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Evaluating impacts of CO2 intrusion into an unconsolidated aquifer: II. Modeling results

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#### **ABSTRACT** 20

Large scale deployment of  $CO<sub>2</sub>$  geological sequestration requires the assessment of the risks. One of the potential risks is the impact of  $CO<sub>2</sub>$  leakage on shallow groundwater overlying the sequestration site.The understanding of the key chemical processes and parameters are critical for building numerical models for risk assessment. Model interpretation of laboratory and field tests is an effective way to enhance such understanding. As part of this investigation, column experiments in which the  $CO<sub>2</sub>$  saturated synthetic groundwater flowed through a column packed with materials from the High Plains aquifer, were conducted. Changes in concentrations of several constituents in the column effluent and pH were determined. In this paper, a reactive transport model was developed to describe and interpret the observed concentration changes, attempting to shed light on the chemical reactions and mechanisms and key parameters that control the changes in effluent chemistry. The reactive transport model described fairly well the changes in pH and the concentration changes of Ca, Mg, Ba, Sr, Cs, As and Pb. Calcite dissolution and Ca-driven cation exchange reactions were the major drivers for the concentration changes of Ca, Ba, Sr, and Cs. The pH-driven adsorption/desorption reactions led to a concentration increase of As and Pb. The volume fraction and reactive surface area of calcite, CEC and sorption capacity were key parameters in controlling the magnitude of concentration increase. Model results also showed that Ba, which is an important chemical element released into the aqueous phase during these experiments, may be incorporated into the calcite crystal structure and the dissolution of Ba-bearing calcite could be an alternative pathway to explain the increase in aqueous Ba concentration when sediments are exposed to the  $CO<sub>2</sub>$  saturated leaching groundwater. 21 22 23 24 25 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41

#### **1. INTRODUCTION** 42



- Jackson, 2010; Lu et al., 2010; Smyth et al., 2009; Varadharajan et al., 2013; Viswanathan et al., 62
- 2012; Wunsch et al., 2014), although the type of metal being released and the severity of release 63

vary among these experiments. In field tests, however, release of trace metals, especially those of environmental relevance such as As, Pb, Ba, and Cd, has not been observed (Cahill and Jakobsen, 2013; Kharaka et al., 2010; Peter et al., 2012; Spangler et al., 2010; Trautz et al., 2013b; Yang et al., 2013). The difference between the observation of laboratory and field tests in terms of the release of trace metals is probably because the laboratory experiment is too aggressive in leaching out trace metal due to the use of DI water, oxidation, high water/solid ratio and longer reaction time. On the other hand, release of alkali and alkaline earth metals, including Na, K, Ca, Mg, Sr and Ba, were commonly observed both in laboratory and field experiments, although the degree of releases were different. The rise in concentrations of dissolved constituents observed during field tests was typically much less pronounced than in laboratory experiments — field tests show increases about an order of magnitude or less compared to pre- $CO<sub>2</sub>$  levels (20% to 700% in the studies cited above), while orders-ofmagnitude increases have been observed in laboratory tests. While the increase in concentration of dissolved constituents raises concerns, a lot of 64 65 66 67 68 69 70 71 72 73 74 75 76 77

efforts have been invested to understand the controlling chemical processes via model interpretation of laboratory experiments (Viswanathan et al., 2012) and field tests (Zheng et al., 2012). These efforts will facilitate the development of numerical models which will have a better predictability. The chemical processes potentially responsible for the mobilization of trace elements (due to an increase in aqueous carbonate concentration and the decrease of pH include the dissolution of carbonates (Birkholzer et al., 2008; Kharaka et al., 2006b; McGrath et al., 2007), sulfides (Apps et al., 2010; Wang and Jaffe, 2004; Zheng et al., 2009) and iron oxyhydroxide minerals (Kharaka et al., 2006a; Kharaka et al., 2009), as well as surface reactions 78 79 80 81 82 83 84 85

such as adsorption/desorption and ion exchange (Apps et al., 2010; Kharaka et al., 2006a; Kharaka et al., 2009; Zheng et al., 2009). The release of alkali and alkaline earth metals, including Na, K, Ca, Mg, Sr and Ba, which are most commonly observed both in laboratory and field experiments, is thought to be controlled by the dissolution of calcite and Ca-driven cation exchange reactions (Zheng et al., 2012). The reaction path proposed and kinetic model study conducted by Wilkin and Digiulio (2010) further indicates that the geochemical response of an aquifer to  $CO<sub>2</sub>$  leakage is closely related to the aquifer mineralogy. It is thus expected that differences in mineralogy in addition to differences in geology (i.e., aquifer type), and groundwater chemistry at any particular site could lead to different responses to  $CO<sub>2</sub>$  leakage. For this reason, experimental laboratory work and field tests coupled with modeling studies are necessary to assess the response of a particular aquifer and evaluate potential changes in groundwater quality and risks related to a  $CO<sub>2</sub>$  release. 86 87 88 89 90 91 92 93 94 95 96 97

