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# Discerning molecular-level  $CO<sub>2</sub>$  adsorption behavior in amine-modified sorbents within a controlled  $CO<sub>2</sub>/H<sub>2</sub>O$  environment towards direct air capture† 5

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Sorbents designed for direct air capture (DAC) play a crucial role in the pursuit of achieving net-zero carbon dioxide emissions. This study elucidates CO<sub>2</sub> adsorption from dilute, humidified CO<sub>2</sub> streams onto an amine-modified benchmark DAC adsorbent via solid-state NMR spectroscopy. Various NMR techniques, including 1D <sup>1</sup>H MAS, <sup>13</sup>C MAS, 2D <sup>1</sup>H–<sup>13</sup>C HETCOR NMR, and <sup>1</sup>H  $R_2$  and  $R_{1\rho}$  relaxometry reveal the impact of  $CO_2$  partial pressure and H<sub>2</sub>O on  $CO_2$  adsorption behavior. We find that  $CO_2$  concentration governs the stepwise formation of ammonium carbamate, carbamic acid, and physisorbed CO<sub>2</sub>, where relative humidity (RH) at a desired low (<400 ppm) CO<sub>2</sub> loading affects total CO<sub>2</sub> uptake. The relaxation studies reveal the cooperative or competitive nature of  $H_2O$ –CO<sub>2</sub> sorption in CO<sub>2</sub>-dilute humid gas, and in particular polymer swelling upon humidification. From those results, we demonstrate that the observed absorption capacity enhancement by humidity is caused by

pore opening due to sorbent swelling, and not by bicarbonate formation. This NMR-discerned speciation provides insights into sorption behavior at different RHs in dilute CO<sub>2</sub> gas streams, simulating real-world atmospheric conditions, and governs the design of efficient and adaptable material-process combinations for solid sorbent DAC. 20 20

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### Introduction

Direct air capture (DAC) is a promising technology towards netzero carbon dioxide emissions and beyond, $<sup>1</sup>$  notable for its</sup> independence from point source emission locations and its ability to operate without the need for costly infrastructure, such as long  $CO<sub>2</sub>$  pipelines.<sup>2</sup> Particularly, DAC is identified as a critical tool to address hard-to-abate emissions, which are challenging to eliminate due to technical limitations, economic constraints, or considerations of social justice.<sup>3</sup> It also enables the net-negative emission scenarios needed to keep global

warming under 1.5 °C or 2 °C, aligning with international climate targets.<sup>3</sup> One DAC technology currently being scaled is 40

solid sorbent DAC, where air is contacted with a solid porous material that is regenerated using elevated temperature, vacuum, or both. A crucial aspect of solid sorbent DAC is the sorbent's capability to efficiently extract  $CO<sub>2</sub>$  from a humid and ultradilute-CO<sub>2</sub>, *i.e.* 400 ppm, stream, in contrast to the CO<sub>2</sub>-rich (e.g. 4-20%) streams targeted with the point source  $CO<sub>2</sub>$ capture.<sup>4</sup>

Effective DAC sorbents must meet essential criteria such as high  $CO<sub>2</sub>$  capacity, high selectivity over other components found in air, rapid sorption/desorption kinetics, thermal/ chemical stability, cost-effective regeneration, and affordability.<sup>4</sup> These inherent material characteristics of the sorbents are directly linked to the  $CO<sub>2</sub>$  adsorption mechanisms. Additionally,  $CO<sub>2</sub>$  adsorption is influenced by combined external environmental factors and ambient conditions such as temperature,  $CO<sub>2</sub>$  partial pressure, the presence of water vapor in the air, as well as other competing gases including  $N_2$ , and  $O<sub>2</sub>$ <sup>5,6</sup> Indeed, the concentration of water is typically orders of magnitude higher than the concentration of  $CO<sub>2</sub>$  in ambient air, and thus water may compete with  $CO<sub>2</sub>$  for adsorption sites and/ or enhance  $CO<sub>2</sub>$  adsorption via physical or chemical mechanisms. Consequently, environmental factors can fundamentally 40 45 50

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alter the adsorption amount and dynamics of a given material, thereby obfuscating field operation and control of DAC units.

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Amongst the many potential sorbent materials, aminemodified sorbents are widely studied for DAC due to their high  $CO<sub>2</sub>$  capacity at ultradilute- $CO<sub>2</sub>$  concentrations and their high selectivity for  $CO_2$  over  $N_2$  and  $H_2O$ . As a result, they are the only class of adsorbents used in DAC processes at scale today.<sup>7</sup> Thus, there has been some effort in the past two decades to study the impact of humidity on equilibrium  $CO<sub>2</sub>$  uptake in amine-modified adsorbents. There remains, however, challenges to validate working hypotheses for sorption dynamics with reliable experimental studies. $2,8-12$  Generally, it appears that the  $CO<sub>2</sub>$  uptake is enhanced in the presence of water at low relative humidities, yet uptake becomes less favorable at higher humidity levels. Previous studies have attributed enhanced CO<sub>2</sub> adsorption capacity to the formation of ammonium bicarbonate over ammonium carbamate, thereby doubling the potential stoichiometry of adsorption.<sup>13</sup> However, this hypothesis has proven difficult to affirm given that the prolonged timescales required to form bicarbonate are not consistent with observed  $CO_2$  adsorption.<sup>14,15</sup> Some studies have either not observed bicarbonate formation or reported only a very subtle presence of this species in humid  $CO<sub>2</sub>$  environments.<sup>16-18</sup> Instead, these studies have reported the formation of other major species, such as ammonium carbamate. Nevertheless, previous research on these species still does not entirely account for the observed enhanced  $CO<sub>2</sub>$  uptake. In-depth experimental examination of water– $CO<sub>2</sub>$  co-adsorption mechanisms in amine-functionalized adsorbents is largely missing, and therefore the exact nature of the observed adsorption phenomena is yet to be well understood. Absent a molecular understanding relating air composition to process behavior, DAC process performance is compromised, which has large implications for DAC plant siting decisions, as well as design 5 10 15 20 25 30 35

