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1 Enhancement of Boiling with Scalable Sandblasted Surfaces

2

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16 KEYWORDS

17 Pool Boiling, Power Plant, Critical Heat Flux, Heat Transfer Coefficient, Surface Engineering

18

1 Abstract

2 Surface engineering has been leveraged by researchers to enhance boiling heat transfer
3 performance, with benefits ranging from improved thermal management to more efficient power
4 generation. While engineered surfaces fabricated using cleanroom processes have shown
5 promising boiling results, scalable methods for surface engineering are still limited despite most
6 real-world industry-scale applications involving large boiling areas. In this work, we investigate
7 the use of sandblasting as a scalable surface engineering technique for enhancement of pool
8 boiling heat transfer. We vary the size of an abrasive Al_2O_3 sandblasting media (25, 50, 100, and
9 $150\ \mu m$) and quantify its effects on silicon surface conditions and boiling characteristics. The
10 surface morphology and capillary wicking performance are characterized by optical profilometry
11 and capillary-rise tests, respectively. Pool boiling results and surface characterization reveal that
12 surface roughness and volumetric wicking rate increase with the abrasive size, which results in
13 improvements in critical heat flux and heat transfer coefficient of up to 192.6% and 434.3%
14 compared to a smooth silicon surface, respectively. The significant enhancement achieved with
15 sandblasted surfaces indicates that sandblasting is a promising option for improving boiling
16 performance in industry-scale applications.

17

18 1. Introduction

19 Boiling is a vital process in industrial applications, particularly where steam generation is
20 required, such as power plants, water purification, food and chemical processing, and
21 sterilization. For example, the majority of electrical power is generated in power plants that
22 operate using steam cycles, in which various resources (e.g., natural gas, coal, nuclear energy,

1 biomass, and geothermal energy) are used to produce steam that turns turbines attached to
2 generators.¹ The enhancement of boiling performance by engineering boiling surfaces has
3 therefore been studied extensively due to its practical importance across industries. Particularly,
4 cleanroom-processed micro- and nanostructures have been exploited for systematic studies of
5 structural effects on boiling heat transfer enhancement.²⁻¹⁰ For example, surfaces with rough,
6 permeable structures such as micropillars and nanowires have enabled significant enhancements
7 in the operational limit of nucleate boiling, i.e., the critical heat flux (CHF).^{2-4, 7-8} The CHF
8 enhancement is of particular interest for the nuclear reactor safety. When an applied heat flux
9 exceeds the CHF, an instantaneous formation of vapor films over the surface drastically increase
10 the thermal resistance, which leads to thermal runaway and a crucial failure of a boiling system.
11 Nucleation-engineered surfaces such as microcavity arrays, on the other hand, have shown
12 improved heat transfer efficiency as quantified by the heat transfer coefficient (HTC).⁵⁻⁶ Despite
13 the significant enhancement of pool boiling heat transfer, these cleanroom-processed surfaces are
14 not suitable for industry-scale applications due to the limited scalability. Solution-based surface
15 modifications such as surface oxidation, wet etching, synthesis of nanowires, and coatings of
16 nanoporous layers may provide better scalability than clean-room processes;¹¹⁻¹⁶ however, these
17 approaches are often limited to a specific material due to the need for chemical compatibility,
18 and nanomaterials have limited durability that may preclude use in industrial applications.¹⁷

19 In this work, we show a sandblasting process as a scalable surface structuring technique for the
20 enhancement of pool boiling heat transfer for industry-scale boiling applications. Sandblasting is
21 a purely physical bombardment process free of chemical compatibility constraints; therefore, it is
22 applicable to a wide range of materials including Zircaloy, which is commonly used in nuclear
23 reactors.¹⁸⁻²⁰ This simple process also allows sandblasting to be scaled up and widely used in

1 industry for surface roughening or smoothening.²¹ In fact, sandblasting has already been utilized
2 as a physical texturing method to study the effects of surface roughness on boiling heat transfer
3 in previous studies.²²⁻²⁹ The detailed analysis on the structural characteristics of sandblasted
4 surfaces and their effects on boiling heat transfer, however, are still lacking. In this work, we
5 investigated the mechanism of boiling enhancement of sandblasted surfaces by characterizing
6 their surface area ratios and capillary-driven wickabilities, which were found to be critical for
7 CHF during pool boiling.³⁰ The pool boiling experiments were conducted with water on silicon
8 surfaces sandblasted by aluminum oxide particles. We chose silicon as a test surface because of
9 its compatibility with our boiling setup as well as abundant pool boiling literature data on silicon
10 that we can compare with our results. The abrasive media size was varied (25, 50, 100, and 150
11 μm). Surface morphology and capillary-wicking performance were characterized by an optical
12 profilometer and capillary-rise tests. Surfaces sandblasted by larger abrasives (up to 150 μm)
13 exhibited higher roughness and volumetric wicking rate, resulting in greater enhancements of
14 CHF and HTC values.

