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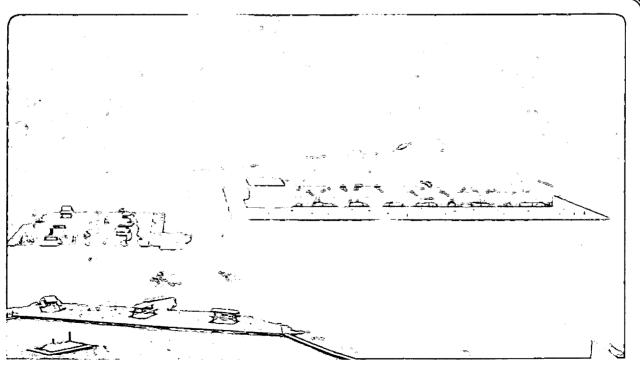
CATALYTIC GASIFICATION OF GRAPHITE OR CARBON Quarterly Report: October 1 - December 31, 1984

H. Heinemann

December 1984

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Quarterly Report

October 1 - December 31, 1984

CATALYTIC GASIFICATION OF GRAPHITE OR CARBON

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I. TASK DESCRIPTION FOR FY 1985

This program is designed to look at the basic chemistry of the reaction of carbonaceous materials with water in the presence of catalysts to produce hydrocarbons and/or synthesis gas. Much of the work is being carried out with graphite as a carbon source to insure that hydrogen or hydrogen in hydrocarbons is derived from water. Relatively low temperatures are being used to favor the equilibrium $C+2H_2O \rightarrow CH_4+CO_2$, which is almost thermally neutral. Our earlier work has shown that, in the presence of KOH as catalyst, higher hydrocarbons up to C_6 can be formed. This raises the question whether hydrocarbons are a primary product and syngas a secondary one formed by steam reforming. The formation of hydrocarbons is a stoichiometric reaction in which each ${\rm H_2}$ in water reacts to form a phenolate and a hydrocarbon: $5C+4KOH \rightarrow 4COK+CH_{1}$. We have shown the presence of phenolate by surface spectroscopy and have found that it can be decomposed over metal oxides to make the reaction truly catalytic: $4COK \xrightarrow{MeOx} 2K_2O+2C+2CO$; $2K_2O+2H_2O$ 4KOH. Future work is directed toward combining flow reactor studies with ultrahigh vacuum surface studies to follow the mechanism, to find the best catalysts for phenolate decomposition, to measure and improve kinetics, and to study the effect of added gases, such as CO or COS.

II. HIGHLIGHTS

Adsorption experiments with CO or ${\rm CO_2}$ on graphite using labelled carbon have shown an exchange of carbon between graphite and CO at very high temperatures, but not between graphite and ${\rm CO_2}$. Since ${\rm ^{13}CO_2}$ is desorbed from adsorbed ${\rm ^{13}CO}$ at 730K (437°C) and below, it must be formed by disproportionation, leaving some carbon on the graphite surface.

In the gasification of graphite over KOH/NiO catalysts at 860K (567°C) more hydrogen and less CO and methane are observed than corresponds to equilibrium. CO_2 is a major product along with hydrogen. To determine whether methane is a major primary product which is then decomposed by steam reforming, methane was added to the steam feed. The vast majority (95+%) of the added methane was recovered in the product, showing that steam reforming plays at most a minor role. However, in the presence of added methane the gasification rate declined. While the reasons for this are not yet clear, they must lie in a surface poisoning by some decomposition product of the small amounts of methane disappearance.

III. PROGRESS OF STUDIES

A. Thermal desorption of 13 CO and 13 CO $_2$ from graphite at low pressures.

Thermal desorption experiments using 13 C labelled 13 CO and 13 CO $_2$ were carried out from the clean graphite surface to determine the nature of the intermediates formed on the surface when either of these two gases is adsorbed. Adsorption of either CO or CO $_2$ on polycrystalline graphite followed by heating at a rate of 5°/sec, gives rise to CO $_2$ desorption at 730K and CO desorption at 1250K. In order to determine if the carbon in the desorbed gaseous molecules is derived from graphite or from the adsorbed gases, labelled 13 CO and 13 CO $_2$ were used. The results indicate that regardless of whether 13 CO or 13 CO $_2$ was adsorbed, CO $_2$ desorbed at 730K contained only 13 C and therefore the carbon in desorbing CO $_2$ comes from the adsorbed gas. Thus, we have clear evidence for the disproportionation of adsorbed CO on clean graphite according to the Boudouard reaction,

$$2CO(ads) \rightarrow C + CO_2(g)$$

CO desorbed at 1230K contained only 12 C and therefore, must derive from graphite. It appears that the oxygen atom produced from the dissociation of adsorbed 13 CO or 13 CO₂ can also react with the graphitic

carbon to produce a strongly adsorbed species that desorbs as CO only at high temperatures, such as 1230K.