and optimization of processes and materials.<sup>5,6</sup>

In this study, we clarify why and how  $H_2O$  impacts  $CO_2$ adsorption in amine functionalized polymer resins. Lewatit® VP OC 1065 is used as an off-the-shelf benchmark sorbent as it exhibits a higher  $CO<sub>2</sub>$  adsorption capacity compared to other resins having the same supportive material.<sup>19</sup> Previous research into this material has provided analyses of pore structure, $20$ concentrations of functional groups,<sup>20</sup> oxidative degradation phenomenology, $21,22$  material regeneration, $20$  thermal and chemical stability over long-term exposure,<sup>23</sup> and performance in  $CO<sub>2</sub>$  and  $H<sub>2</sub>O$  sorption.<sup>20</sup> Additionally, researchers have investigated the molecular interactions between this sorbent and CO<sub>2</sub> using DRIFTS FTIR spectroscopy; they suggested formation of carbamate/carbamic acid and possibly bicarbonate under dry conditions, yet they concluded that the exact nature of captured species was undetermined.<sup>20</sup> Computational investigations have examined preferred adsorption processes in the presence of water, discussing direct amine– $H_2O$  interactions and amine catalyzed formation of carbamic acid,<sup>24</sup> suggesting that carbamic acid formation is the preferred pathway. Previous studies on  $CO<sub>2</sub>$  adsorption capacity have shown that water does not impede  $CO<sub>2</sub>$  adsorption between 0-60% RH;<sup>10</sup> however, the role of water in adsorption may vary with changes

in partial pressure.<sup>25</sup> Nevertheless, research to understand adsorption pathways in the presence of water remains limited. We surmise that a deeper molecular understanding of water/ amine/ $CO<sub>2</sub>$  interactions is currently lacking, and it is key to the design of sorbent-based DAC processes.

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Expanding on those earlier discoveries, this study focuses on elucidating the interaction of amine-functionalized polymer resins with  $CO<sub>2</sub>$  under both dry and wet conditions using  $^{13}$ C and <sup>1</sup>H solid-state NMR (ssNMR) spectroscopy. By varying  $CO<sub>2</sub>$ partial pressure and relative humidity, this NMR study identifies and quantitates chemisorbed species to assess enhanced or reduced  $CO<sub>2</sub>$  adsorption capacity. We find conclusive evidence that bicarbonate is not formed under humid conditions, contrary to earlier hypotheses. Furthermore, the  $CO<sub>2</sub>$ adsorption reaction within Lewatit® VP OC 1065 is primarily dictated by the  $CO<sub>2</sub>$  partial pressure during adsorption. NMR relaxometry reveals polymer pore swelling at higher humidity levels, and this modulates the competitive and cooperative adsorption of  $H_2O$  and  $CO_2$ . These findings allow the adjustment of current co-adsorption models to enhance their predictive capabilities and provide more robust insights on adsorbent performance. 10 15 20

### Results and discussion

#### Impact of CO<sub>2</sub> partial pressure on adsorption (under dry conditions)

The material Lewatit® VP OC 1065, featuring primary amine groups presumed to serve as chemisorption sites for  $CO<sub>2</sub>$ , was selected as a prototypical material to investigate the role of  $CO<sub>2</sub>$ partial pressure in its adsorption mechanism for DAC application. Activated materials were loaded at varying  ${}^{13}CO_2$  partial pressures ( $pCO<sub>2</sub> = 1000$ , 35 or 8 mbar) under dry conditions and analyzed using solid-state NMR spectroscopy. The <sup>13</sup>C CPMAS spectra presented in Fig. 1 demonstrate distinct chemisorption peaks between 155–170 ppm at various  $CO<sub>2</sub>$  loadings, with at least two discernible environments at 164 and 160 ppm. Additionally, Fig. S1a† employs direct polarization <sup>13</sup>C DPMAS and reveals a physisorption peak at 125 ppm, observed only at approximately 1000 mbar. Detailed spectral analysis (Fig. S1b†) further describes the characteristic peaks of the sorbent materials at 40–50 ppm, 120–130 ppm, and 140–150 ppm. 30 35 40

To better identify the different chemisorbed species, 2D  $^{1}$ H-<sup>13</sup>C Heteronuclear Correlation (HETCOR) NMR was employed to probe the through space close proximities between  ${}^{1}H$  and <sup>13</sup>C nuclei. <sup>13</sup>C-<sup>1</sup>H FSLG-HETCOR, where the FSLG protocol enhances the <sup>1</sup>H resolution in 2D HETCOR spectra, are shown in Fig. 2. This 2D correlation map clearly demonstrates variation in the formation of ammonium carbamate and carbamic acid across different  $CO<sub>2</sub>$  loadings. At a  $CO<sub>2</sub>$  partial pressure  $(pCO<sub>2</sub>)$  of 35 mbar, the <sup>13</sup>C resonance at 164 ppm is associated exclusively with NH  $(3.7$  ppm) and NH<sub>3</sub><sup>+</sup>  $(7.8$  ppm) (Fig. 2a). In contrast, at approximately 1000 mbar (Fig. 2b), the resulting  ${}^{13}C$ spectrum can be deconvoluted into three environments: I at 164 ppm, II at 161.1 ppm, and III at 159.2 ppm. The  ${}^{1}$ H projections for each 13C environment reveal different close proximities between carbons and protons (Fig. 2c). The three 45 50 55



Fig. 1  $13$ C solid-state CPMAS (contact time 2 ms) NMR of CO<sub>2</sub> adsorbed at various pressures (1000 mbar in blue, 35 mbar in green or 8 mbar in orange) within Lewatit® VP OC 1065. Signals observed between 140 to 150 ppm originate from the backbone in Lewatit® VP OC 1065, where not affected by CO<sub>2</sub> adsorption.

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<sup>13</sup>C resonances at 164, 161.1, and 159.2 ppm (environment I, II, and III, respectively) correlate with  $^1\mathrm{H}$  signals of NH at 3.7 ppm and  $NH_3^+$  at 7.8 ppm. In addition, the  $^{13}$ C site at 159.2 ppm (environment III) correlates with COOH at 15.1 ppm, while the  $13^{\circ}$ C site at 161.1 ppm (environment II) exhibits a weaker correlation with COOH (Fig. 2c) than environment III at 159.2 ppm. Based on this observation, we surmise that environment II may not be a distinct species but rather a mixed species comprising both ammonium carbamate and carbamic acid; this observation is consistent with previous NMR studies of melamine porous network polymer adsorbents.<sup>26</sup> These results demonstrate that ammonium carbamate (NHCOO−) is dominantly formed at  $pCO<sub>2</sub> = 35$  mbar, while both ammonium carbamate (NHCOO−) and ammonium carbamic acid (NHCOOH) contribute to  $CO_2$  adsorption at  $pCO_2 = 1000$  mbar.