The objective of this study is to determine the geochemical reactions that occur and influence changes in pH and trace metal mobilizations in groundwater aquifers after the intrusion of the  $CO<sub>2</sub>$  gas. Batch and column experiments in which materials from the High Plains aquifer were exposed to  $CO<sub>2</sub>$  saturated synthetic groundwater (SGW) were conducted to simulate the impact of an accidental release of  $CO<sub>2</sub>$  on a shallow aquifer. These experiments are presented in the first paper of this two paper series (Lawter et al., 2015). A reactive transport model was developed to interpret the observed concentration changes in the column effluent water, attempting to shed light on the chemical reactions and key parameters that control the concentration changes of some constituents. Modeling the batch experiment presented in the first paper of this series (Lawter et al., 2015) would help to improve and/or further consolidate the geochemical 98 99 100 101 102 103 104 105 106 107

conceptual model and the reactive transport model, but which have been previously developed based on the batch experiments conducted on other sand-based sediment (Zheng et al., 2015). 108 109

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#### **2. COLUMN EXPERIMENTS** 111

#### **2.1 Materials and Methods** 112

Modeling was based on column experiments conducted on sediments from the High Plains aquifer in Kansas, obtained from the Drill Core Library at the Kansas Geological Survey. Sediments originated from a single well (CNG), but depths varied from 8 feet to 150 feet. The sediments used in this study were from 58'-60' (CNG 60) and 109'-111' (CNG 110). Characterizations were conducted for these sediment samples to determine chemical composition, crystallization, and surface morphology. Acid extractions conducted on the sediments revealed the sediments contained contaminants of concern for groundwater quality, such as As, Sr, and Pb. The SGW with a chemical composition and pH similar to that of the High Plains aquifer [based on USGS groundwater data for the High Plains aquifer (Becker et al., 2002)], was used in all laboratory experiments and as the influent solution in the models. The recipe used to make SGW is given in Lawter et al. (2015); the composition of the SGW is listed in Table 1. 113 114 115 116 117 118 119 120 121 122 123 124

The column experiments are explained in more detail in Lawter et al. (2015), but will be described briefly here. The columns were conducted at room temperature (21  $\pm$  2 °C) and were initially leached with SGW for several days to achieve hydrological equilibrium (i.e., full saturation) and were then leached with CO2 gas-saturated SGW. CO2 gas was continuously purged in the influent bottle at a rate of 0.5 mL/min. Stop flow conditions were used to 125 126 127 128 129

determine the effect of increased fluid residence time on elemental release to observe timedependent reactions and processes in the columns. Stop flow conditions were applied after the initial leaching with SGW prior to CO2 injection (time = 70 hours, stopped for 170 hours) then twice more at approximately 250 hours and 350 hours, with the stop flows lasting 122 hours. During the experiment, about one sample per pore volume (PV) was collected, while the effluent samples were collected more frequently after the stop-flow events. The pH was measured continuously online. At the end of the experiments, selected effluent samples were analyzed by both ICP-OES and -MS to determine the aqueous concentrations of major, minor, and trace elements. Column parameters and other related information are listed in Table 2. 130 131 132 133 134 135 136 137 138

#### **2.2 Sediment Characterization: XRD and SEM/EDS** 139

Full results can be found in Qafoku et al. (2013), Shao et al. (2014) and Lawter et al. (2014) but a summary is provided below. Quantitative XRD analyses (QXRD) were conducted for the High Plain aquifer sediments used in this work. The results indicate that quartz and feldspar are the major minerals for the sediments (Qafoku et al., 2013). Small amounts of mica were also detected in the silt fraction of both samples. For the <2mm fraction used in the experiments, CNG 110 contained 1% calcite (the silt and clay fractions contained 35% and 11% calcite, respectively), but no detectable calcite was found in CNG 60. Scanning Electron Microscopy (SEM) and Energy-Dispersive X-ray Spectroscopy (EDS) data shows the presence of Ca bearing phases in CNG 60 (most likely, calcite coatings), which was undetected in the QXRD results (Lawter et al., 2014). These results indicate that the sandy sediments used in this work represent one aquifer type (largely unconsolidated aquifers) overlying potential  $CO<sub>2</sub>$ sequestration repositories within the continental US. 140 141 142 143 144 145 146 147 148 149 150 151