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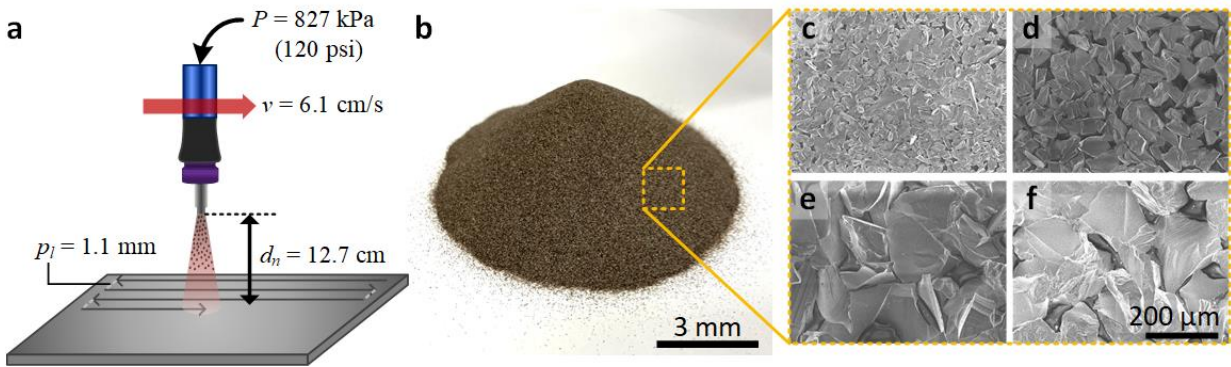
16 2. Preparation and characterization of sandblasted surfaces

17 2.1. Sandblasting process

18 Sandblasted boiling samples were prepared based on a 650- μm -thick silicon substrate with
19 thermally grown 1 μm SiO_2 layers on both sides. The top SiO_2 layer was completely etched by
20 reactive-ion etching to expose underlying silicon before sandblasting with a laboratory-scale
21 sandblaster (AccuFlo AF10 Standard Tank, Comco Inc.). A schematic of the sandblasting
22 process is shown in Figure 1a. The blasting nozzle was mounted on an XY linear stage and is

1 raster scanned over the surfaces with a constant line-pitch (p_l) of 1.1 mm and a sweeping speed
2 (v) of 6.1 cm/s, where its motion is controlled with a microcontroller (Arduino Uno). The nozzle-
3 to-sample distance (d_n) and blasting pressure (P) were fixed at 12.7 mm and 827 kPa (120 psi),
4 respectively. In order to create different structural features, Al_2O_3 abrasives with four different
5 nominal sizes (25, 50, 100, and 150 μm) were tested. Figure 1b shows a pile of Al_2O_3 abrasives,
6 where each abrasive has a blocky and sharp shape as shown in scanning electron microscope
7 (SEM) images (Figure 1c – 1f). The nominal size of abrasives was calculated as an equivalent
8 diameter sphere by laser diffraction patterns (HELOS, Sympatec).