Speciation of the local  $^{13}$ C environment at I (164 ppm) and III (159.2 ppm) is further clarified by exploiting the  $^{13}$ C chemical shift anisotropy (CSA) of these sites. While the CSA is typically averaged out during MAS, at slower spinning speeds the spinning sidebands of the NMR spectra are observed and these sidebands may be used to estimate the CSA for each isotropic

chemical shift.<sup>27</sup> The  $^{13}$ C CSA associated with each chemical shift is shown in Fig.  $S2\dagger$  and can be used to distinguish between protonated (COOH) and deprotonated (COO−) species (see ESI for details†).28,29 This analysis corroborates the HET-COR spectra, validating the identification of ammonium carbamate (site I) and carbamic acid (site III). Furthermore, a significant decrease in resonance at 159 ppm in Fig. S3,<sup>†</sup> detected after exposing the  $CO<sub>2</sub>$ -loaded materials at 1000 mbar to the ambient air, provides clear evidence for carbamic acid to be associated with environment III; this moiety is an unstable species in the air. 20 25

In summary, the variations in  $CO<sub>2</sub>$  partial pressure determine the interaction mechanisms with Lewatit® VP OC 1065 in the absence of water. Fig. 3 illustrates that the adsorption occurs as a stepwise process with respect to the partial pressure of  $CO<sub>2</sub>$ : at low  $CO<sub>2</sub>$  loading, adsorption is mainly governed by the formation of ammonium carbamate; as the  $CO<sub>2</sub>$  loading gradually increases, the formation of carbamic acid accompanies the formation of ammonium carbamate. At higher  $CO<sub>2</sub>$ pressures, we surmise that mixed ammonium carbamate and carbamic acid pairs appear. Moreover, physisorption appears 30 35



Fig. 2  $2D<sup>1</sup>H-<sup>13</sup>C FSLG-HETCOR spectra recorded with a contact time of 50 µs for Lewatit® VP OC 1065 loaded with (a) 35 mbar or (b) approx. 1$ bar of <sup>13</sup>CO<sub>2</sub>. The chosen contact time of 50 µs highlights protonated carbon sites. (c) Individual <sup>1</sup>H projection for each <sup>13</sup>C environment (I, II, and III in (b)) observed in the 2D spectrum in (b) at approximately 1 bar of  $^{13}CO_2$  are deconvoluted with colored dashed lines: NH (red), NH<sub>3</sub><sup>+</sup> (green), and COOH (blue).

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Fig. 3 Proposed stepwise CO<sub>2</sub> adsorption process at increasing CO<sub>2</sub> partial pressures: illustration of molecular structures (top) and the computed isosteric heat of adsorption (bottom). Isosteric heats of adsorption (-∆H<sub>ads</sub>) calculated from the isotherm data described previously (reproduced from ref.25 with permission from the Royal Society of Chemistry).

exclusively at the highest  $CO<sub>2</sub>$  loading (1000 mbar). These NMR analyses are consistent with previously computed isosteric heats of adsorption ( $-\Delta H_{\text{ads}}$ ) under dry conditions as a function of  $CO_2$  loading (Fig. 3, bottom).<sup>25</sup> These heats of adsorption reveal a step-wise change with  $CO<sub>2</sub>$  loading, and the present NMR results provide a basis for their molecular interpretation. 40

#### Co-adsorption of  $H_2O$  and  $CO_2$

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Water vapor plays a complex role in  $CO<sub>2</sub>$  adsorption, and can serve both as a facilitator and an inhibitor of adsorption, depending on the environmental conditions and on the type of adsorbent used.<sup>30</sup> Acting as a free base, water can initiate various reaction pathways such as hydrolysis of carbamates to bicarbonate, as reported in both theoretical calculation and NMR studies on aqueous amine solution.31,32 Additionally, Grand Canonical Monte Carlo (GCMC) studies showed the hydration of materials can generate additional adsorption active sites at the terminal water molecules in MIL-101,<sup>33</sup>

boosting  $CO<sub>2</sub>$  adsorption, especially under low-pressure mixed gases. Conversely, water can also have detrimental effects on CO2 adsorption by competing for adsorption sites. This competition can arise when water molecules weaken the interaction between  $CO<sub>2</sub>$  and the adsorbent surface through  $e.g.,$ a reduction in the electric field, $34$  or dominate the binding occupancy due to their strong dipole moments.<sup>35</sup> The formation of water clusters can further obstruct  $CO<sub>2</sub>$  adsorption.<sup>36</sup> We utilized the apparatus shown in Fig. S4† to systemically investigate the influence of water on  $CO<sub>2</sub>$  adsorption onto Lewatit® VP OC 1065. Activated materials were loaded with varying amounts of water to establish relative humidities (RHs) of 0%, 30%, and 80% (labelled RH0, RH30, and RH80, respectively) at a controlled  $CO<sub>2</sub>$  concentration of approximately 0.15 mbar (equivalent to 150 ppm). The chosen  $CO<sub>2</sub>$  concentration, set below atmospheric levels (∼400 ppm), aims to observe potentially maximized adsorption effects and to maximize the detection sensitivity for all species, including potential minor 40 45 50 55 species. It has been previously reported that adsorption efficiency doubled at 0.2 mbar  $CO<sub>2</sub>$ , 25 °C, and increased more than 2.5 times at 0.1 mbar  $CO<sub>2</sub>$ , 70 °C, and decrease as the pressure increases.<sup>25</sup> This approach allowed us to probe the molecular interactions at low partial pressure under different humidity conditions via solid-state NMR.