### **3. MODELING** 152 153

### **3.1 Model setup** 154



phases allowed to form are given in Table 3. These data were taken from Data0.dat.YMPv4.0, a EQ3/6 (Wolery, 1993) database qualified by the U.S. Department of Energy for the Yucca Mountain. 175 176 177

As SGW initially displaces the pore water residing in the column, the measured concentrations for the first effluent water sample actually represents the initial water composition in the column. The model therefore uses first measured concentration of the effluent as the initial concentrations. The concentrations of major cations and anions in the SGW were calculated from the recipe found in Lawter et al. (2014) and those for the trace elements are assigned small values of 10<sup>-15</sup>. The SGW was pH adjusted to a value of 7.5 prior to the start of the experiment and the concentration of dissolved  $CO<sub>2</sub>$  is calculated by assuming equilibrium with atmosphere  $(CO<sub>2</sub>$  partial pressure of 10<sup>-3.4</sup> bar), which yields a total concentration of dissolved  $CO<sub>2</sub>$  of  $2.35\times10^{-4}$  M. After the SGW is purged with CO<sub>2</sub>, the pH decreases to 4 and the concentration of dissolved  $CO<sub>2</sub>$  is calculated by equilibrating with  $CO<sub>2</sub>$  partial pressure of 0.14 bar (2 PSI, see Table 2) which leads to a total dissolved  $CO<sub>2</sub>$  concentration of  $5.1 \times 10^{-3}$  M. The simulations were conducted with TOUGHREACT Version 2 (Xu et al., 2011), which 178 179 180 181 182 183 184 185 186 187 188 189

implements a general form of rate law for the dissolution and precipitation of solid phases (Lasaga et al., 1994; Steefel and Lasaga, 1994): 190 191

$$
r = kA \left| 1 - \left(\frac{K}{Q}\right)^{\theta} \right|^{n}
$$
 (1)

192

where r is the kinetic rate, k is the rate constant  $(mol/m<sup>2</sup>/s)$  which is temperature dependent, A is the reactive surface area per kg water, K is the equilibrium constant for the mineral–water 193 194

reaction written for the destruction of one mole of mineral, and Q is the reaction quotient. Here, for simplicity, the exponents  $\theta$  and  $\eta$  are assumed equal to 1. The reactive surface area, A, is a function of the mineral specific surface area (e.g.,  $\text{cm}^2/\text{g}$  mineral) and the volume fraction of the mineral in the sediment. 195 196 197 198

The rate constant for calcite dissolution is given as a combination of neutral, acid and carbonate mechanisms (Palandri et al., 2005; Plummer et al., 1979): 199 200

201

$$
k_{\Box} = 1.5 \times 10^{-6} e^{-E_{a}^{m}/RT} + 0.5 e^{-E_{a}^{H}/RT} a_{H} + 9.6 \times 10^{-5} e^{-E_{a}^{CO2}/RT} a_{CO2}
$$
(2)

where  $E_a^{nu}$ ,  $E_a^H$  and  $E_a^{CO2}$  are activation energies with values of 23.5, 14.4 and 35.4 (kJ/mol), respectively. The rate constant for the neutral, acid and carbonate mechanisms, are respectively 1.5×10<sup>-6</sup> (mol/m<sup>2</sup>/s), 0.5 (mol/m<sup>2</sup>/s/M) and 9.6×10<sup>-5</sup> (mol/m<sup>2</sup>/s/M).  $a_H$  is the H<sup>+</sup> activity and  $a_{CO2}$ is the activity of dissolved  $CO_2$ . In the model, the specific surface area of calcite (60 cm<sup>2</sup>/g) was calibrated, together with the initial calcite volume fraction, to match the breakthrough of alkaline earth metals observed for the column test on sample CNG 60. The same specific surface area of calcite is also used in the base model for sample CNG 110. 203 204 205 206 207 208 209

