Predicting the metabolic capabilities of *Synechococcus elongatus* PCC 7942 adapted to different light regimes

Jared T. Broddrick^{a,b}, David G. Welkie^a, Denis Jallet^{c,1}, Susan S. Golden^a, Graham Peers^c, and Bernhard O. Palsson^{b,†}

^aDivision of Biological Sciences, University of California, San Diego, La Jolla, CA, USA, ^bDepartment of Bioengineering, University of California, San Diego, La Jolla, CA, USA, ^cDepartment of Biology, Colorado State University, Fort Collins, CO, USA

ABSTRACT

There is great interest in engineering photoautotrophic metabolism to generate bioproducts of societal importance. Despite the success in employing genome-scale modeling coupled with flux balance analysis to engineer heterotrophic metabolism, the lack of proper constraints necessary to generate biologically realistic predictions has hindered broad application of this methodology to phototrophic metabolism. Here we describe a methodology for constraining genome-scale models of photoautotrophy in the cyanobacteria *Synechococcus elongatus* PCC 7942. Experimental photophysiology parameters coupled to genome-scale flux balance analysis resulted in accurate predictions of growth rates and metabolic reaction fluxes at low and high light conditions. Additionally, by constraining photon uptake fluxes, we characterize the metabolic cost of excess excitation energy. The predicted energy fluxes are consistent with known light-adapted phenotypes in cyanobacteria. Finally, we leverage the modeling framework to characterize existing photoautotrophic and photomixtotrophic engineering strategies for 2,3-butanediol production in *S. elongatus*. This methodology, applicable to genome-scale modeling of all phototrophic microorganisms, can facilitate the use of flux balance analysis in the engineering of light-driven metabolism.

19

20

21

24

25

29

30

31

33

34

36

37

39

40

41

42

1. INTRODUCTION

There is significant interest in engineering light-driven metabolism towards the production of fuels and chemicals. Cyanobacteria represent the simplest phototrophs and have been employed to produce a variety of products [38]. Synechococcus elongatus PCC 7942 (hereafter, S. elongatus), a genetically tractable obligate phototroph, has been engineered for the production of a wide variety of chemicals to include 3-hydroxypropinoate [24], succinate [25], and 1,3-propanediol [13]. Despite its classification as an obligate pho-10 totroph, this organism has also been engineered for mixotrophic 11 metabolism, using carbon sources such as glycerol [16] and glu-12 cose [17] to generate bioproducts of interest. While experimental 13 and computational fluxomics have been central to effective engi-14 neering of heterotrophic organisms [2, 19], their application to the 15 engineering of phototrophic metabolism has been limited. 16

Fluxomics contributes to metabolic engineering by identifying
 the resource partitioning through a metabolic network. Reaction

⁺Corresponding author: palsson@ucsd.edu

fluxes are determined experimentally via ¹³C metabolic flux analysis (MFA), or computationally using methods such as flux balance analysis (FBA) [39]. Recent developments in ¹³C MFA have resulted in characterization of photoautotrophic metabolic fluxes [51] and the engineering of cyanobacteria such as *S. elongatus* [15]. Flux balance analysis coupled with genome-scale modeling (GEM) has a long history of facilitating bioprocess design [18], and has the potential to advance the engineering of phototrophic metabolism [27]. Still, despite the availability of several phototrophic GEMs [11], there are few examples of GEMs being employed in the design of light-driven metabolic processes [7].

The potential of a GEM to engineer a metabolic network for bioproduction depends on its ability to accurately predict flux through the network. Simple constraints such as the glucose and oxygen uptake rate result in accurate assessments of heterotrophic reaction fluxes [29]. The ability to define the metabolic flux state with as few parameters as possible requires a mechanistic understanding of the governing constraints on the system. Recent modeling in *S. elongatus* resulted in accurate prediction of photoautotrophic growth through photophysiology constraints [6]. In this study, a mechanistic description of photon uptake coupled with constraints on oxygen evolution resulted in accurate predictions of photoautotrophic growth to include the transition to a linear growth curve as a result of self-shading. With the recent publication of ¹³C MFA

KEYWORDS

cyanobacteria, photosynthesis, Synechococcus elongatus, flux balance analysis, constraint based modeling, genome scale modeling

Manuscript compiled: Friday 19th October, 2018

¹ Present address: LISBP, Université de Toulouse, CNRS, INRA, INSA (LISBP-INSA

Toulouse), 135 Avenue de Rangueil, 31077 Toulouse, France

reaction fluxes for S. elongatus [15, 1], it is possible to assess the 100 43 ability of photophysiology constraints to characterize photoau-44 101 totrophic metabolism. 45 102

GEMs can also quantify alternative electron transport (AET) 103 within the metabolic network. Photosynthetic organisms absorb 104 47 light in excess of basic biomass and maintenance requirements. A 105 48 fraction of this excitation energy is dissipated upstream of the pho-106 49 tosystem as fluorescence, heat or other non-radiative dissipation 107 50 mechanisms [45]. The remaining fraction is directed to through 51 108 the photosynthetic apparatus and generates the reductant and 52 109 chemical energy necessary for growth. Excitation energy in excess 53 of growth requirements is quenched via various alternative elec-54 tron transport pathways [26]. AET has been shown to constitute 55 up to 40% of the total linear electron flux through the photosys-113 56 tems in cyanobacteria [12]. Characterizing and quantifying AET 57 114 can facilitate engineering strategies that divert these electrons to 115 58 bioproducts.