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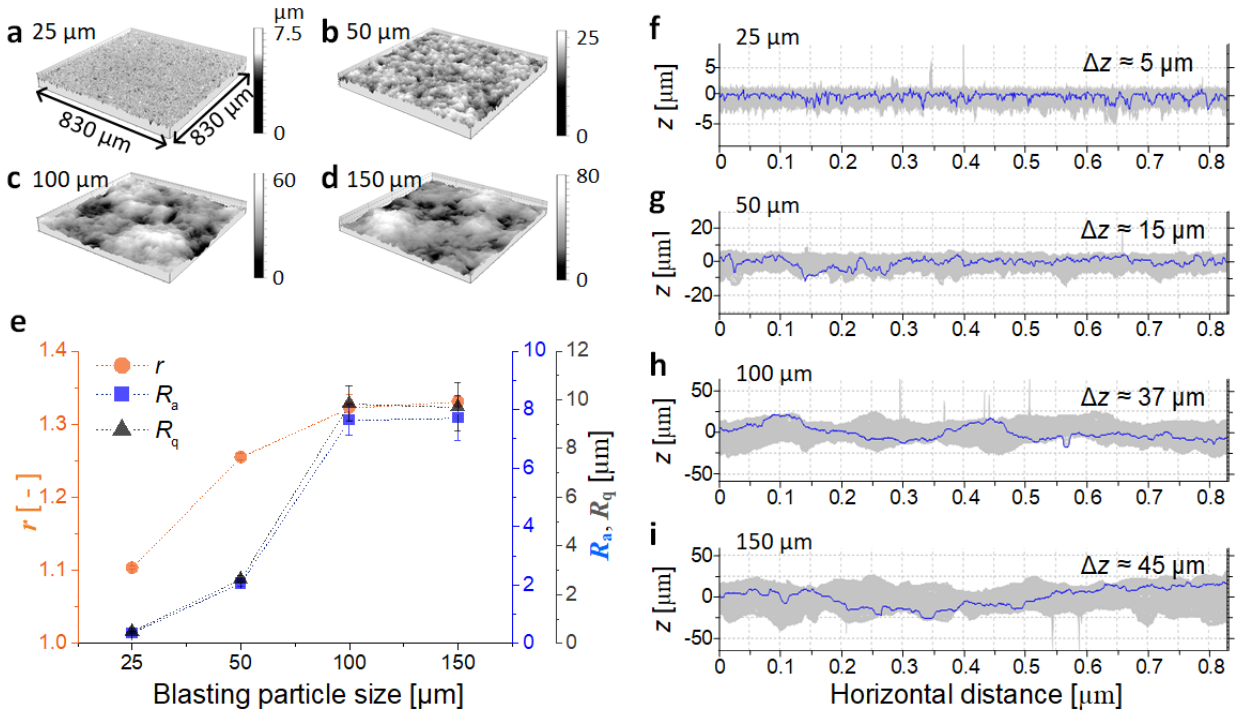
11 **Figure 1.** Sandblasting process and abrasives. (a) A schematic of the sandblasting process.
12 Sandblasting pressure (P), sweeping speed (v), line-pitch (p_l), and nozzle-to-sample distance (d_n)
13 were fixed while changing the Al_2O_3 abrasive size from 25 to 150 μm . (b) Optical image of a
14 pile of sandblasting abrasives. (c – f) Scanning electron microscope images of sandblasting
15 abrasives of 25, 50, 100, and 150 μm , respectively.

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17 **2.2. Morphology of sandblasted surfaces**

1 The surface structures created by the sandblasting process were analyzed quantitatively by an
2 optical profilometer (Non-contact 3D profiler CCI, Taylor Hobson) as shown in Figure 2. Figure
3 2a–d show the three-dimensional profile images of surfaces sandblasted by 25, 50, 100, and
4 150 μm , respectively. The roughness (r), defined as the ratio of actual surface area to projected
5 area, has been proposed as a critical surface feature determining CHF values in previous works.²
6 ³¹ Figure 2e shows the change in r along with the arithmetic-mean roughness (R_a) and root-mean-
7 square roughness (R_q) as functions of blasting abrasive size. We measured the roughness
8 parameters at ten different randomly selected positions on each surface. The average and
9 standard deviation values were used as data points and error bars, respectively. All three
10 parameters increased noticeably as abrasive size increased from 25 to 100 μm , while the
11 differences of parameters between the cases of 100 and 150 μm abrasives were insignificant and
12 within error bar ranges. The plots of surface profiles in a horizontal direction are shown in
13 Figure 2f–h. Grey regions represent the overlapped profiles over the other horizontal direction,
14 from which the peak-to-valley amplitude Δz was characterized. The peak-to-valley amplitude
15 increased with the abrasive size. A blue line in each plot shows a typical profile at a specific
16 position in the other horizontal direction. SEM and energy-dispersive X-ray (EDS) images of
17 sandblasted surfaces are provided in Section I of the Supporting Information.

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Figure 2. Surface structures characterized by an optical profilometer. (a–d) Three-dimensional profiles of surfaces sandblasted by 25, 50, 100, and 150 μm, respectively. (e) Surface area ratio (r , orange circles), arithmetic-mean roughness (R_a , blue squares), and root-mean-square roughness (R_q , gray triangles) as functions of blasting abrasive size. Error bars represent the standard deviations of ten different measurements at random positions on each surface. (f–i) Profile plots in one of the horizontal directions of surfaces sandblasted by 25, 50, 100, and 150 μm, respectively. The blue line and grey region indicate a profile at a fixed position and the overlaps of all profiles in the perpendicular horizontal direction, respectively. The peak-to-valley amplitude Δz was characterized based on the grey region.