The rate constant for magnesite dissolution is also given as a combination of neutral, acid and carbonate mechanisms (Palandri et al., 2005): 210 211

$$
k_{\Box} = 4.75 \times 10^{-10} e^{-E_{a}^{m}/RT} + 4.16 \times 10^{-7} e^{-E_{a}^{H}/RT} a_{H} + 1.74 \times 10^{-6} e^{-E_{a}^{CO2}/RT} a_{CO2}
$$
(3)

where  $E_a^{nu}$ ,  $E_a^H$  and  $E_a^{CO2}$  are activation energies with values of 23.5, 14.4 and 62.8 (kJ/mol), respectively. The rate constant for the neutral, acid and carbonate mechanisms, are respectively  $4.75 \times 10^{-10}$  (mol/m<sup>2</sup>/s),  $1.46 \times 10^{-7}$  (mol/m<sup>2</sup>/s/M) and  $1.74 \times 10^{-6}$  (mol/m<sup>2</sup>/s/M). In the model, the specific surface area of magnesite  $(200 \text{ cm}^2/\text{g})$  was calibrated, together with the initial magnesite volume fraction, to match the breakthrough of Mg and pH observed for the column test on sample CNG 60. We use the same specific surface area of magnesite in the base model for sample CNG 110. 213 214 215 216 217 218 219

Because minerals other than calcite and magnesite have negligible effects on the chemical changes in the column due to the short duration of the experiment, their surface areas and rate constant are taken from Xu et al. (2006) and Zheng et al. (2012) without further calibration. Note that  $Fe(OH)<sub>3</sub>(s)$  has intangible dissolution over the course of the experiment, which means its dissolution has little effect on the chemical change in the experiment, and as the adsorbent it is important. 220 221 222 223 224 225

#### **3.2. Modeling results**  226

The focus of this paper is the interpretation of concentration changes observed in the CNG 60 column, which shows systematical and well correlated changes in concentration of various elements. The model interpretation of pH, and some alkali and alkaline earth metals including Ca, Mg, Ba, Sr and Cs whose changes have been widely observed in the laboratory and field tests, and As and Pb which are of great environmental concern and less commonly observed in the field and lab tests are specifically targeted. A model for the column test on sample CNG 110 was also developed based on that for CNG 60. 227 228 229 230 231 232 233

#### *3.2.1. Models for the CNG 60 column: The base case* 234

The pH drops immediately following flowing  $CO<sub>2</sub>$  saturated SGW through the column, although the extent of drop varies depending on the pH buffering processes. Figure 1 shows the comparison of the measured and simulated pH for the CNG 60 column experiment. In the current model, dissolution of calcite and magnesite are the major reactions that buffer pH, with less pH buffering effect from the surface protonation. The pH buffering by the dissolution of calcite has been well understood and demonstrated (Birkholzer et al., 2008; Carroll et al., 2009; Wang and Jaffe, 2004); the pH buffering by the surface protonation is also well known and has been demonstrated recently in the context of the impact of  $CO<sub>2</sub>$  leakage on groundwater (Zheng et al., 2009; Zheng et al., 2012). However, the effect of magnesite dissolution on pH is not widely reported. As demonstrated in Figure 3, removal of magnesite leads to underestimation of pH after around 400 hours. As the  $CO<sub>2</sub>$  saturated SGW flushes through the column, calcite dissolution is the primary pH buffer process. After about 400-500 hours, calcite is most likely depleted. Because surface protonation has limited pH buffer capacity, pH keeps decreasing and eventually reaches a level close to the pH of the injected SGW ( $pH = 4$ ), if additional  $pH$ buffering from magnesite dissolution is not considered (Figure 3, "model no magnesite"). This motivates the consideration of magnesite in the base model. Also motivating the inclusion of magnesite in the model is the concentration level of Mg, which will be discussed later (Figure 2). Measured breakthrough curves for Ca, Ba, Sr and Cs show a similar trend — a sharp increase in concentration upon the arrival of  $CO<sub>2</sub>$  saturated SGW and then a quick drop. A similar trend has also been observed in a field test conducted in Mississippi (Trautz et al., 2013b), which was interpreted with a model concept that considered the dissolution of minute amount of calcite and the concurrent cation exchange reactions (Trautz et al., 2013b; Zheng et 235 236 237 238 239 240 241 242 243 244 245 246 247 248 249 250 251 252 253 254 255 256