In this study we show constraining a GEM of *S. elongatus* with 60 the photon uptake rate derived from whole-cell absorbance and 61 the net oxygen evolution rate results in accurate predictions of 116 62 metabolic fluxes. First, we generate the necessary constraints from 63 the photophysiology of S. elongatus acclimated to two light intensi-64 ties differing by an order of magnitude. Next, we incorporate these 65 constraints with the GEM to predict growth rates at the two cul-66 ture conditions. The resulting metabolic reaction fluxes predicted 67 120 by the model showed good agreement with the experimental ¹³C 121 MFA results. We then use the GEM to assess alternate energy flows 122 in *S. elongatus*, quantifying excess light energy captured by the system. Finally, we use the modeling framework to characterize 71 124 existing engineering strategies for 2,3-butanediol production in S. 72 elongatus. Overall we present the governing constraints of pho-73 toautotrophic metabolism, obtained by experimentally accessible 74 127 protocols, that result in accurate prediction of photoautotrophic 75 128 metabolic reaction fluxes. This methodology, applicable to genome-129 77 scale modeling of all phototrophic microorganisms, can facilitate 130 the use of flux balance analysis in the engineering of light-driven 78 131 metabolism. 79 132

2. MATERIALS AND METHODS 80

2.1 Culture conditions.

Synechococcus elongatus PCC 7942 wild type, stored in our labora-138 82 tory;s culture collection as AMC06, was cultured at 30°C in 400 ¹³⁹ 83 mL BG-11 medium in 1 L Roux flasks. Flasks were bubbled with 140 air under continuous illumination in a temperature controlled in- 141 cubator. Cultures were light acclimated (low light (n=3) at 60 μ mol 142 photons m⁻² s⁻¹, high light (n=4) at 600 μ mol photons m⁻² s⁻¹) for 87 72 hours, diluted and grown until mid-exponential phase before 143 88 144

being harvested. 89

2.2 Cell physiology measurements. 90

Cell densities were manually determined using an improved 91 148 Neubauer hemocytometer. Growth rates were determined based 149 92 on the change in cell counts from inoculation to harvest. Cell dry 93 150 weight was determined by taking 50 mL of culture (n=3) and fil-94 tering it onto a GF/C glass microfiber filter (diameter: 47mm). 152 95 Filters containing cellular biomass and media controls (n=3) were 153 96 dried at 95°C overnight. Cellular dry weight was determined by 154 97 subtracting the post-filtration mass from the pre-filtration mass, 98 155 after normalizing to the media control.

2.3 Determination of cell dimensions.

For imaging, thin pads of 1% (wt/vol) agarose were prepared using Mini-PROTEAN® Tetra Cell Casting Module. From this gel, 1-2 cm square pads were cut and placed onto a microscope slide and 2-5 ul cell culture liquid was added to the pad and let dry. Then a microscope slide cover was gently placed onto of the agarose pad and cells were imaged using a DeltaVision inverted epifluorescence microscope (Applied Precision, Issaquah, WA). Images were captured using a CoolSnap HD charge-coupled device (CCD) camera (Photometrics, Tucson, AZ). Cell length and width were determined using the straight line tool in ImageJ [44]. For high light (n=210) and low light (n=238) acclimated cells the mean and standard deviation were determined and the mean ± 2 standard deviations was used to determine cell volume by modeling the cell shape as a core cylinder capped with two hemispheres according to the following equation:

$$Vol = \pi \left(\frac{w}{2}\right)^2 \left(l - \frac{w}{2}\right) + \frac{4}{3}\pi \left(\frac{w}{2}\right)^3 \tag{1}$$

Where *l* is the cell length and *w* is the cell width.

2.4 Pigment extraction.

133

134

135

136

137

145

146

147

156

Cells (4 mL culture) were collected by centrifugation at 10,000 x g at 5°C for 15 minutes. The supernatant was discarded and the cell pellet was frozen at -80°C until processed. Chlorophyll was extracted with 50 μ L DMSO and 1950 μ L of methanol, incubated in the dark for 30 minutes, and centrifuged at 10,000 x g at 5°C for 15 minutes. The pigment containing supernatant was transferred to a 1 cm path length cuvette. Absorbance spectra were collected used a Cary 60 UV-Vis Agilent spectrophotometer in scan mode (350-800 nm, scan interval of 1 nm). Chlorophyll concentrations were determined using the equations for the appropriate solvent [42].

Phycobilisomes were extracted from the thawed cell pellets by resuspension in 2 mL PBS (10 mM phosphate, 150mM NaCl, pH 7.0) with a protease inhibitor (cOmpleteTM, Sigma-Aldrich). Cells were lysed by sonication (Fischer Scientific Sonic Dismembrator 500, 50% power, 8 seconds on, 30 seconds off for 5 cycles) with the tube chilled in an ice bath during lysis to prevent overheating. Microscopic observation of post-sonicated samples indicated a lysis efficiency of over 90%. Lysed samples were centrifuged at 45,000 x g at 5°C for 60 minutes. 200 μ L of the phycobilisome containing supernatant was transferred to a 96 well plate. Absorbance spectra were collected using an Infinite 200 PRO Multiplate Reader (Tecan) spectrophotometer in scan mode (400-750 nm, scan interval of 1 nm). Phycocyanobilin and apophycocyanobilin concentrations were determined using published extinction coefficients [4] after correcting the well plate path length to a 1 cm equivalent.