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Water adsorption may not be easily discernible in  ${}^{1}$ H NMR because its chemical shift at 4.5 ppm overlaps with the broader

 ${}^{1}$ H NMR signals from Lewatit® VP OC 1065, which displays overlapping peaks spanning from 0 to 10 ppm. Nevertheless, Fig. 4a reveals a gradual increase in the  $H_2O$  signal intensity at 4.5 ppm as the RH increases, and an intense signal is observed for  $H<sub>2</sub>O$  at 80% RH. This indicates that higher RH results in increased water adsorption. More interestingly, for  $CO<sub>2</sub>$ adsorption across all RHs, a single resonance is consistently observed around 164.5 ppm as a chemisorption in  $^{13}$ C CPMAS NMR spectra (Fig. 4b). The formation of a chemisorbed species 10 15

around 164.5 ppm is confirmed by  $2D^{13}C^{-1}H$  HETCOR (Fig. 4c), demonstrating clear correlations between the  $^{13}$ C site at 164.5 ppm with proton signals emanating from NH and  $\mathrm{NH}_3^{-1}$ groups. This establishes that ammonium carbamate forms at the tested  $CO<sub>2</sub>$  partial pressure, regardless of the RH percentage. However, water can dissolve  $CO<sub>2</sub>$  under humid conditions and lead to the formation of moieties such as bicarbonate or carbonate.<sup>31,37</sup> Those dissolved moieties may experience high mobility, and thus may remain undetected in CPMAS NMR studies. $38,39$  Therefore,  $13$ C direct excitation was utilized to discern the presence of mobile dissolved species. The single resonance near 164.5 ppm (highlighted area in Fig. 5a) and the lack of additional resonances near it clearly demonstrate the exclusive formation of ammonium carbamate across all conditions, both dry and wet, at the controlled  $pCO<sub>2</sub>$ . 1 5 10 15

It is worth noting that only when the partial pressure of  $CO<sub>2</sub>$ greatly exceeds 400 ppm atmospheric levels do we observe



Fig. 4 Solid-state MAS NMR spectra of Lewatit® VP OC 1065 dosed with co-adsorption (N<sub>2</sub>, CO<sub>2</sub>, and H<sub>2</sub>O) at low pCO<sub>2</sub> with variable RHs (RH0, RH30, and RH80). (a) <sup>1</sup>H DEPTH NMR; (b) <sup>13</sup>C CPMAS NMR with 200 µs of contact time; (c) <sup>13</sup>C-<sup>1</sup>H FSLG-HETCOR 2D spectra with 200 µs of contact time. Activated Lewatit refers to a state where sample pretreatment (high vacuum) lead to no adsorbed species. In 13C CPMAS NMR spectra, \* indicates spinning sideband and signals at 40-50 ppm, 120-130 ppm, and 140 to 150 ppm arise from the backbone in Lewatit® VP OC 1065, where not affected by  $CO<sub>2</sub>$  adsorption.



Fig. 5 Quantitative CO<sub>2</sub> adsorption at various relative humidities. (a) Solid-state  $^{13}$ C NMR obtained by direct excitation under MAS on samples exposed to a mixture gas  $N_2$  + CO<sub>2</sub> + H<sub>2</sub>O at 25 °C with RH0 (bottom, green), RH30 (middle, blue), and RH80 (top, red). (b) Tabulated values of quantified CO<sub>2</sub> adsorption corresponding to the NMR spectra shown in (a). In table, I (chem or raw) represents the integral area associated with chemisorbed species or sorbent itself in the spectra, and N (chem or raw) denotes the number of carbons associated with chemisorbed species or sorbent itself. (c) Comparison of the adsorbed CO<sub>2</sub> obtained from NMR (N<sub>2</sub> + CO<sub>2</sub> + H<sub>2</sub>O) with the isotherm experiments CO<sub>2</sub>, RH30 (CO<sub>2</sub> + H2O), and water at 25 °C. Isotherm experiments were described previously and reproduced from ref.25 with permission from the Royal Society of Chemistry.

species other than ammonium carbamate. The  $2D^{-13}C^{-1}H$ HETCOR spectra recorded on the 80% RH and 1 bar  $pCO<sub>2</sub>$ sample suggests the formation of other interactions among  $CO<sub>2</sub>$ , H<sub>2</sub>O, and the material (Fig. S5†). This spectrum suggests the possibility of ammonium carbamate and urea presence at high CO<sub>2</sub> loadings as indicated by the correlations at  $\delta(^{13}C)$  = 161 and 158.1 ppm, respectively. The observed correlation remains challenging to identify a particular species without ambiguities and a more in-depth study would be needed to understand their species formed at high  $pCO<sub>2</sub>$  and high RHs.

Following the detection of chemisorbed species in the presence of water at low CO<sub>2</sub> loading, further analysis elucidates the impact of  $H_2O$  on  $CO_2$  adsorption capacities through quantitative analysis of the spectra shown in Fig. 5. The quantification of adsorbed  $CO<sub>2</sub>$  was estimated from the ratios of integrated areas of the resonance corresponding to chemisorbed  $CO<sub>2</sub>$  to that associated with the polymer material. This approach allows for the determination of an enhancement factor,<sup>25</sup> simplifying the comparison of adsorbed  $CO<sub>2</sub>$  under different conditions relative to that under dry conditions. Our analysis shows that the adsorbed  $CO<sub>2</sub>$  doubles at 30% RH compared to the dry condition (0% RH). In other words, water aids in  $CO<sub>2</sub>$  adsorption at 30% RH by enhancing the formation of ammonium carbamate, but this increase does not manifest at 80% RH. Estimated  $CO<sub>2</sub>$  adsorption at 30% RH from NMR results aligns with the adsorbed  $CO<sub>2</sub>$  calculated at the corresponding pressure from the isotherm experiments conducted 45 50

previously (Fig. 5c).<sup>25</sup> This finding is also in accordance with the previous isotherm experiments at different RHs that showed a two-fold increase in  $CO<sub>2</sub>$  adsorption at 30% RH and a subsequent small reduction in adsorption as RH increases.<sup>25</sup>

#### NMR relaxometry to explore water impact

The NMR results above suggest that the presence of water does not yield additional chemical bonding or reactions between  $CO<sub>2</sub>$ and the sorbents at low partial pressures of  $CO<sub>2</sub>$ . Nevertheless, we find that variation in relative humidities increases the total  $CO<sub>2</sub>$  uptake at 30% RH, but not at 80% RH. We surmise that this effect arises from changes in the properties of the resins with hydration and/or molecular dynamics between guest molecules and sorbents. We deployed  ${}^{1}H$  NMR relaxation studies to examine these questions upon water adsorption. The changes in <sup>1</sup>H NMR relaxation rates indicate a change in the correlation times  $(\tau_c)$ , which characterize motion of protons (e.g. a shorter correlation time indicates faster proton motion). These constructs derive from the original Bloembergen–Pound–Purcell (BPP) theory and have been further elaborated in subsequent NMR treatises.<sup>40,41</sup> 40 45 50