al., 2012). Here we apply the same concept but recalibrate the quantity of calcite and surface area (which affect the dissolution rate of calcite). A volume fraction of 0.045% and a specific surface area of 60 cm<sup>2</sup>/g are used for calcite, which leads to a decent fit of the measured breakthrough curve of Ca as shown in Figure 1. Calcite is not observed by XRD because the volume fraction is well below the detection limit of 1%, but Ca bearing coating was detected in CNG 60 by SEM/EDS analysis. It is also noteworthy that a volume fraction of calcite below the XRD detection limit is also used in the model for the field test described in Trautz et al. (2013a), where the presence of calcite in the sediments was later confirmed by micro-X ray spectroscopy. The specific surface area of 60 cm<sup>2</sup>/g for calcite is also higher than that used in Trautz et al.  $(2013a)$  $(9.8 \text{ cm}^2/\text{g})$ , which is justified considering the difference between the column test with  $\leq 2 \text{ mm}$ sample in this paper and the field test in Trautz et al. (2013b). Because the dissolution rate of calcite is a function of pH and dissolved  $CO<sub>2</sub>$  (or  $CO<sub>2</sub>$  partial pressure) as shown in Equation (2), the dissolution of calcite is significantly accelerated upon the arrival of  $CO<sub>2</sub>$  saturated SGW which is low in pH and high in dissolved  $CO<sub>2</sub>$ . Such an acceleration of calcite dissolution is the key for a sharp increase in Ca concentration, but the concentration decrease after the peak (Figure 1) is due to the depletion of calcite. 257 258 259 260 261 262 263 264 265 266 267 268 269 270 271 272

The increase in Ca concentration due to calcite dissolution triggers a series of cation exchange reactions. As a result, the concentrations of most alkali and alkaline earth metals show a similar pulse-like shape in the breakthrough curves, e.g., Sr, Ba (Figure 1) and Cs (Figure 2). The model reasonably follows the measured breakthrough curves of Sr and Cs, but underestimates the measured data of Ba although qualitatively the model results and data for Ba match. The quantitative mismatch between model results and data for Ba could be eased if 273 274 275 276 277 278

another Ba release mechanism is considered, which will be discussed later in this paper. In the current model, Mn is controlled only by cation exchange reaction. Model results match the first peak in the Mn breakthrough curve but fail to catch the stepwise increase in the Mn concentration in the effluent (Figure 2). The fact that Mn concentration keeps increasing indicates there is dissolution of Mn bearing minerals. However, no Mn bearing minerals were detected in mineral characterization; they might be of too small quantity to be identified. Interestingly the breakthrough curve of Si shows a pattern (Figure 2) similar to Ca, Cs, Sr and Ba, except Si has a more pronounced peak after the second and third stop-flow events. The similarity between Si and and Ca breakthrough had also been observed in a field test in Mississippi (Pugh et al., 2013). Because Si bearing minerals are unlikely to dissolve as quickly as calcite, and based on findings previously presented in the literature (Pugh et al., 2013), we included adsorption/desorption reactions for Si in the model (see Table 4) and, as a result, a qualitative match between model and experimental data was achieved for Si (Figure 2). The SGW contains a fairly high concentration of Na which largely determines the concentration of Na in the effluent. However, cation exchange with Ca can also cause small pulses in the breakthrough curve of Na, as shown in Figure 2. In addition, the SGW contains about  $1.57 \times 10^4$  mg/L Mg. Without an additional source of Mg from magnesite, as shown by the "model no magnesite" in Figure 3, cation exchange makes the simulated Mg concentration after the first peak fairly lower than that of measured data. The dissolution of magnesite in the base model improves the fit between measured and simulated Mg concentration. Increasing the dissolution rate of magnesite could raise the concentration level of Mg after the first peak and improve the fit. However, this will drive the pH higher and decrease the fit between measured 279 280 281 282 283 284 285 286 287 288 289 290 291 292 293 294 295 296 297 298 299 300

and simulated pH. If dolomite instead of magnesite is used, model results for Mg are similar, but the fit between measured and simulated pH and Ca become slightly worse. 301 302

Generic modeling works (Apps et al., 2010; Zheng et al., 2009) and models for the field test (Zheng et al., 2012) have shown that desorption due to pH drop could be the main process that controls the release of trace elements such as As and Pb in response to the  $CO<sub>2</sub>$  leakage in groundwater. The close match between the measured and simulated breakthrough curve of As (Figure 1) in this paper seems to support this concept. The surface complexation reactions for As are listed in Table 2; the amount of the adsorbent, which is assumed to be  $Fe(OH)<sub>3</sub>(s)$  is calibrated. Note that here we use the adsorption/desorption of As from  $Fe(OH)_3(s)$  as a proxy of all possible adsorption/desorption reactions including those that could occur on the surface of clay minerals. The fit of measured Pb concentration with model results (Figure 1) is less desirable, but the model catches the concentration changes fairly well after the third stop-flow event. 303 304 305 306 307 308 309 310 311 312 313