2.5 Cellular absorption coefficients.

Cellular absorption coefficients were determined based on published protocols [32]. 1 mL of culture volume was added to 9 mL of BG-11 media and cells were collected by vacuum filtration onto a GF/C glass microfiber filter (47 mm diameter). The filter was placed on top of a 96-well plate with a plate cover along with a negative control consisting of a filter through which 10 mL of BG-11 media had passed. Absorbance spectra were collected using a Infinite 200 PRO Multiplate Reader (Tecan) in scan mode (400-750 nm). Spectra from a total of 6 wells per filter were collected, averaged, blank subtracted and normalized to an OD750 value of 0. The wavelength specific absorption coefficient was determined, along with correcting for filter amplification using the coefficients for Synechococcus WH103 in [32], according to the following equation:

$$a_{\lambda} = 2.303 \left(0.301 \left(A_{\lambda} \right) + 0.45 \left(A_{\lambda}^2 \right) \right)$$
(2)

211

212

221

222

223

235

241

242

243

244

245

247

256

257

259

265

266

267

where A_{λ} is the absorbance at a given wavelength. The cell nor-157 213 malized absorption coefficient (a_{cell}^* , units: cm^2 cell⁻¹) and the 158 214 pigment normalized coefficient (a_{pigm}^* , units: cm² μ g⁻¹ pigments) 159 215 were determined by dividing a_{λ} by either the total number of cells 160 216 deposited on the filter or the total pigment mass, respectively, and 161 217 then multiplying the resulting value by the filter area onto which 162 218 the cells were deposited (12.7 cm^2 for the 47 mm diameter GF/C 163 219 filter). 164

2.6 Simultaneous oxygen evolution and chlorophyll fluores-165 cence parameters. 166

Rapid light curves (RLCs) were performed as outlined in [14]. A 167 224 Walz Dual PAM 100 fluorometer in a temperature controlled cus- 225 168 tom cuvette holder and a FireSting Optical Oxygen Meter were 169 used for the simultaneous measurement of chlorophyll fluores-170 cence and oxygen evolution. Approximately 30 mL of culture was 171 removed and cells were pelleted by centrifugation $(3000 \times g, 10)$ 172 minutes at 30°C). Cell pellets were resuspended in fresh media 173 to the target cell density (HL: 5x10⁸ cells mL⁻¹, LL: 2.5x10⁸ cells 174 mL⁻¹) and kept in the dark for 10 minutes prior to analysis. Dark 229 175 230 respiration rates were collected for approximately 10 minutes prior 176 to running RLCs. A red actinic light (635 nm) was used to provide 231 177 a saturating pulse (600 ms, 10,000 μ mol photons m⁻² s⁻¹) for fluo-232 178 rescence measurements. Cells were illuminated for 1 min steps at 233 234 the following increasing intensities (μ mol photons m⁻² s⁻¹): 180

HL: 0, 8, 24, 43, 75, 109, 146, 195, 259, 339, 435, 547, 674, 844, 1033, 181 1565, 2386, 2924 182

LL: 0, 8, 24, 43, 75, 109, 146, 195, 259, 339, 435, 547, 844, 1565, 2386 183 236 The chlorophyll fluorescence parameters Fv/Fm, Y(II), qP and 237 184 NPQ were determined as described [45, 23]. Net oxygen evolution 238 185 rates were normalized to cell count. Shading in the round cuvette 239 186 was accounted for by calculating the attenuation across the cuvette 240 187 path length according the following equation: 188

$$QF_{I_o} = 2 \int_{\lambda=400}^{\lambda=700} \int_{y=0}^{y=r} I_{o_\lambda}(\lambda) - I_{o_\lambda}(\lambda) e^{-a^*_{cell}(\lambda) \cdot c \cdot 2\left(r^2 - y^2\right)^{\frac{1}{2}}} dy \, d\lambda$$
(3)

246 where QF_{I_0} is the quantum flux in μ mol photons m⁻² s⁻¹ at a given 189 PAR value (I_o), λ is the wavelength, $I_{o_{\lambda}}(\lambda)$ is the fraction of the 190 248 PAR at a given wavelength λ , *r* is the radius of the cuvette (0.56 191 249 cm), a_{cell}^* is the wavelength-specific absorption coefficient in cm² 192 250 cell⁻¹, and c is the cell density in cells cm⁻³. QF was converted 193 to μ mol photons cell⁻¹ s⁻¹ by multiplying QF_{L} by the rectangular 194 252 surface area of the cuvette (width = 0.56 cm, height = 1.15 cm), 195 253 converted to m² and dividing by the total number of cells in the 196 254 cuvette. This QF value was used as the independent variable in 197 255 plots of oxygen-based photosynthesis (Po) versus QF. 198

2.7 Genome-scale metabolic modeling. 199

The *S. elongatus* genome-scale model (GEM) *i*[B785 [6] was updated 200 258 to include additional content (Table S1). 201