B. Catalytic studies of the graphite-steam reaction using a flow reactor.

We have found that a combination of KOH and NiO is a good catalyst for the gasification of graphite with steam in the temperature range of 730-950K. With KOH alone the reaction was stoichiometric below 850K and stopped after one turnover. With KOH/NiO catalyst $\rm H_2$ and $\rm CO_2$ were the major products and their yield and concentration are displayed in Figure 1A. $\rm CH_4$ and $\rm CO$ are also produced but in small amounts.

The dominant net reaction appears to be

$$C + 2H_2O \xrightarrow{NiO/KOH} 2H_2(gas) + CO_2(gas)$$

The formation of $\mathrm{CO}_2(\mathrm{gas})$ instead of $\mathrm{CO}(\mathrm{gas})$ can be readily explained using the results of our CO thermal desorption studies that indicate that it disproportionates to C and CO_2 . If CO formation is the first step in the $\mathrm{C/H}_2\mathrm{O}$ reaction (along with H_2 formation), followed by its disproportionation, only CO_2 will be detected. It is interesting that gas production is detected only above the desorption temperature of CO_2 , 730K. The possibility that CO is converted to CO_2 by the watergas shift reaction cannot fully be excluded at this time.

During the catalyzed ${\rm C/H_2O}$ reaction more hydrogen is detected than

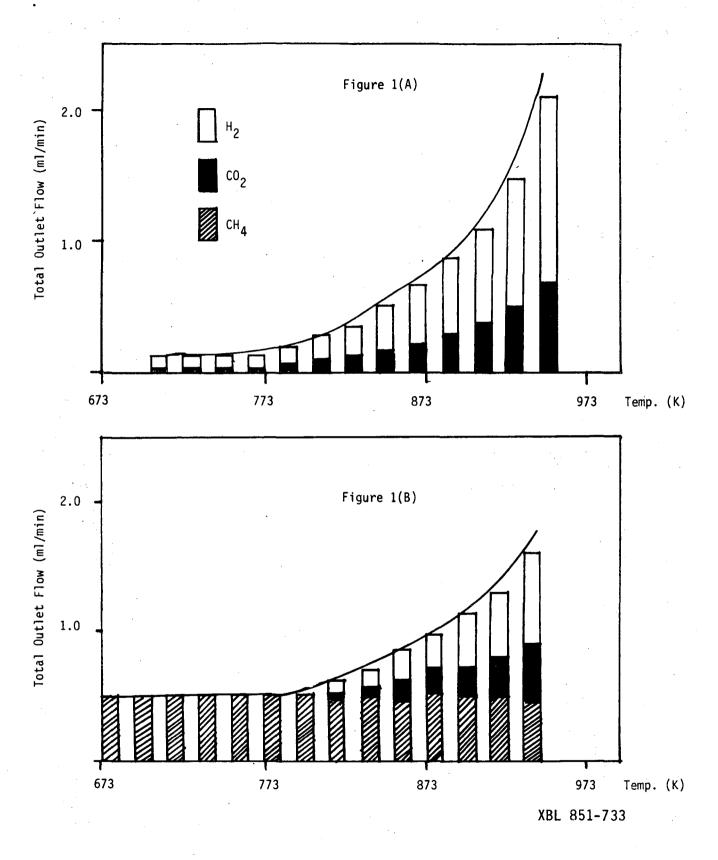
indicated by the stoichiometry of the net reaction (C + $2H_2O \rightarrow CO_2$ + It was thought that if CH_4 is also produced, which is thermodynamically certainly feasible at the low temperatures (2C + $2H_2O \rightarrow CH_4 + CO_2$), its reactions with steam ($CH_4 + CO_2$) ${\rm H_20} \rightarrow {\rm 3H_2} + {\rm CO}$) could account for the increased amount of hydrogen. In order to obtain evidence for the presence of methane steam reforming, CH_{Δ} was mixed with steam and the mixture was passed over graphite at a flow rate of 0.5 ml/min. in the presence of KOH/NiO catalyst. results are shown in Figure 1B. The addition of CH_4 decreases the rate of gas production by a factor of two while only a small fraction (1-5%)seems to react with steam. The inhibition of gas production (${\rm H_2}$ and CO_2) by CH_4 may be due to the deposition of carbon from the disproportionation of CO that has been produced by the $\mathrm{CH_{\Delta}}$ + $\mathrm{H_{2}O}$ While only a small fraction of the methane that was introduced reacted, this reaction could account for the observed larger than 2:1 H_2 :CO ratio which was detected in the catalyzed C/ H_2 O reaction.

In order to carry out the steam gasification of graphite in the presence of $\mathrm{CH_4}$ (or other gases), a time consuming modification of the flow reactor had to be undertaken. Work is now in progress studying the effect of added CO and/or $\mathrm{CO_2}$ on steam gasification of graphite.

Figure Captions

Figure 1A: Total outlet flow when passing steam over a graphite sample loaded with .4% KOH and .4% NiO. Charge rate 1 ml water/min.

Figure 1B: Total outlet flow when passing steam and methane over a graphite sample loaded with .4% KOH and .4% NiO. Charge rate 1 ml water/min. Steam/methane ratio = 2.



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