#### *3.2.2. An alternative model with Ba impurity in calcite* 314

Because most sediments contain some clay and subsequently cation exchange reaction is ubiquitous, the dissolution of calcite and the concurrent Ca-driven cation exchange have been used so far to explain the change of Ba concentration. Another possibility that could not be ruled out is that Ba could be present in calcite as an impurity so that Ba is released concomitantly with Ca as calcite dissolves. This concept has been used by Lu et al. (2010) to interpret the release of metals upon  $CO<sub>2</sub>$  intrusion in groundwater in their laboratory experiment. This concept was also tested here by modeling the dissolution of calcite containing 2.5 mol % Ba impurity as shown by the following reaction. 315 316 317 318 319 320 321 322

Ba-Calcite + CO2(g) + H2O = 0.975Ca+2 + 0.025Ba+2 + 2HCO<sup>3</sup> - (4)

323

The equilibrium constant for reaction (4) was calculated by assuming an ideal solid solution between calcite and witherite. This seems to result in a better fit for Ba concentration compared to the base case (Figure 4), suggesting that this is a plausible process for the release of Ba. 324 325 326

#### *3.2.3. Models for the CNG 110 column: The base model* 327

Based on the model for sample CNG 60 and correcting the amount of minerals according to the experimental measurement, a model was created to describe the data collected from the column test conducted with sample CNG 110. CNG 110 differs significantly in the content of calcite with CNG 60. Differences in other major minerals such as quartz and feldspar in sample CNG 110 in comparison with CNG 60 most likely have only negligible effects on elemental concentration changes considering the short duration of the test. 328 329 330 331 332 333

Like the model for sediment CNG 60 model, the model for sediment CNG 110 catches the measured breakthrough curve of pH, but the modeling curve starts to deviate after 400 hours of experimental time (Figure 1). The fact that simulated pH remains at the same level before and after 400 hours indicates that calcite has not been depleted. Model results for CNG 60 shows it takes 400-500 hours to run out of calcite at a volume fraction of 0.045%, so it is not possible to deplete 1% calcite in 400 hours. 334 335 336 337 338 339

Upon the arrival of  $CO<sub>2</sub>$  saturated SGW, the dissolution of calcite leads to a quick increase of Ca concentration and maintains a relatively high level thereafter. On the contrary, measured data shows a slow increase and does not reach the high concentration level shown by model results (Figure 1). 340 341 342 343



The CNG 60 model explains the concentration changes in As and Pb by desorption caused by the drop of pH, but the CNG110 model fails to match the observed data for As and Pb. 364 365

As the pH in the CNG 110 column test decreases less than that in the test on CNG 60, there is less desorption and therefore As and Pb are lower as shown by the model for CNG 110, although it departs from measured data (Figure 1). 366 367 368

#### *3.2.4. An alternative model for CNG 110 with higher CEC* 369

The CEC is a key parameter that affects the Ba and Sr solid and liquid phase concentrations. In the base model for CNG 110, a CEC of 1.55 meq/100 g was used which was also used for the model for CNG 60. However, as the clay content in CNG 110 is different, the CEC varies as well. In a sensitivity run, the CEC was increased to 8 meq/100 g, hoping to improve the match between model and measured data. Higher CEC leads to higher concentration after the initial rising, but still fails to make the simulated initial peak closer to the measured data for Ba and Sr (Figure 5). 370 371 372 373 374 375 376

The model for CNG 60 shows that inclusion of Ba impurity in calcite leads to a better fit of measured data of Ba. This was also applied to the model for CNG 110, with 1 mol% Ba included in calcite. The continuous dissolution of calcite results in a sustainable increase in Ba concentration, which deviates significantly from the measured experimental data. 377 378 379 380