While it is expected that polymer can swell with adsorbates, <sup>1</sup>H NMR relaxation provides insight into the expansion behavior of polymer resin pores during water adsorption. Particularly, the spin–spin relaxation  $(R_2 = 1/T_2)$  measurement presents a well-established relationship between transverse relaxation rates and physical characteristics of porous media through 55

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exchange between unbound and sorbent-bound states, as presented in eqn S1.† <sup>42</sup>–<sup>44</sup> Thus, Fig. 6 and S6† shows two wellseparated distributions given by water molecules within the pores (pore-confined  $H_2O$ ) and those outside the pores (free H2O), at least when water is beyond the saturation point. Since  $R_2$  is proportional to correlation time, free H<sub>2</sub>O with faster molecular motion characterized by shorter correlation time, results in lower  $R_2$  relaxation rates (longer  $T_2$  relaxation times). The time evolution of these  $R_2$  profiles following water adsorption indicates an approximate 8% decrease in the transverse relaxation rates  $(R_2)$  of pore-confined water (Fig. 6b). We thus conclude that there is a discernible surface-tovolumetric expansion of the pores by  $\approx 8\%$  with long expo-sure to water, *i.e.*, polymer swelling. The specific, time-evolving shapes of pores are difficult to measure directly and are not revealed by this type of relaxation analysis. A detailed study, however, of parameters such as tortuosity as a function of water adsorption measured via PFG NMR would assist in connecting pore expansion to specific geometric changes in the pores. Such studies would provide further insight into mass transfer kinetics of sorption. 1 5 10 15 20

Polymer swelling upon water adsorption is further confirmed by  $R_2$  measurements using heavy water (D<sub>2</sub>O), highlighting proton signals from the polymer sorbent and not the adsorbed water. This is demonstrated through two complementary experiments: one varying over time with saturated  $D_2O$ adsorption and the other varying with RH levels. In both experiments, a decrease in  $R_2$  indicates faster local motion (shorter correlation times) of polymer, as explained by BPP theory. The time variant  $R_2$  profiles (Fig. S6c and d†) show a noticeable decrease in  $R_2$  with saturated  $D_2O$  adsorption. Although precise analysis with  $D_2O$  is limited by a low signal-tonoise ratio and a complicated  $R_2$  distribution as seen via Inverse Laplace Transform (ILT) analysis, we nevertheless see adsorbed water as "lubricating" local chain motion in the Lewatit® VP OC 1065, consistent with studies of other polymers.<sup>45</sup> Furthermore, RH variant measurements reveal a clear decrease in  $R_2$  as RH 25 30 35

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levels increase by comparing the slopes of each signal decay without ILT analyses (Fig. 7a). While estimating the  $R_2$  value from these measurements encounters limitations such as signal loss during the initial echo period, these changes suggest that the incorporation of  $D_2O$  molecules into the sorbent increases local motions of polymer segments,<sup>46</sup> characterized by shorter correlation times (decreased  $R_2$  rates) for protons specific to the polymer. The gradual decrease in  $R_2$  as RH level increases indicates enhanced polymer segmental mobility of the sorbent,<sup>46</sup> a "lubrication" that likely enhances  $CO<sub>2</sub>$  adsorption by enabling easier access of guest molecules to adsorption sites. This increase in polymer mobility with RH level is not limited to our chosen sorbent but has also been observed in  $PEI:AI<sub>2</sub>O<sub>3</sub>$ , using fluorescence and NMR characterizations.<sup>16</sup> 10

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These differing  $R_2$  experiments have been tailored to observe the system of interest from different perspectives. The low magnetic field measurement is highly sensitive to protons in water while it is less sensitive to protons in sorbent. To complement a low signal-to-noise ratio with  $D_2O$  measurement at low magnetic field, the experiments at high magnetic fields are conducted to probe the signal directly from the sorbent itself. 15  $20$ 

Spin–lattice relaxation serves as a further guide to understanding how water interacts with the adsorption properties of Lewatit® VP OC 1065 during water adsorption. Here, we choose to use proton NMR spin–lattice relaxation rates in the rotating frame  $(R_{1\rho}={T_{1\rho}}^{-1})$ , measured under a spin-lock field  $(B_{\rm sl})$ . This measurement is chosen because it allows to detect bound water motion at mid-kHz range.<sup>45</sup> For very slow motion ( $\omega_1 \tau_c \gg 1$ ),  $R_{10}$  is inversely proportional to correlation time. Specifically, faster motion with shorter correlation time increases  $R_{1\rho}$ (shorter  $T_{10}$  relaxation times) as given by BPP theory. Fig. 8 isolates humidity effects on the relaxation mechanisms using only  $N_2$  and  $D_2O$  (or  $H_2O$ ). The bound water motion is observed in Fig. 8b, showing a pronounced increase in  $R_{10}$  with increasing humidity when using  $H_2O$ , whereas  $R_{1\rho}$  remains unchanged when using  $D_2O$  (as presented in Fig. 8a). 25 30 35



Fig. 6 Changes in transverse relaxation rates ( $R_2^{-1}$  =  $T_2$ ) of water saturated within material, measured at a resonant <sup>1</sup>H frequency of 13.11 MHz. (a)  $R_2$  distribution interpreted as pore-confined H<sub>2</sub>O (faster R<sub>2</sub>, i.e. shorter T<sub>2</sub>) and free H<sub>2</sub>O (slower R<sub>2</sub>, i.e. longer T<sub>2</sub>); (b) magnified view of (a), highlighting the changing  $R_2$  distribution of pore-confined H<sub>2</sub>O. Dashed black and solid red lines are a guide to the eye.



Fig. 7  $1 + 1$  MMR relaxation decay curves obtained at 9.4 T of activated and water vapor (including N2, using either (a) D2O or (b) H2O) adsorbed materials at 25 °C with RH30, and RH80 for  $R_2 = (1/T_2)$  relaxations. Considering potential deuterium exchange in polymer, the data presented in D<sub>2</sub>O is used after reactivating D<sub>2</sub>O adsorbed sample in (a). Measurements with activated and RH30 in (b) are overlapped in the graph. 15 15

Consequently, in this slow motional timescale, the higher  $R_{10}$ observed with increased RH level suggests faster water molecular motion. This trend is shown as a steeper slope and persists also in experiments performed with co-adsorption of  $CO<sub>2</sub>$ , where  $R_{10}$  also increases with RH level (see Fig. S7b†). These results suggest that bound water motion is also "lubricated" by increased relative humidity.