Simulations were performed in a similar manner to [6]. The 202 260 biomass objective function was updated to account for differences 203 261 in pigments between the low and high light conditions (Table 1). 204 Demand reactions to allow dissipation of excitation energy at PSII 263 205 and PSI were added to assess the minimum quantum requirement 264 206 of biomass production: 207

DM_chla_qy2_c: chla_qy2*_c \rightarrow cholphya_c 208

DM_chla_qy1_c: chla_qy1*_c
$$\rightarrow$$
 cholphya_c

Photoautotrophic growth was simulated for a 12 hour time period broken into 20 minute psuedo-steady-state segments. Light was modeled coming from the side of the flask. The Roux flasks had approximately 375 mL of culture at the time of the experiments which resulted in a light-facing surface area of 80 cm² and a path length of 4.7 cm. At the beginning of each simulation, the appropriate constraints were updated. First, the total biomass in the culture was divided by the cell dry weight to determine the total cells in the culture. Next, the photon uptake rate was determined by dividing the culture into 50 slices along the 4.7 cm path length. These slices were considered thin enough that cell shading was assumed to be negligible. Thus, we used the spectral distribution of photon flux for the given light source at the experimental irradiance $(I_0(\lambda))$, the cell specific spectral absorption coefficient (a_{λ}^*) , and the cell count, to determine the photon uptake flux (I_a) in units of μ mol photons (time interval)⁻¹ using the following equation:

$$I_a = \frac{cell}{SA} \int_{400}^{700} I_0(\lambda) a^*_{cell}(\lambda) d\lambda \tag{4}$$

where *cell* is the total number of cells in the slice and *SA* is the light-facing surface area of the slice. Light attenuated in one slice was removed from $I_0(\lambda)$ for the subsequent slices, accounting for shading along the culture path length. A running total of the absorbed light was used to set the reaction bounds of the photon exchange reactions in the GEM.

The P_O vs. QF curves were fit to a Platt [41] equation for photosynthesis prediction (P), using quantum flux as the independent variable.

$$P = P_{max} (1 - e^{-\frac{\alpha \times QF}{P_{max}}}) e^{-\frac{\beta \times QF}{P_{max}}}$$
(5)

 P_{max} is the maximum photosynthetic rate, α and β are the parameters that describe the initial slope of the curve, and the photoinhibition (if present), respectively. These curves were used to determined the oxygen evolution rate at each slice. The total oxygen evolution across the culture path length was used to set the bounds of the oxygen exchange reaction in the GEM (reaction ID: EX o2 e).

Non-growth associated maintenance (NGAM) was calculated from the experimental dark respiration rate. This value was set as the lower bound for an fictional plastoquinone oxidase (reaction ID: NGAM), which forces a minimal amount of reductant mediated oxygen consumption consistent with the observed dark respiration rate.

The simulation was performed by maximizing the BOF reaction using the parsimonious FBA function [28] as implemented in CO-BRApy [8]. The flux through this reaction is equal to the biomass accumulation in milligrams over the 20 minute time interval. This biomass was added to a running total of the total culture biomass and used to parameterize the next 20 minute simulation interval. All calculations and simulations were performed using in-house scripts developed in IPython [40].

2.8 Comparison with ¹³C isotopically-nonstationary metabolic flux analysis.

For low light simulations, the predicted flux vector from the model simulation was divided by the flux through the RPBCcx model reaction (RubisCO carboxylase) and multiplied by 100. The experimental data was normalized to 100 units of flux through the RUBP + CO2 \rightarrow 3PGA + 3PGA reaction in Supplemental Table A2 for wild type S. elongatus PCC 7942 in [15]. For high light simulations, the same process was applied, except fluxes were normalized to the sum of the CO₂ and bicarbonate exchange fluxes, multiplied by 100, and compared with the experimental fluxes reported in Supplemental Table 5 in [1].

3. RESULTS 268

319 In this study we set out to assess the ability of genome-scale model-269 ing coupled with photophysiology constraints to predict metabolic 270 321 capabilities in *S. elongatus*. To this end, we first collected the neces-271 322 sary physiology data necessary to parameterize the models. This 272 323 resulted in a comprehensive comparison of low versus high light 273 324 acclimated cultures. Next, we integrated these data as constraints 274 325 on the model simulations, comparing model simulations with in 275 vivo growth rates and fluxes. Finally, we assess the alternate en-276 327 ergy flows through the photosystems as a result of the absorption 277 of excess excitation energy. 278

3.1 Photoacclimation of S. elongatus PCC 7942.. 279

S. elongatus was acclimated and cultured at a high light condition 280 of 600 μ mol photons m⁻² s⁻¹ (HL, n=4) and a low light condition of 281 $60 \,\mu$ mol photons m⁻² s⁻¹ (LL, n=3). Specific growth rates were 0.081 334 282 \pm 0.015 and 0.047 \pm 0.004 hr 1 respectively for HL and LL cultures. $^{\scriptscriptstyle 335}$ 283 While cells grown at both light levels had approximately the same 284 cell width (1.2 \pm 0.1 and 1.1 \pm 0.1 μ m at HL and LL respectively), 285 LL cells were significantly longer resulting in a 20% increase in cell 286 volume at LL (Table 1). 287

Table 1 Physiology parameters of S. elongatus acclimated to low and high light.