#### **4. DISCUSSION** 381

#### **4.1. About the initial amount of calcite** 382

In the column test, pH decreases upon the arrival of  $CO_2$ -saturated SGW at the outlet, and the Ca concentration soars up quickly and then decreases after reaching a peak concentration. The temporal profiles for the concentration of other alkali and alkaline earth metals such as Sr and Ba in the effluent follow almost precisely the pattern of Ca. Similar patterns of temporal 383 384 385 386

concentration changes have also been observed in a field test conducted in Mississippi (Trautz et al., 2013b). In this test, groundwater from a confined hydrostratigraphic interval was pumped and carbonated above ground, then re-injected into the same interval (in a dipole, closed loop system) of an aquifer at approximately 50 m deep. Injection of carbonated groundwater at this site lasted for around 5 months, preceded by an extensive monitoring period of background conditions and followed by a post-injection monitoring period of around 10 months. Four monitoring wells were emplaced downstream of the injection well. The concentration changes of alkali and alkaline earth metals in the nearest monitoring well shows exactly the same pulse-like shape as we observed in the column tests presented in this paper. To mimic the Ca concentration profile at the Mississippi field test with reactive transport model, a small amount of calcite (~0.006–0.009%), an amount that is enough to create the concentration peak but lead to depletion of calcite after the arrival of  $CO<sub>2</sub>$ -charged water, has to be used in the model. The concentration change of the rest of the alkali and alkaline earth metals then can be interpreted as Ca-driven cation exchange reaction. However, because calcite were not detected using XRD, doubt on such model interpretation had been raised when the model was first published (Trautz et al., 2013b), despite the amount of calcite used in the model being much lower than the detection limit of XRD. A later laboratory study with the same sediment (Varadharajan et al., 2013) found calcite using micro-X ray spectroscopy, which confirmed the validity of considering a small amount of calcite in the model. Intuitively, we applied the same model concept to interpret the breakthrough curve of Ca, Sr, Cs and Ba for the column test conducted with sample CNG 60, and found a good match between model and experimental data. We therefore conclude that a small amount of calcite does exist in sample CNG 60 as indicated by the SEM/EDS results and despite not being detected by XRD. 387 388 389 390 391 392 393 394 395 396 397 398 399 400 401 402 403 404 405 406 407 408 409

#### **4.2. About the impurity of trace metals in calcite** 410

It is not uncommon for calcite to contain metal impurities. Some researchers (Kirsch et al., 2014; Lu et al., 2010; Wunsch et al., 2014) thus proposed the dissolution of calcite with impurities to explain the concurrent rise in concentrations of Ca and other metals. In this paper, we first used the dissolution of calcite and Ca-driven cation exchange to explain the breakthrough curve of Ba, and then tried to use the dissolution of calcite with Ba impurity (Section 3.2.2) to match the data. The former model catches the initial and final concentration of Ba and the latter model catches the peak better. In another study Zheng et al. (2014), we tested both these concepts (or models), and the concept of calcite dissolution with Ba impurity did a less desirable job to match the Ba release from a batch experiment (Varadharajan et al., 2013). These two concepts have the same the reaction kinetics that is controlled by the calcite dissolution rate. The difference between these two concepts is that in the first concept, cations interfere with each other due to competition on exchangeable sites and are constrained by CEC, whereas in the second concept, cations are more independent of each other and are only constrained by the fraction of impurity in the calcite. The conclusion is that both concepts are plausible and a model for a column (or batch) test cannot delineate which one is at play. 411 412 413 414 415 416 417 418 419 420 421 422 423 424 425

**4.3. Constraining relevant chemical parameters for large scale model** 426

In the context of assessing the risk of  $CO<sub>2</sub>$  leakage on groundwater, reactive transport models are indispensible tools. The predictability of a reactive transport model is dictated by the chemical reactions considered in the model and key parameters for these reactions. Column tests with the sediment from the target aquifer and the interpretive reactive transport model for the column will play a key role in raising our confidence for the large scale reactive transport 427 428 429 430 431