2.3. Wickability of sandblasted surfaces

1 In addition to surface roughness r , the surface wickability has been found to be a good indicator
 2 for pool boiling CHF enhancements.^{3-4, 32} To characterize the wickability of sandblasted surfaces,
 3 we performed capillary rise tests (Figure 3a). A sample was moved vertically toward the
 4 reservoir of water until it came in contact, resulting in upward capillary rise flow through the
 5 sandblasted surface. The propagation speed of the capillary rise was captured with a digital
 6 camera at 30 frames per second. Figure 3c shows the time-lapse images of propagating wicking
 7 front on the surface sandblasted by 150 μm abrasives as an example. Once the sample contacted
 8 the surface of water, a capillary meniscus formed (highlighted in white dashed lines) first, and
 9 liquid propagated (wicking front shown with yellow dashed lines) upward with the speed (u)
 10 associated with the balance between capillary pressure and viscous resistance. This liquid
 11 propagation through porous sandblasted structures can be described by Darcy's law (or the
 12 Brinkman equation, if viscous shearing is the dominant flow resistance compared to structural
 13 permeability) as

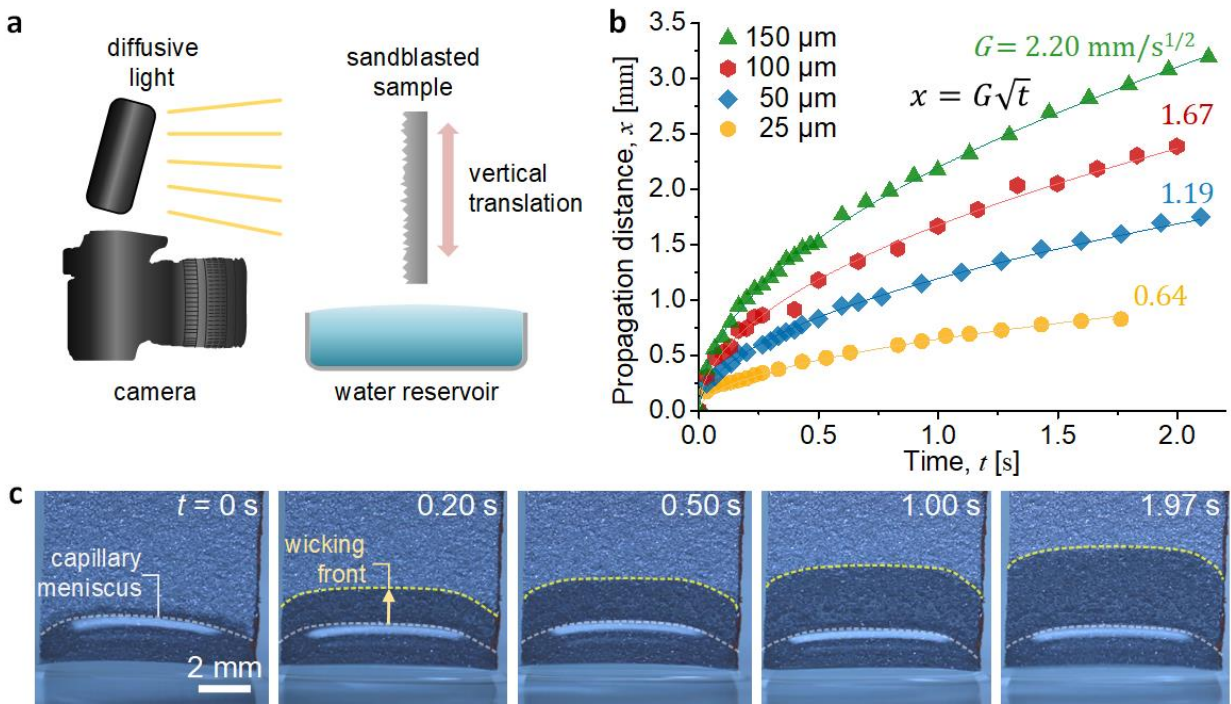
$$\frac{dx}{dt} = \frac{K_B \Delta P_{\text{cap}}}{\mu x}. \quad (1)$$

14
 15 Here x , t , and μ are the propagation distance, time, and dynamic viscosity of liquid. P_{cap} and K_B
 16 are the capillary pressure and effective permeability that structured surfaces exhibit. By solving
 17 the equation with initial condition $x(t = 0) = 0$, the propagation distance (x) can be expressed
 18 as a square root function of time (t) with a propagation coefficient G as a proportional
 19 coefficient, i.e.,

$$x = \sqrt{\frac{2P_{\text{cap}}K_B}{\mu} t} = G\sqrt{t}. \quad (2)$$

1 The measured propagation distances are shown in Figure 3b as a function of time along with
 2 fittings of square root function. Propagation coefficient G values derived from curve fitting
 3 (shown next to each curve) increased with the abrasive size, indicating a silicon surface
 4 sandblasted by larger abrasives (up to 150 μm) exhibited better surface wickability.