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Further, at 30% RH, the relaxation measurements of  $R_{10}$  and  $R<sub>2</sub>$  reveal different response to the faster correlation time of water molecular motion. While the faster correlation time affects  $R_{1\rho}$  as depicted in Fig. 8b,  $R_2$  shows minimal change even under conditions where  $H<sub>2</sub>O$  contributes to relaxation in Fig. 7b. This demonstrates that motion of bound water adsorbed at 30% RH is sensitively detected by  $R_{1\rho}$ , and reflects changes in the correlation times for local water motion at millisecond timescales (kilohertz frequencies); however, it is hardly detected by  $R_2$ , which can detect microsecond (MHz) frequencies and zero-frequency. Thus, this lack of influence on  $R<sub>2</sub>$  can imply that the water adsorbed at up to 30% RH is tightly bound to the sorbent or includes a few additional layers of water, which do not significantly affect  $R_2$  measurements. The water protons in both scenarios may not have sufficient 30 35 40

freedom to contribute to  $R_2$  relaxation. Therefore,  $R_{10}$  is more effective than  $R_2$  in discerning motion of bound water at this humidity level. 20

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As RH level increases from 30% RH to 80% RH, it is important to note that  $R_2$  begins to respond to faster correlation times, becoming sensitive to changes in water molecular motion. A less steep slope in Fig. 7b indicates a noticeable reduction in the  $R_2$  relaxation rate, alongside an increase in  $R_{10}$ shown by a steeper slope (Fig. 8b). Both relaxation rates reflect a response to the faster motional correlation time, consistent with enhanced molecular mobility due to the adsorption of additional water molecules. This suggests that the water adsorption extends beyond the tightly bound state, which  $R_2$ cannot clearly detect at 30% RH, and likely involves multiple layer adsorption and potentially progressing to capillary water condensation, yielding increased mobility. For the sorbents exposed at 80% RH with  $CO<sub>2</sub>$ , a consistent trend is observed where  $R_{10}$  increases and  $R_2$  decreases as RH level rises (see Fig. S7†). Furthermore, this enhanced water adsorption at 80% RH is corroborated by the well-resolved and intense signal around 4.5 ppm attributed to bulk water in Fig. 4a. This increased water content within pores may block potential  $CO<sub>2</sub>$ 25 30 35 40



Fig. 8<sup>1</sup>H NMR relaxation decay curves obtained at 9.4 T of activated and water vapor (including N2, using either (a) D2O or (b) H2O) adsorbed materials at 25 °C with RH30, andRH80 for  $R_{1r}$ (=1/T<sub>1r</sub>) relaxations. Considering potential deuterium exchange in polymer, the data presented in  $D_2O$  is used after reactivating  $D_2O$  adsorbed sample in (a).

adsorption sites or pathways, thereby impeding  $CO<sub>2</sub>$  adsorption at 80% RH. This observation aligns with the general trend of increased water sorption at high RH levels,<sup>36,47</sup> where water sorption escalates from monolayer to multilayer, and eventually leading to capillary condensation of water molecules.<sup>47</sup> Furthermore, a similar transition from enhanced adsorptive to competitive behavior with increasing RH has also been observed in other studies using FTIR. Indeed, FTIR study on polyimide covalent organic frameworks further has identified peaks corresponding to water uptake at varying RH levels and highlighting water molecules readily occupy adsorption sites, suggesting a strong affinity for water adsorption at higher RH values (around 38–42% RH) in  $H_2O$ –CO<sub>2</sub> adsorption.<sup>36</sup> 10

We conclude that increasing RH induces pore swelling, concomitant with a significant increase in water adsorption. This leads to a complex interplay between  $CO<sub>2</sub>$  and  $H<sub>2</sub>O$ adsorption, impacting adsorption capacity. This corroborates the dominant  $CO_2$  adsorption over  $H_2O$  adsorption at 30% RH, as observed in the enhanced  $CO<sub>2</sub>$  uptake in both the isotherm experiment and NMR experiment.<sup>25</sup> At 30% RH, when only tightly bound water adsorption or only a few more layers may compete with  $CO<sub>2</sub>$  in the swollen pores, the  $CO<sub>2</sub>$  adsorption capacity is enhanced. Conversely, at 80% RH, the substantial amount of water adsorption likely attracts more water and reduces  $CO<sub>2</sub>$  adsorption capacity despite the expanded pores within the sorbent. Finally, lubrication of molecular motion for both the polymer and bound water occurs with increasing RH exposure. 15 20 25

### **Conclusions**

The  $CO<sub>2</sub>$  adsorption behavior in polymer resin Lewatit® VP OC 1065 for DAC applications was investigated using solid-state NMR. The  $CO<sub>2</sub>$  partial pressure and the relative humidity were found to be key factors influencing the sorption. In the absence of water, the effect of  $CO<sub>2</sub>$  partial pressure on both chemisorption and physisorption processes highlights a stepwise process characterized by the sequential formation of ammonium carbamate, carbamic acid, and ultimately physisorption, all contingent upon the  $CO<sub>2</sub>$  loading levels. Additionally, the relative humidity at low  $CO<sub>2</sub>$  loadings influences total  $CO<sub>2</sub>$  sorption, with increased sorption capacity at 30% RH, and decreased  $CO<sub>2</sub>$ sorption capacity at 80% RH. At the low  $CO<sub>2</sub>$  partial pressures, however, we found that the RH does not change the  $CO_2$ -amine binding mechanism, even while changing the overall  $CO<sub>2</sub>$ uptake; this is in contrast with previous studies theorizing the formation of bicarbonate species thereby improving the stoichiometry. Bicarbonate is not observed in any of the experiments undertaken here.