	Growth rate (h ⁻¹)	Cell volume (μm^3)	pgDW cell ⁻¹
Low Light	0.047 ± 0.004	3.4 ± 0.6	1.3 ± 0.2
High Light	0.081 ± 0.015	2.8 ± 0.3	1.0 ± 0.2

There were significant differences in light harvesting pigments 350 288 as a result of photoacclimation. Total pigments (phycocyanin (PC), 289 351 allophycocyanin (APC) and chlorophyll *a* (chla) at LL were 4.9 fold 290 higher than at HL (Table 2). Chla and APC increased at a similar 291 353 rate (3.4 and 3.8 fold respectively). Almost all chla in *S. elongatus* is contained within the photosystems [48] and APC is a linker 293 pigment-protein complex physically and energetically connecting 356 294 the light harvesting PC with the photosystems. Thus, this increase 295 in chla and APC is likely attributed to an increase in the num- 358 296 ber of PSI and PSII complexes present at LL. The light harvesting 359 297 pigment-protein complex PC increased 5.7 fold at LL compared to 360 298 HL. The larger -fold increase in PC versus APC suggests not only 361 299 did the number of phycobilisomes increase but the rod length of 300 each phycobilisome increased at LL compared to HL. The phyco- $_{\scriptscriptstyle 363}$ 301 bilisomes constituted 28% of the cellular biomass at LL compared 302 364 to 7% at HL. 303

The pigment content and composition of the cell dictates its 366 304 light harvesting capacity. This cell-specific absorption coefficient 367 305 is an important modeling parameter as it determines the photon 368 306 uptake rate and the extent of self-shading that occurs in the culture. 369 307 We compared the cell normalized absorption coefficient (a*_{cell}) and 370 308 the pigment normalized coefficient (a_{pigm}^*) at both light levels (Fig. ₃₇₁ 309 1). LL acclimation resulted in 2.3 times more light absorbed per cell 310 372 than the HL cells, despite the 4.9 fold increase in total pigments. $_{\scriptscriptstyle 373}$ 311 This decrease in light capture efficiency on a per-pigment basis is 312 374 illustrated in the LL to HL a* $_{\rm pigm}$ ratio of approximately 0.5 (Fig. $_{
m 375}$ 313 1B, area under the curve: HL: 7.4 vs LL: 3.6 cm² μ g⁻¹ nm⁻¹). Thus, 376 314 while low light acclimation allowed *S. elongatus* to absorb more 377 315 light per cell, there were diminishing returns with respect to the 378 316 resources needed to harvest the light energy. 317

3.2 Photophysiology of S. elongatus at low and high light. 318

As the GEM requires quantitative incorporation of photophysiology constraints, we converted both the photon uptake and the photosynthesis versus irradiance (P vs. I) curve into a modelcompatible format. The photon uptake rate is derived from the PAR spectrum and the a*_{cell} values. The PAR spectrum is a wavelength density function describing the relative distribution of photons. For example, a red LED exclusively delivers photons in the 600-700 nm range while a white LED distributes the photons over a broader range of wavelengths. The a*_{cell} describes the wavelengthspecific attenuation of light. For example, the cyanobacterial light harvesting pigment phycocyanin preferentially captures orange and red photons and is responsible for the absorption maximum at 620 nm in Fig. 1. Therefore, the intersection of the PAR spectrum and the a^{*}_{cell} describes the cell-specific attenuation of light, which is the photon uptake rate.

326

328

329

330

331

332

333

336

337

338

339

340

341

342

343

344

345

346

347

348

349

352

355

357

365

We simultaneously measured chlorophyll fluorescence parameters and oxygen evolution using a rapid light curve (RLC) protocol [14]. In an improvement over previous photoautotrophic modeling of *S. elongatus* [6], we converted the incident light (photosynthetically available radiation, PAR) to the quanta of light absorbed by the cells (quantum flux, QF). This representation is necessary to convert between light sources of different spectral quality. In the previous study [6], the P vs. I curve was determined with a white LED and the culture light source was a fluorescent lamp. For S. elongatus, these light sources result in similar QF rates. In this study, the oxygen evolution and fluorescence were collected using a red actinic light, while the cells were cultured under fluorescent light. These light sources have dramatically different spectral qualities; thus, necessitating a conversion.

Upon conversion the P vs. I curve becomes a P vs. QF curve and describes the maximum photosynthesis rate as a function of photon uptake. In this study we used oxygen evolution as a proxy for photosynthesis (P_O). While a culture under full diurnal, solar irradiance may experience a wide variety of QF values, constant light cultures only experience a small section of the P_O vs. QF curve. Thus, the only relevant section of the curve is the maximum $QF(QF_{max})$, representative of photon capture rates of cells closest to the light source, and the minimum QF (QF_{min}), representative of the photon capture rate at the point farthest from the light source, attenuated by cell shading. Thus, we report both the maximum $QF(QF_{max})$, representative of photon capture rates of cells closest to the light source, and the mean QF (QF_{mean}), representative of the average photon capture rate across the full path length.

To induce sufficient fluorescence signal, PAM measurements often require high cell densities. The resulting increase in cell shading decreases the quanta of light absorbed across the path length of the sample cuvette. In an improvement over the previous modeling effort [6], we calculated the photon uptake accounting for cuvette shape, path length, cell density and cellular pigmentation [50]. This transformation dramatically affected the calculated oxygen evolution rate at a given photon absorption rate (P_O vs. QF) (Fig. S1).