5



6

7 **Figure 3.** Surface wickability measurements of sandblasted surfaces. (a) Schematic of
 8 experimental setup for wickability measurement. A sandblasted surface is immersed vertically
 9 into the reservoir of water while a digital camera captures the speed of capillary rise at 30 frames
 10 per second. (b) The propagation distance (x) of capillary rise plotted as a function of time (t). The
 11 data points and lines represent experimental measurements and the fitting of square root
 12 functions, respectively. Propagation coefficient values (G) for each surface are shown next to the

1 corresponding case. (c) Time-lapse images show an example of the wicking front of water on the
2 surface sandblasted by 150 μm Al_2O_3 abrasives.

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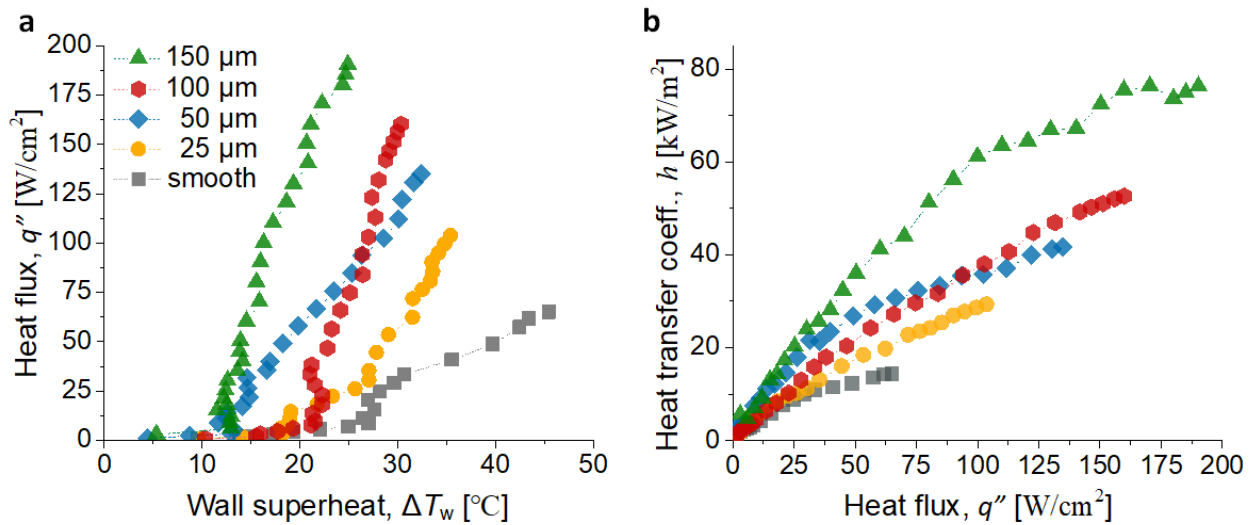
4 3. Pool boiling experiments

5 The pool boiling heat transfer characteristics of the sandblasted surfaces were characterized with
6 high-purity deionized water at saturated atmospheric conditions. On the back side of each boiling
7 sample, a 100-nm-thick serpentine Pt heater was patterned by a lift-off process to define the $10 \times$
8 10 mm^2 heating area, which also served as a resistive temperature detector for temperature
9 characterization. All test samples were cleaned by solvents (acetone, methanol, and isopropyl
10 alcohol) and argon plasma before boiling to remove organic contaminants.³⁴ The details of the
11 experimental setup and boiling heat transfer characterization methods are provided in Section II
12 of the Supporting Information.

