organonitrate aerosol mass concentrations require (a) the conversion of gas phase organonitrates to mass concentration, using assumed values for the average organonitrate molecular weight; and (b) assumptions about average density of SMPS-measured aerosol and the average organonitrate molecular weight to convert mixing ratios to mass concentrations for comparison to SMPS-derived total aerosol mass concentration. We assume an aerosol density of  $1.4 \text{ g cm}^{-3}$ , and that ANs+PNs are on average hydroxynitrates of molecular weight  $214 \text{ g mol}^{-1}$  ( $286 \text{ g mol}^{-1}$  for  $\beta$ -caryophyllene), hence at the experiments’ ambient pressure ( $P_{\text{atm}} = 0.8 \text{ atm}$ ),  $1 \text{ ppb} = 7.0 \mu\text{g m}^{-3}$  ( $9.4 \mu\text{g m}^{-3}$  for  $\beta$ -caryophyllene).

In addition, we investigate the observed nitrogen balance in these high-concentration experiments by comparing molar  $\text{NO}_2$  release from  $\text{N}_2\text{O}_5$  ( $\Delta[\text{NO}_2]/-\Delta[\text{N}_2\text{O}_5]$  in ppb units) and organonitrate formation ( $\Delta[\text{ANs} + \text{PNs}]/-\Delta[\text{N}_2\text{O}_5]$  in ppb units) to assess closure. For these measurements, we use data 30 min after initiation of the chamber experiment, to ensure that  $-\Delta[\text{N}_2\text{O}_5]$  is still well-constrained.

Several key similarities and differences among BVOC emerge in this comparison. First, we note that in all experiments except  $\alpha$ -pinene, organonitrates constitute a substantial fraction of total aerosol mass (greater than 60%), and a large fraction (50–100%) of observed organonitrates are in the aerosol phase. This indicates that the organonitrates produced in  $\text{NO}_3$  + monoterpene or sesquiterpene reactions tend to be of low volatility, with the largest aerosol-phase fraction (lowest volatility) nitrate arising from the oxidation of the single sesquiterpene tested,  $\beta$ -caryophyllene. This is consistent with expectation based on the sesquiterpene’s larger molecular weight.

There is a correlation between organic nitrate molar yields and aerosol mass yields (see Table 3), with  $\alpha$ -pinene’s low organonitrate yield corresponding to no SOA production, while  $\Delta$ -3-carene and limonene have both larger organonitrate yields and SOA yields. However, the correlation is not strong (consistent with previous observations by Hallquist et al.<sup>12</sup>). For example,  $\beta$ -caryophyllene does not fit the trend: despite the largest SOA yield, it has the second-lowest organonitrate yield. We note that the  $\beta$ -caryophyllene experiment differed from others in terms of initial conditions, with  $[\text{BVOC}] \gg [\text{N}_2\text{O}_5]$ , which may explain this discrepancy. In addition, as a sesquiterpene ( $\text{C}_{15}$ ),  $\beta$ -caryophyllene starts at a lower volatility than other precursors, which may also affect the degree to which non-nitrate products might also partition to the aerosol phase. Its larger size also may affect vapor-phase wall losses, which are observed to be faster for larger carbon number



molecules,<sup>29</sup> potentially depressing apparent SOA yield relative to the monoterpenes ( $C_{10}$ ). All of the organonitrates produced from  $\beta$ -caryophyllene are observed in the condensed phase.

The nitrogen balance provides additional indications of differences among precursors (a schematic of N balance is shown in SI Figure S8).  $NO_2$  release greater than 1 indicates that some of the  $NO_3$  + BVOC products fragment to rerelease  $NO_2$  (the first  $NO_2$  molar equivalent comes from the initial dissociation of  $N_2O_5$ ). This  $NO_2$  release is greatest for  $\alpha$ -pinene, which does not produce SOA, suggesting that the non-nitrate/fragmentation products are less condensable.