Instead, we found that the impact of water on  $CO<sub>2</sub>$  uptake is accounted for by considering the molecular dynamics of water and the surrounding sorbent polymer induced by water adsorption. We assert that the adsorption of water into the pores leads to pore expansion over time, opening migration pathways and thereby increasing the availability of  $CO<sub>2</sub>$  sorption sites  $(i.e.,$  amino groups). The specific RH levels affect the extent of pore expansion and local water molecular motion. Two

distinct NMR relaxation regimes suggest a transition from water molecules that are tightly bound or form only a few layers on the adsorbate at 30% RH to water molecules that exhibit capillary condensation and include more multilayered structures at 80% RH. This observation likely contributes to variations in  $CO<sub>2</sub>$ adsorption capacity under different RH conditions, with corresponding changes in the relaxation rates.

Our analysis conclusively shows that, in ultra dilute  $CO<sub>2</sub>$ streams, the effect of water on  $CO<sub>2</sub>$  adsorption is not chemical but physical. Specifically, our findings contribute to understanding the underlying water/carbon dioxide co-adsorption phenomena in amine-modified polymer resins. The presence of water induces the pore opening due to polymer swelling and thereby affecting  $CO<sub>2</sub>$  sorption without altering the chemical reaction route. These insights are critical to underpin optimized DAC materials and process designs moving forward. Finally, the experimental framework demonstrated here allows future studies to address the same questions for other amine-modified DAC adsorbents classes. 10 15 20

### Experimental methods

#### Sample preparation and NMR analysis under dry and wet conditions

The sorbent material used in this study, Lewatit® VP OC 1065, underwent activation by heating at 100 °C under ultra-high vacuum ( $\sim$ 10<sup>-3</sup> torr) for several hours before gas adsorption. Subsequently, the activated samples were subjected to both dry and wet conditions.

For dry adsorption experiments, the activated samples in the packed rotor were subjected to varying partial pressures of  ${}^{13}CO_2$  (Sigma-Aldrich carbon- ${}^{13}C$  dioxide <3 atom%  ${}^{18}O$ , 99.0 atom%  $^{13}$ C) using a home-built *ex situ* dry gas apparatus. The partial pressures used were 8, 35, and approximately 1000 mbar, and each adsorption lasted for one hour. NMR experiments for the dry gas adsorbed samples were carried out at  $11.75$  T using a Bruker 4 mm dual-channel CPMAS probe.  $^{13}$ C MAS NMR spectra were acquired at room temperature with a MAS rate of 10 kHz. The <sup>1</sup>H  $\rightarrow$  <sup>13</sup>C cross-polarization (CP) transfer under MAS (CPMAS) experiments were obtained with a contact time of  $\tau_{CP} = 2$  ms, during which a constant RF-field equal to 52 kHz was applied on the  $^{13}$ C, while the  $^{1}$ H RF-field amplitude was linearly ramped from 30 to 59 kHz. During  $^{13}$ C acquisition, high-power  ${}^{1}H$  decoupling was applied using the two-pulse phase-modulated (tppm15) decoupling scheme with an RF field amplitude set to 50 kHz.<sup>48</sup> A total of 128-2k transients were averaged with a repetition time of 2 s. 35 40 45

The 2D <sup>1</sup>H-<sup>13</sup>C CP-based heteronuclear correlation (CP-HETCOR) spectra were acquired using a contact time of 50  $\mu$ s and 70 kHz of on-resonance frequency switched Lee-Goldberg (FSLG) homonuclear decoupling during the  $t_1$  evolution period.<sup>49</sup> During <sup>13</sup>C acquisition, high-power <sup>1</sup>H decoupling was applied using the tppm 15 decoupling scheme with an RF-field amplitude set to 50 kHz. In total, 80  $t_1$  increments were recorded ( $\Delta t = 26.95$  µs), each made of 200 transients with a repetition time of 2 s, leading to an overall experimental time of ∼9 hours. 50 55

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Direct excitation carbon spectra were acquired using highpower <sup>1</sup>H decoupling was applied using the tppm 15 decoupling scheme with an RF-field amplitude set to 25-50 kHz. They were employed to probe physiosorbed  $CO<sub>2</sub>$  and quantify carbon in the adsorbed samples with a recycle delay of 2 s and 120 s with 16–2k and 256 transients, respectively. The chemical shift anisotropy (CSA) tensors were estimated from the low-speed MAS <sup>13</sup>C spectra collected at a MAS rate of 3 kHz with a recycle delay of 120 s. The spectral deconvolutions were performed using Dmfit software.<sup>50</sup>

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Under humid conditions at a controlled low partial pressure of  $CO<sub>2</sub>$ , the activated samples were loaded into an ex situ coadsorption apparatus, where the partial pressure of  $^{13}CO_2$  in the gas mixture and the amount of  $H_2O$  vapor precisely controlled by manipulating their flow rates. Relative humidity (RH) levels of 0%, 30%, and 80% were explored, with each adsorption lasting 3–4 hours. NMR experiments discussed for the humid gas adsorbed samples were conducted at 9.4 T, monitoring at a MAS rate of 10 kHz using a Bruker 3.2 mm probe. A rotor-synchronized DEPTH pulse was employed to suppress background  ${}^{1}H$  signals.<sup>51</sup> <sup>13</sup>C CPMAS spectra were measured with a contact time of  $\tau_{\text{CP}} = 0.2$  ms, during which a constant RF-field equal to 61 kHz was applied on the  $^{13}C$ , while the  ${}^{1}$ H RF-field amplitude was linearly ramped from 71 to 89 kHz. During  $^{13}$ C acquisition, high-power  $^{1}$ H decoupling was applied using Small Phase Incremental Alternation with 64 steps (SPINAL-64) decoupling scheme with an RF-field amplitude set to 89 kHz.<sup>52</sup> A total of 2k–4k transients were averaged with a repetition time of 1.5–2 s resulting in experimental times of 1–2 hours. Carbon quantification was accomplished by direct excitation with SPINAL-64 decoupling scheme set to 89 kHz. A total of 160 transients were averaged with a recycle delay of 140 s resulting into 6 hours and 13 min experimental time. Additionally, 2D  $^{1}$ H- $^{13}$ C HETCOR spectra were recorded with a contact time of 200 µs during the CP transfer and FSLG of around 89 kHz during <sup>1</sup>H evolution period while keeping the rest of CP parameters. In total, 64 $t_1$  increments were recorded  $(\Delta t = 44.8625 \,\mu s)$ , each made of 16-512 transients with a repetition time of 1.5–2 s resulting in experimental times of 0.5–12 hours. 15 20 25 30 35 40

For all 2D HETCOR spectra under dry and wet conditions, proton chemical shifts were referenced by  ${}^{1}H-{}^{1}H$  FSLG pulse sequence immediately after acquiring the 2D HETCOR without altering any parameters.<sup>53</sup> Short cross-polarization contact times (50  $\mu$ s) were used throughout this work to emphasize carbon-13 peaks proximate to protons, albeit at a signicant loss of signal-to-noise. For 2D HETCOR experiments dosed at 150 ppm  $CO<sub>2</sub>$ , the contact time was increased to 200  $\mu$ s to improve sensitivity.