13 Figure 4a shows pool boiling curves, i.e., heat flux (q'') as a function of wall superheat (ΔT_w), of
14 a smooth silicon surface and the sandblasted silicon surfaces. During the experiments, we
15 gradually increased the input heat flux by controlling the applied voltage up to the CHF point, at
16 which point thermal runaway occurred as indicated with an arrow in the plot. HTC, i.e., the slope
17 of a point from the origin on a boiling curve (by definition), is also plotted as a function of heat
18 flux in Figure 4b. All sandblasted surfaces demonstrated the increase of CHF and HTC as the
19 abrasive size increased. This result is similar to a previous work that has shown the monotonic
20 increase of CHF and HTC with the increase of arithmetic-mean roughness of copper surfaces
21 roughened by sandpapers.³⁵ CHF values monotonically increased from 65.1 W/cm^2 for the
22 smooth surface to 103.8 , 135.0 , 160.1 , and 190.5 W/cm^2 for 25 , 50 , 100 , and $150 \mu\text{m}$ abrasives,

1 respectively, resulting in up to 192.6% CHF enhancement. It is interesting to note that the
 2 surface sandblasted by 50 μm abrasives showed higher HTC values than the surface sandblasted
 3 by 100 μm abrasives at the early stage ($\Delta T_w < \sim 25^\circ\text{C}$), which may be associated with the
 4 optimal cavity size for the earlier onset of nucleate boiling.³⁶ A future parametric study including
 5 other sandblasting parameters may provide a detailed analysis about the early stage behavior of
 6 nucleate boiling. Nonetheless, the HTC values at CHF points showed a similar trend with CHF,
 7 i.e., an increase in HTC with increasing abrasive size. The maximum HTC value at CHF was
 8 14.3 kW/m^2 for the smooth silicon, which increased to 29.3, 41.6, 52.6, and 76.3 kW/m^2 for
 9 surfaces sandblasted by 25, 50, 100, and 150 μm abrasives, respectively, resulting in up to
 10 433.6% enhancement. The CHF and HTC enhancements achieved with sandblasted silicon
 11 surfaces were comparable to that of cleanroom-processed surfaces,^{2, 4-6} indicating promise for the
 12 use of a sandblasting process as a scalable surface engineering technique for boiling heat transfer
 13 enhancement.

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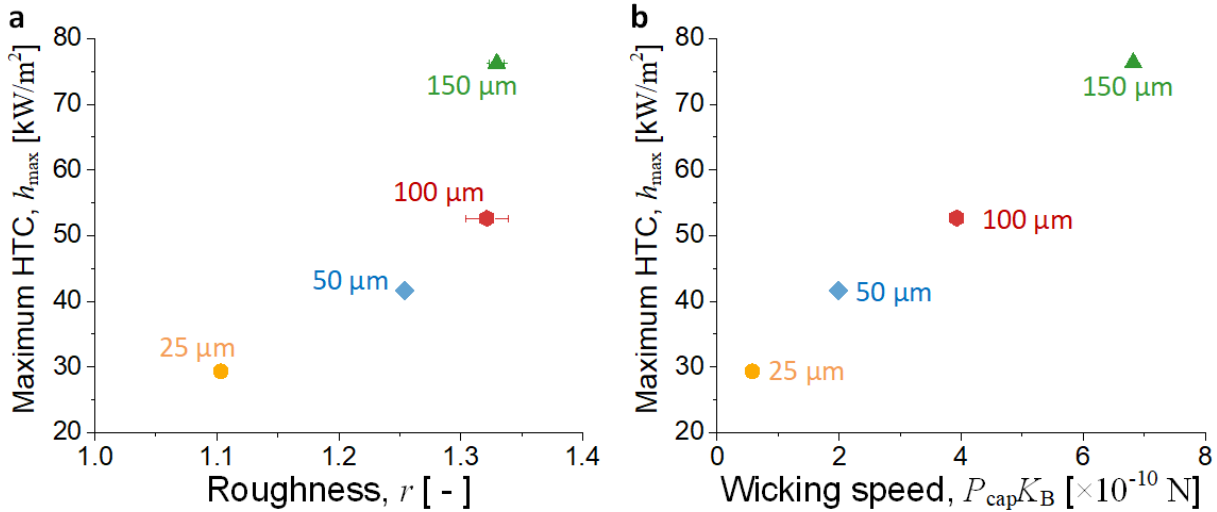
1 **Figure 4.** Pool boiling results of a smooth and sandblasted silicon surfaces. (a) Pool boiling
2 curves of water. (b) Heat transfer coefficient as a function of heat flux. The experimental
3 uncertainty was smaller than the marker size.