Po versus QF curves showed the LL acclimated cells had a significantly steeper light limited slope of photosynthesis, α , and a higher maximum photosynthetic rate, P_{max} , compared to HL cultures (Fig 2A). This resulted in similar cell-specific maximum oxygen evolution rates at the experimental QF for the two light levels with the HL PO at QFmax approximately 20% higher than the LL condition (Table 3). Comparing the mean oxygen evolution rates, this difference increases to almost 40%, quantifying the impact of cell shading on culture productivity. When the Po versus

Table 2 Comparison of pigments in S. elongatus acclimated to low and high light.

							Ratios (LL:HL)			
	Chl a (pg/cell)	PC (pg/cell)	APC (pg/cell)	PC:Chl a	APC:Chl a	PC:APC	Total pigments	Chl a	PC	APC
Low light	0.037 ± 0.002	0.29 ± 0.05	0.08 ± 0.02	7.8	2.2	3.6	4.9	3.4	5.7	3.8
High light	0.011 ± 0.000	0.05 ± 0.01	0.02 ± 0.00	4.6	1.9	2.4				



Figure 1 Cell- and pigment-specific absorption coefficients for S. elongatus acclimated to low and high light. (A) Cell-specific absorption coefficient. (B) Pigment-specific absorption coefficient. The pigment mass includes phycocyanin, allophycocyanin and chlorophyll a. Shaded areas represent one standard deviation from the mean (HL n=4, LL n=3).

427

428

QF curves were normalized to gram dry cell weight, the difference 410 380 in mean oxygen evolution rate increased to 75% (Fig. 2B), which is 411 381 similar to the difference in specific growth rate (72%, Table 1). 382

Interpretation of chlorophyll fluorescence measurements in 413 383 cyanobacteria differs from that in algae and higher plants [46, 35]. 414 384 As such, we report the maximum quantum yield of PSII (Fv/Fm), 415 385 the effective quantum yield of PSII as a function of QF (Y(II)), 416 386 and the fraction of open reaction centers (qL) (Table 3 and Fig. 417 387 S2). However, the values were not quantitatively integrated with 418 388 our model simulations. S. elongatus PCC 7942 lacks the orange 419 389 carotenoid protein that confers the blue light activated phycobil- 420 390 isome fluorescence quenching mechanism in cyanobacteria [20] 421 391 and we did not observe non-photochemical quenching (NPQ) in- 422 392 duced fluorescence in either acclimation condition. The effective 393 quantum yield was approximately two-fold higher for the LL accli- 424 394 mated cells (0.33 \pm 0.01 vs. 0.15 \pm 0.01 at LL and HL respectively), ₄₂₅ 395 suggesting an increase in excitation energy diverted to PSI, consis- 426 396 tent with previous observations in cyanobacteria [35]. 397

3.3 Genome-scale modeling of S. elongatus at low and high 429 398 liaht. 399 430

The photophysiology results were translated into modeling con- 431 400 straints to simulate photoautotrophic growth of S. elongatus. The 432 401 a*cell coupled with the experimental PAR intensity and spectral 433 402 quality of the fluorescent light was used to determine the photon 434 403 uptake constraint for the simulations. This uptake value, equiv- 435 404 alent to QF, was used to determine the oxygen evolution rate of 436 405 the culture. This value constrained the oxygen exchange flux for 437 406 the simulations. The biomass objective function (BOF) [9] defines 438 407 which metabolites and in what ratio must be synthesized to gener- 439 408 409 ate the macromolecular cellular components necessary for growth. 440 We updated the BOF to reflect the differences in pigment mass between the two growth conditions prior to performing simulations.

The quality of the model simulations depends on the accuracy of the experimental photophysiology parameters. Thus, we not only simulated growth using the mean values, but also the upper bound (UB) and lower bounds (LB) of the Po vs. QF curves, a^{*}cell and dry cell weight (pg cell⁻¹). As the experimental growth curves are based on cell counts, the dry cell weight converts the biomass accumulation predicted by the model to cell counts; thus, having an impact on the accuracy of the model growth rate predictions.

The model predicted a LL mean growth rate of 0.033 h^{-1} (UB: 0.044, LB: 0.025) compared to an experimental value of 0.047 \pm 0.004 h⁻¹ representing a 30% underestimation by the model (Fig. 3). For the HL condition the model predicted a mean growth rate of 0.051 h⁻¹ (UB: 0.067, LB: 0.039) compared to an experimental value of 0.081 ± 0.015 h⁻¹ representing a 38% underestimation by the model (Fig. 3). While the upper bound of the simulations values approached the range of the experimental observations, the model tended to underestimate the growth rate at both high and low light.

We explored whether or not maintenance energy requirements forced upon the model could explain the growth rate discrepancies. Maintenance energies in phototrophs differs from that of heterotrophs as the energy source, light, is uncoupled from the carbon source, inorganic carbon. Thus, as long as the culture is not light-limited, maintenance energy costs will not affect growth rate.