models. First, a column test is a screening tool to determine which elements could be released by the leakage of  $CO<sub>2</sub>$ . Batch experiments can be used for such purpose as well, but tend to be too aggressive because of the large water-to-solid ratio and long residence time for water-rock interaction. For example, batch experiments (Varadharajan et al., 2013) were conducted for the sediments from an aquifer where a field test was conducted (Trautz et al., 2013); some elements in the EPA primary groundwater regulation list, such as As, Pb, showed significant increases in the batch experiment, but were not even detected in the field test(Pugh et al., 2013). Because column tests are typically conducted at water-to-solid ratio close to field conditions and take into account the interaction between transport processes and chemical reactions, it is a better proxy to the field condition and therefore a better tool than batch experiments to determine which elements are going to be released. Second, interpretation of column tests with reactive transport models helps to delineate the controlling chemical reactions and calibrate the key parameters. For example, in this paper, a close match between the model and column data for Sr clearly indicates that Ca-driven cation exchange is the reaction that controls the release of Sr, and the reactive surface area of calcite and CEC are the key parameters which can be well constrained from the Ca and Sr breakthrough curves. Matching the As and Pb data with model results confirms the control of adsorption/desorption on the release of As and Pb and can be used to calibrate the amount and surface area of adsorbents. 432 433 434 435 436 437 438 439 440 441 442 443 444 445 446 447 448 449

**5. CONCLUSIONS**  450

To assess the long term risk of  $CO<sub>2</sub>$  geological sequestration, numerical models have to be employed to evaluate the potential impact of the  $CO<sub>2</sub>$  leakage on shallow groundwater overlying the sequestration site. The understanding of the key chemical processes and parameters 451 452 453

are critical for the predictablity of numerical models. Model interpretation of laboratory and field tests was an effective way to enhance such understanding. Column experiments in which  $CO<sub>2</sub>$ saturated SGW flows through a column packed with material from High Plains aquifer were conducted and concentrations of several chemical constituents in the effluent water were determined. In this paper, reactive transport model was developed to interpret the observed concentration changes, attempting to shed light on the chemical reactions and key parameters that control the concentration changes of these constituents. 454 455 456 457 458 459 460

The column test conducted with sediment CNG 60 shows systematical and well correlated changes in concentration of various elements. A reactive transport model can match the concentration changes of pH, Ca, Mg, Ba, Sr, Cs, As and Pb fairly well. Calcite dissolution and Ca-driven cation exchange reactions are the major drivers for the concentration changes of Ca, Ba, Sr, and Cs, which is consistent with the findings revealed by models developed with data generated from other sites (Trautz et al., 2013b; Zheng et al., 2012). The pH-driven adsorption/desorption reactions are the reason for concentration increases of As and Pb. The volume fraction and reactive surface area of calcite, CEC and sorption capacity are key parameters in determining the magnitude of concentration increase. Model results also show that the dissolution of calcite with Ba impurity could be an alternative explanation of the increase in Ba concentration. The model interpretation of column test clearly showed that understanding the metal-sediment association and key parameters are critical for the predictability of numerical models. 461 462 463 464 465 466 467 468 469 470 471 472 473

The model for sample CNG 60 was corrected for the amount of minerals (mainly calcite) based on the measurement for sample CNG 110, to interpret the column test results for the 474 475

sample CNG 110. Although the model follows well the experimental pH data, it fails to explain the concentration changes of the rest of the constituents. The poor correlation between the concentration of Ca, Ba and Sr, and the erratic concentration of Ca are probably the reasons for the mismatch between data and model. Pb and As data are also quite scattered so that it is hard to draw a clear trend and subsequently to interpret them with a model. While re-examination of the column test for sample CNG 110 and the conceptual geochemical modeling might be helpful for better understanding of the observations from column test for sample CNG 110, it illustrates the challenge we are facing when modeling the intriguing interactions between transport and chemical reactions involved in the test. 476 477 478 479 480 481 482 483 484

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- 493

#### **FIGURE CAPTIONS** 494

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**Table 1.** Cation exchange reactions and selectivity coefficients, using the Gaines-Thomas convention (Appelo and Postma, 1994). 496 497 498

**Table 2.** Surface complexation reactions and surface complexation constants (logK) on ferrihydrite (Dzomback and Morel, 1990; Appelo et al., 2002; Jordan et al., 2007). 499 500 501

**Table 3.** Equilibrium constants (logK) and initial volume fraction of minerals in the sediment (on a dry basis). LogK are for reactions that are written with the primary species listed in the first column of Table 2. 503 504 505

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#### **FIGURE CAPTIONS** 507



**Figure 3.** Simulated and observed breakthrough curves of pH and Mg with and without magnesite included in the model for the column test of sample CNG60. **Figure 4.** Observed breakthrough curves of Ba for the column test of sample CNG 60 (both graphs) and CNG 110 (right graph), and simulated results in the base model and a model with Ba impurity in calcite. **Figure 5.** Observed breakthrough curves of Ba and Sr for the column test of sample CNG110 and simulated results in the base model and a model with higher CEC value. 

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