5 3.3. Mechanism of heat transfer coefficient enhancement

6 We attribute the HTC enhancement to the potential increase in the nucleation site density and
7 bubble departure frequency on sandblasted surfaces. As shown in surface profile images (Figure
8 2a – 2d), the sandblasting process created rough cavities, which could serve as nucleation sites.
9 In addition, capillary-driven wicking may accelerate bubble departure frequency by providing
10 the additional evaporation from thin wicked liquid. Considering high-pressure boiling
11 applications such as nuclear reactors, it is important to compare the relative contribution of
12 nucleation site density and bubble departure frequency to the HTC enhancement of sandblasted
13 surfaces. As pressure increases, the nucleation energy barrier decreases and thus, the structural
14 effects on nucleation site density can be diminished.³⁷ On this account, if the dominant
15 mechanism for the HTC enhancement is the increase of nucleation site density, sandblasted
16 surfaces may not enhance HTC effectively for high-pressure boiling applications. To determine
17 the dominant mechanism, between nucleation and frequency, we plotted the maximum HTC
18 values against roughness (r) and wicking speed ($P_{\text{cap}}K_B$) in Figure 5. The surface roughness can
19 be directly obtained from the optical profile measurement (Figure 2) and the wicking speed
20 $P_{\text{cap}}K_B$ can be obtained from the capillary-rise test (Figure 3) according to Darcy's law as
21 $P_{\text{cap}}K_B = \mu G^2/2$, where μ is the dynamic viscosity of water. The maximum HTC values
22 generally increase with both roughness and wicking speed. Samples blasted by 100 μm and 150

1 μm abrasives, however, show a stronger correlation of HTC values with wicking speed than
 2 roughness, indicating that the increased bubble departure frequency induced by wicking may
 3 play a more important role for the HTC enhancement.

4



5

6 **Figure 5.** Relationships of maximum heat transfer coefficient with (a) roughness (r) and (b)
 7 wicking speed ($P_{\text{cap}}K_B = \mu G^2 \Delta z / 2$) of sandblasted surfaces. Sandblasting abrasive size is
 8 indicated next to each data point.

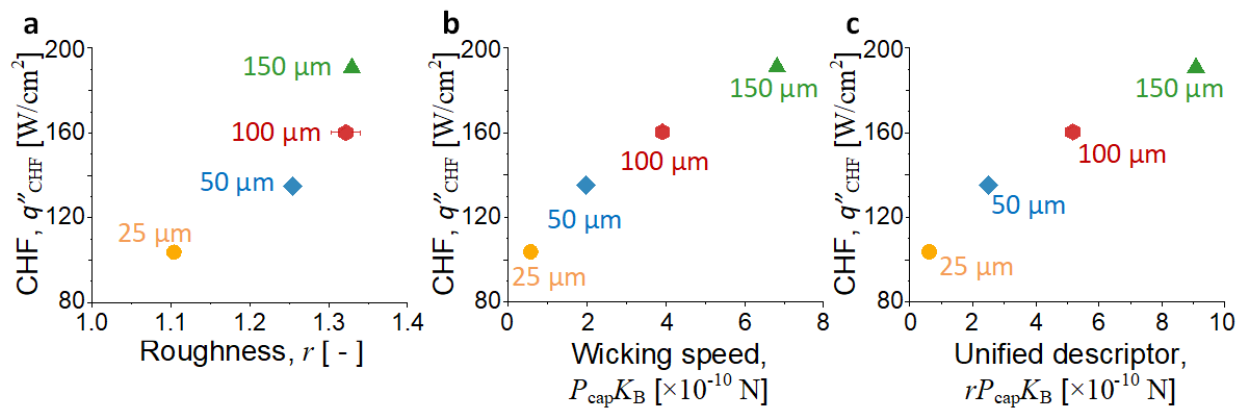
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10 3.4. Critical heat flux and surface characteristics

11 While past work has shown that roughness and wickability can enhance CHF enhancement, a
 12 recent study based on cleanroom-processed micropillar arrays showed that a single parameter
 13 such as roughness (r) or wicking speed ($P_{\text{cap}}K_B$) is not sufficient to describe the CHF
 14 enhancement of hemi-wicking surfaces. Instead, the unified descriptor ($\xi^n P_{\text{cap}}K_B h$) showed an