In all cases, the total N balance after 30 min reaction time sums to less than two total, the total that would be expected for closure (as there are two molar equivalents of N in each  $N_2O_5$  precursor upon which the N balance is based). This shortfall could be due to faster wall losses of organonitrates, or to the production of  $NO_y$  species not measured, most notably,  $HNO_3$ . Previous chamber studies of  $NO_3$  +  $\beta$ -pinene and limonene have demonstrated substantial  $HNO_3$  formation;<sup>16,17</sup> in these experiments,  $\beta$ -pinene and limonene exhibit the least total N closure. Furthermore, as can be seen in the three available time-dependent N balances, the N shortfall is largest at the beginning of the experiments, when  $[NO_3]$  most dramatically exceeds  $[BVOC]$ , resulting in the greater likelihood of other later-generation  $NO_3$  reactions such as H abstraction to produce  $HNO_3$ .

In summary, SOA yield is greater for the sesquiterpene than monoterpenes, and within the monoterpenes is roughly correlated with the production of low-volatility nitrates. SOA formation is hindered by excessive fragmentation and  $NO_2$  release (as observed in  $\alpha$ -pinene).

## ■ IMPLICATIONS FOR MODELING SOA FORMATION

The observed SOA yields range widely, from 0 to 86% at  $10 \mu\text{g m}^{-3}$  background aerosol, but display consistent trends across experiments at different initial concentrations, suggesting that differences are a function of BVOC precursor molecular structure. In past global modeling efforts, a single yield has been applied for aggregate  $NO_3$  + terpenes, for example, Pye et al.<sup>38</sup> use a parametrization based on Griffin et al.,<sup>39</sup> which gives SOA yield at  $10 \mu\text{g m}^{-3}$  of 26% and find that adding in  $NO_3$  oxidation of terpenes increased global SOA production by 3 Tg/yr. If we apply our speciated yields to the case of a Rocky Mountain front range forest, where the mix of BVOC is 1:1:1  $\alpha$ -pinene/ $\beta$ -pinene/ $\Delta$ -carene,<sup>40</sup> then we obtain a BVOC-weighted yield of 24%–36% (range based on yields from two  $\Delta$ VOC methods), which falls in line with the Pye et al. aggregate model because high yield from some BVOC outweighs zero yield from  $\alpha$ -pinene. However, in parts of the country where  $\alpha$ -pinene is dominant among terpenes (coastal Pacific northwest, deep south<sup>41</sup>), this aggregate number may overestimate  $NO_3$ -initiated SOA production, while areas where other terpenes dominate (central plains, northeastern U.S.), the aggregate may underestimate  $NO_3$ -initiated SOA production.

An additional factor to note when comparing to the real atmosphere is that the relative importance of  $NO_3$  oxidation vs  $O_3$  varies among these molecules: at 10 ppt  $NO_3$  and 30 ppb  $O_3$ , nitrate reaction rates proceed 20–90 times faster than ozonolysis for all the monoterpenes, but for  $\beta$ -caryophyllene, only half as fast.<sup>6</sup> Thus,  $\beta$ -caryophyllene will be relatively less likely to be oxidized by  $NO_3$ . A true assessment of the role of these reactions requires more detailed regional modeling that can capture the spatial overlap of speciated natural BVOC

emissions with anthropogenic  $NO_x$  plumes and resulting oxidation chemistry.

## ■ ASSOCIATED CONTENT

### Supporting Information

NCAR chamber facility description; schematic of the NCAR environmental chamber facility (Figure S1); instruments used in chamber experiments (Table S1); wall loss analysis; wall loss characterization for the NCAR chamber (Figure S2); determination of  $\Delta$ VOC; derivation of cumulative  $\beta$ -pinene FVOC time series (Figure S3); kinetics box model mechanism (Figure S4); rate constants used in the above model (Table S2); wall loss characterization for the NCAR chamber; exemplary model run for  $\beta$ -pinene high concentration experiment (Figure S5); molecular structural effects on alkoxy radical fate; proposed initial steps of nitrate oxidation (Figure S6); Full time series of organonitrate measurements (Figure S7); schematic of nitrogen balance (Figure S8); and additional references. This material is available free of charge via the Internet at <http://pubs.acs.org/>.

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### Notes

The authors declare no competing financial interest.

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