 $R_2$  and  $R_{10}$  relaxation measurements at 9.4 T were performed at room temperature.  $R_2$  relaxation was conducted by using a rotor synchronized spin-echo pulse sequence with a spinning rate of 20 kHz. Echo time were varied from 100 μs up to around 10 ms with a time interval of 100 to 200  $\mu$ s.  $R_{1\rho}$  relaxation measured at a MAS rate of 10 kHz was collected with the sequence consisting of 90° excitation pulse followed with a spin-locking time (TSL) from 50 µs to 20 ms, using 12 to 16

TSL points with a spin-locking field strength of around 84 kHz followed by a rotor-synchronized spin echo detection (using 180° refocusing pulse).

The  $D_2O$  adsorption experiments were conducted to investigate the interaction between deuterium oxide and activated materials, with a specific focus on revealing the molecular dynamics of water and its impact on the sorbent resin. Nitrogen  $(N<sub>2</sub>)$  was chosen as the carrier gas and was directed through a bubbler containing  $D_2O$  to saturate the gas with  $D_2O$  vapor, achieving the targeted relative humidity level. To maintain consistency with parallel experiments conducted under similar humid conditions, the duration of  $D_2O$  exposure was adjusted accordingly, ensuring uniform exposure times across all experiments. 5 10

 ${}^{1}$ H and  ${}^{13}$ C chemical shift were referenced with respect to tetramethylsilane using the  $CH<sub>2</sub>$  resonance of adamantane as a secondary external reference at  $\delta_{\rm iso} \,(^{13}{\rm C})$   $=38.48$  ppm and  $\delta_{\rm iso}$  $({}^{1}H) = 1.8$  ppm. 15

#### Low magnetic field transverse relaxation measurement  $(R_2)$

This experiment aims to measure the swelling of Lewatit® VP OC 1065 in H<sub>2</sub>O using low magnetic field <sup>1</sup>H  $T_2$  relaxation at room temperature. The 0.3 T unilateral magnet NMR-MOUSE (MObile Universal Surface Explorer) PM25 was interfaced to a Magritek Kea II spectrometer to detect transverse relaxation of the polymer over 3 hours, during which time 52 CPMGs were recorded.<sup>54-58</sup> For all experiments,  $\pi/2$  pulse lengths were 2.5 µs and the repetition time for signal averaging was 10 s. A total of 1000 echoes separated by a delay of 55 µs were recorded, and 128 scans were signal averaged. To cancel artifacts arising from pulse imperfections, the initial  $\pi/2$  rf pulse and the receiver were phase cycled between +x and  $-x$  while holding the  $\pi$  rf pulse phase constant at  $+y$ . Inversion of the multiexponential time decay to a distribution of  $R_2$  was accomplished with Laplace inversion using the Lawson and Hanson algorithm in Prospa software v3.61. $59,60$  A smoothing value of 0.9 was chosen by minimizing  $\chi^2$  without oversmoothing. 25 30 35

These experiments detect two significant  $R_2$  relaxation rates, and the shorter  $T_2$  relaxation time is attributed to water imbibed within the porous polymer network. Subsequent observation of the polymer swelling over 24 hours was detected in a similar way. 40

#### Adsorption isotherm experiments and the calculation of the isosteric heat of adsorption

Single and binary component  $CO<sub>2</sub>$  and water isotherms for Lewatit were measured using the DVS Vacuum system from Surface Measurement Systems. The DVS uses a gravimetric magnetic suspension balance to measure the mass of the sample throughout adsorption and desorption. Samples of between 30-60 mg were first outgassed in the DVS at a temperature of 100 °C. A turbomolecular pump was used to achieve pressures of 10−<sup>5</sup> bar and ensure thorough outgassing of the sample prior to adsorption. Once the sample was outgassed and the system was brought down to the adsorption temperature, the pressure of adsorbate was increased stepwise, and the mass

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was allowed to equilibrate before moving to the next pressure step. Desorption branches were similarly obtained by decreasing the pressure in the same stepwise manner. The DVS can operate in dynamic or static mode. Dynamic mode is when the gas/vapour flows through the chamber whereas static mode is when the gas is pulsed into the chamber. Water isotherms were measured using dynamic mode and  $CO<sub>2</sub>$  isotherms were measured using static mode.

Co-adsorption isotherms were measured using semi-static mode. For these measurements, Lewatit was outgassed as above and the first adsorption step pre-adsorbed the sample with water at a determined relative humidity while the following pressure doses were  $CO<sub>2</sub>$ . Working under the assumption that

 $CO<sub>2</sub>$  does not affect water adsorption,<sup>10</sup> subsequent mass increases were attributed to  $CO<sub>2</sub>$  adsorption. Desorption was not performed for co-adsorption experiments as there is

currently no way to differentiate between water and CO2

The isosteric heat of adsorption was calculated using the<sub>3 R. Bergman and A. Anatoly, *The Case for Carbon Dioxide*</sub> Clausius–Clapeyron equation. The heat of adsorption across 20

many different  $CO<sub>2</sub>$  loadings was obtained by interpolating the isotherms.

#### Data availability 25

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All data supporting the findings of this study are available within the main article and the electronic ESI.† All raw NMR data have been deposited on Dryad at https://doi.org/10.5061/ dryad.h70rxwdsx.

### Author contributions

A. S. conceived and designed the research, conducted experiments and analysis, and wrote the original draft. J. Y. performed the measurement of adsorption isotherms and participated in discussion. J. W. and S. N. F. conducted  $R_2$  measurements at low magnetic field and analyzed the data. K. P., S. G., and M. v. S. participated in discussions and offered valuable comments and experimental analyses. R. G. assisted with setting NMR pulses and participated in discussion. All authors edited the manuscript. J. A. R. supervised the research.

## Conflicts of interest

There are no conflicts to declare.

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Protection of the Environment to RMI's climate tech accelerator

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