1 improved linear correlation with the CHF, where ζ , h , and n are thin film density, thickness of
 2 wick layer, and experimental fitting parameter, respectively.³⁰ This unified descriptor represents
 3 the combined effects of enhanced evaporation from the liquid thin films around structures and
 4 the delay of dry-out by capillary wicking. Here we rearrange the unified descriptor as
 5 $(\xi^n h)(P_{\text{cap}} K_B)$, where $\xi^n h$ can be approximated as surface roughness r . Accordingly, we
 6 approximate the unified descriptor as $rP_{\text{cap}} K_B$. In Figure 6, we compared the correlations of CHF
 7 with roughness (Figure 6a), wicking speed (Figure 6b), and the unified descriptor (Figure 6c).
 8 CHF values of sandblasted surfaces exhibited monotonic increases with all three parameters. The
 9 unified descriptor, however, showed the best correlation with the CHF among the three
 10 parameters (Figure 6c), which is consistent with the previous study with micropillars.³⁰ Note that
 11 sandblasted surfaces have artificial nucleation sites such as cavities as opposed to micropillar
 12 arrays, which can exhibit more complex CHF enhancement mechanisms associated with the
 13 increased nucleation site density.⁶ Nonetheless, the consistent linear correlation of CHF values of
 14 sandblasted surfaces with the unified descriptor suggests that sandblasted surfaces can be
 15 optimized for the CHF by controlling the unified descriptor in future work.

16



17

1 **Figure 6.** Relationships of critical heat flux with (a) roughness (r), (b) wicking speed ($P_{\text{cap}}K_B =$
2 $\mu G^2 \Delta z / 2$), and (c) the unified descriptor ($rP_{\text{cap}}K_B$) of sandblasted surfaces. Sandblasting
3 abrasive size is indicated next to each data point.

4

5 4. Conclusions

6 In this work, we showed that a sandblasting process is promising as a surface engineering
7 technique for enhancement of pool boiling heat transfer in industry-scale applications. We
8 fabricated sandblasted silicon surfaces using Al_2O_3 abrasives with four different sizes, i.e., 25,
9 50, 100, and 150 μm . The morphology of the sandblasted surfaces was quantitatively
10 characterized using an optical profilometer; all three measures of roughness (r , R_a , and R_q)
11 increased noticeably as abrasive size increased from 25 to 100 μm , while the difference of
12 roughness parameters between the 100 and 150 μm cases is marginal. Surface wickability was
13 characterized as a propagation coefficient of one-dimensional capillary flow, and showed
14 increasing trend of surface wickability with increasing abrasive size. Pool boiling performance of
15 sandblasted surfaces was subsequently characterized with high-purity deionized water at
16 saturated atmospheric conditions. Sandblasted surfaces demonstrated significant CHF and HTC
17 enhancements compared to a smooth surface. The highest enhancement was achieved with the
18 surface sandblasted by 150 μm abrasives, where CHF and HTC were enhanced up to 192.6% and
19 433.6%, respectively. The CHF enhancement of sandblasted surfaces showed a stronger
20 correlation with the unified descriptor, compared to that with roughness and wicking speed
21 alone.³² In this work, we used silicon as a base material, of which the heat transfer enhancement
22 is limited to specific applications, such as electronics cooling. To further demonstrate the

1 applicability of sandblasting for heat transfer enhancements of nuclear power plants,
2 investigations of durability and boiling performance under high pressure with commercial
3 materials for nuclear reactors such as Zircaloy is needed, which will be pursued in future work.
4 Furthermore, we expect that further enhancements can be achieved by investigating an optimal
5 sandblasting condition. For example, we tested the abrasive size up to 150 μm in this study, but
6 there can be an optimal abrasive size larger than 150 μm . In addition, an optimal boiling surface
7 with higher roughness and volumetric wicking rate can be found through a parametric study
8 including the other sandblasting parameters such as pressure (P), sweeping speed (v), line-pitch
9 (p_l), and nozzle-to-sample distance (d_n). Nevertheless, the significant enhancement of boiling
10 heat transfer demonstrated in this work promises the potential of a sandblasting process for
11 industry-scale boiling applications.

12

13 Authors' Contributions

14 Y. Song and E. N. Wang conceived the idea. Y. Song, C. Wang, G. Su, and M. M. Rahman
15 conducted boiling experiments. Y. Song and D. J. Preston performed EDS analysis. Y. Song and
16 H. Cha fabricated sandblasted surfaces. Y. Song and J. H. Seong characterized surface
17 morphology with optical profilometry. Y. Song characterized surface wickability. B. Philips, M.
18 Bucci, and E. N. Wang guided the work. D. J. Preston, M. Bucci, and E. N. Wang acquired the
19 financial supports. The manuscript was written through contributions of all authors.

20

21 Supporting Information

1 Scanning electron microscope and energy-dispersive x-ray spectroscopy images of sandblasted
2 surfaces; Pool boiling experimental setup and characterization

3

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13 Preston acknowledges funding support from the Rice University Faculty Initiatives Fund.

14

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