Growth-associated maintenance (GAM), represented as growthdependent ATP consumption, has been inconsistently applied to phototrophic GEMs. Genome-scale models of the cyanobacterium Synechocystis sp. PCC 6803 include GAM values ranging from 53 to 1.3 mmol ATP gDW⁻¹ h⁻¹ [34, 21]. GAM requirements in our



Figure 2 Oxygen evolution versus quantum flux for *S. elongatus* acclimated to low and high light. (A) Cell-specific P_o versus QF curves. (B) Dry cell weight-specific P_o versus QF curves. Vertical dashed lines represent the maximum quantum flux received by the cultures at the experimental irradiance. Abbreviations. LL: low light, HL: high light, QF: quantum flux.

Table 3 Comparison of photosynthetic rates in *S. elongatus* acclimated to low and high light. The chlorophyll fluorescence parameter qL is reported for QF_{mean}.

							Ratios	Ratios (HL:LL)		
	QFmax*	QF _{mean} *	Pomax [†]	Pomean ⁺	Fv/Fm	qL	Pomax	Pomean	-	
Low Light	2.5x10 ⁻¹¹	1.6x10 ⁻¹¹	$6.6\pm 0.8 {\rm x10^{-13}}$	$4.6\pm 0.5x10^{13}$	0.30	0.93	1.2	1.4		
High Light	1.1x10 ⁻¹⁰	6.0x10 ⁻¹¹	$8.1\pm 0.7 {\rm x10^{-13}}$	$6.3\pm 0.4~{\rm x10^{-13}}$	0.20	0.71				

* µmol photons cell⁻¹ s⁻¹

⁺ μmol O₂ cell⁻¹ s⁻¹

S. elongatus GEM include a growth associated maintenance cost 464 441 of 30 mmol ATP gDW⁻¹ h⁻¹; however, this is a largely arbitrary 465 442 value. Our GEM sets the non-growth associated maintenance 466 443 (NGAM) to the dark respiration rate. This value represents the 467 444 residual reductant-mediated oxygen consumption that is necessary 468 445 to maintain viability in the absence of light. This value varies with 446 the incident irradiance. We observed dark respiration rates of 469 447 0.41 and 0.15 mmol O₂ gDW⁻¹ h⁻¹ for *S. elongatus* at HL and LL $_{470}$ 448 respectively; with a corresponding reductant consumption rate of 449 471 4 mmol electrons per 1 mmol O₂. Finally, there is an NGAM cost 450 472 associated with the repair of the photosystem II (PSII) D1 subunit. 451 This subunit is damaged at a rate proportional to PSII flux [3], is 452 474 independent of growth rate, and incurs an ATP and GTP cost at 453 475 the ribosome to biosynthesize a replacement subunit. 454 476

Upon removing all GAM and NGAM requirements, the growth 477 455 rate was unchanged at LL and HL. Additionally, we quantified the 478 456 energy in excess of growth and maintenance requirements by fixing 479 457 the growth rate at the maximum value and optimizing for either 480 458 an ATP hydrolysis reaction or a plastoquinone-mediated oxygen 481 459 consumption reaction. At LL, an ATP hydrolysis flux of 19 mmol 482 460 ATP gDW⁻¹ h⁻¹ and a respiratory flux of 0.7 mmol electrons gDW⁻¹ 483 461 h⁻¹ could be sustained above and beyond growth and maintenance 484 462 requirements. At HL, these values increased to 122 mmol ATP and 485 463

2.0 mmol electrons gDW⁻¹ h^{-1} , suggesting the cultures are not light limited at either irradiance. Thus, the growth rate discrepancy between our simulations and the observed experimental values was not due to excessive maintenance energy requirements forced on the model.

3.4 Comparison of GEM predicted reaction fluxes with ¹³C MFA.

While growth rate can be inferred from empirical models, genomescale models have the advantage of predicting the flux for all biochemical reactions in the metabolic network. In the case of S. elongatus, constraining the oxygen evolution rate with net P_O, the photon uptake rate with QF and the biomass objective function with the light-condition-specific cellular composition, reaction fluxes are predicted for 861 intracellular reactions. Recent studies have used ¹³C metabolic flux analysis (MFA) to experimentally determine the reaction flux for central metabolism in S. elongatus [15, 1]. We compared our LL condition predicted reaction fluxes with those published for *S. elongatus* at a similar growth rate [15], normalized to 100 units of RubisCO carboxylase flux to account for the slight difference in growth rate. The predicted reaction fluxes, determined using parsimonious FBA (pFBA) [28], showed remarkable similarity to the experimental values (Fig. 4 and Fig. 5A, B). The primary difference was in metabolic fluxes



Figure 3 Experimental versus simulated growth rates for *S. elon*gatus acclimated to low and high light. For experimental values, error bars represent the standard deviation (HL: n=4, LL: n=3). For the simulation values, the error bars represent the model upper and lower bounds of the model predictions based on the error of the experimental inputs. Abbreviations. Exp: experimental, Sim: simulated.

537

538

540

541

542

543

544

545

546

550

555

557

558

559

562

563

564

565

566

567

568

569

570

571

578

surrounding the malate dehydrogenase (MDH); a reaction that 547 486 was inferred from the ¹³C MFA data, but to date the gene responsi-487 ble for catalyzing this reaction is unidentified in *S. elongatus* PCC 549 488 7942 489

We compared our HL predicted reaction fluxes with those pub- 551 490 lished for S. elongatus PCC 7942 at near optimal growth rates [1]. 552 491 Again, pFBA flux predictions showed good agreement with the 492 experimental values (Fig. 6 and Fig. 5C, D). The primary discrep-493 ancies were in the phosphatase reactions in the Calvin-Benson 494 cycle. However, the net flux into and out of these reactions were 495 in agreement. Overall, the GEM flux predictions constrained by 496 photophysiology constraints were consistent with ¹³C MFA results 497 across the range of observed growth rates. 498

Using flux variability analysis (FVA), we explored whether or 499 not alternate optimal solutions existed for the LL and HL models. 500 For both LL and HL conditions, FVA ranges were narrow for all 501 reactions except those connected to an ATP or reductant consum-502 ing reaction (Fig. 5a,c). As discussed above, both conditions have 503 ATP and reductant pools in excess of growth and maintenance 504 requirements. As a result, the FVA ranges for these reactions are 505 wide as the available energy pools can drive flux through these 506 energy consuming reactions. Therefore, the discrepancy in flux 507 predictions are likely a result of the minimization of total flux 508 performed by pFBA. 509

3.5 Predicted excitation energy routes in S. elongatus. 510

The GEM's biomass objective function defines the energetic re- 572 511 quirements for growth down to the metabolite level. Compar- 573 512 ing constrained versus unconstrained photon uptake enabled an 574 513 assessment of excitation energy absorbed in excess of biosynthe- 575 514 sis and maintenance needs. We simulated growth using the up- 576 515 per bound constraints as they more closely recapitulated in vivo 577 516 growth rates and thus, realistic energy needs. 517

At low light, with a QF of $2.0 \times 10^{-11} \mu$ mol photon cell⁻¹ s⁻¹, 579 518 the model where all excess excitation energy can be dissipated 580 519

upstream of the photosystems (unconstrained) predicted only 33% 520 of the excitation energy was necessary to satisfy the electron needs 521 for biomass production and maintenance. We then constrained the 522 photon uptake to account for the entire quanta of absorbed photons. 523 The GEM includes experimentally determined wavelength-specific 524 energy transfer efficiencies [48]. Based on these values and the 525 emission spectra of the growth light, approximately 30% of the 526 QF is lost before reaching the reaction centers. This quanta, along 527 with the biomass and maintenance requirements accounted for 528 529 63% of the absorbed photons. The remaining 37% was consumed by alternative electron transport (AET). At high light, with a QF of 530 $7.5 \times 10^{-11} \,\mu$ mol photon cell⁻¹ s⁻¹, the unconstrained model predicted 531 only 11% of the excitation energy was necessary to satisfy the 532 electron needs for biomass production and maintenance. After 533 accounting for wavelength-specific energy transfer efficiencies, 534 58% of the absorbed QF was consumed by AET. 535

The AET predicted by the model depends on their relative metabolic cost. The simulations predicted relatively high flux through PSI, even at low light. The model includes a basal PSI superoxide generation rate of 1% [49], while PSII includes a D1 repair cost proportional to flux. The model flux predictions preferentially routed excitation energy through PSI since the combined action of superoxide dismutase and catalase detoxifies the ROS to water with no energy input required. Compared to the unconstrained simulation, the constrained simulation predicted an increase in charge recombination at PSII which increases damage to the PSII D1 protein. This damage is mitigated by de novo synthesis of a new protein at a significant ATP/GTP cost at the ribosome. The model predicted increased cyclic electron flow around PSI is required to generate the chemical energy necessary for D1 protein biosynthesis (Table 4). Thus, the D1 repair cost determines both the predicted bifurcation of excitation energy between PSII and PSI and the cyclic electron flow rate, balancing ATP and reductant ratios necessary to satisfy photodamage mitigation and repair mechanisms. A summary of predicted excitation energy routing, D1 repair costs and quantum yields of carbon fixation and oxygen evolution are shown in Table 4.

3.6 Model-driven engineering of 2,3-butanediol production in S. elonaatus.

The chemical precursor (R,R)-2,3-butanediol (23BD) has been sccussfully produced in S. elongatus via both phototrophic [37] and photomixotrophic strategies [31, 17]. We explored the ability of the photophysiology constrained GEM to optimize 23BD production in *S. elongatus*. We added the 23BD biosynthesis pathway to the GEM (Dataset S1) and removed the non-network constraints. These constraints are restrictions on pathway usage and magnitude that were necessary to recapitulate published in vivo gene essentiality data [43, 6]; however, the organism can be engineered to overcome these constraints. The model suggested an optimal solution that uses the phosphoketolase (PKT) pathway to bypass lower glycolysis (Fig. 7b). Previous modeling in S. elongatus also suggested this pathway was optimal; however, based on the essentiality of lower glycolytic enzymes, it was concluded this bypass was not active during photoautotrophic conditions [6]. PKT uses the Calvin-Benson-Bassham (CBB) cycle intermediates frucose-6phosphate (F6P) or xyulose-5-phosphate as substrates. It has been hypothesized the lack of available substrates, due to high CBB flux, may explain the lack of PKT flux. S. elongatus engineered to consume exogenous glucose was shown to have an elevated F6P pool [17]. Thus, hypothesizing an overexpresed PKT pathway could tap into this F6P pool, we performed an in silico comparison



Figure 4 Simulated versus experimental metabolic reaction fluxes for *S. elongatus* at low growth rates. (A) Predicted fluxes at low light by the *S. elongatus* genome-scale model *i*JB792. (B) Experimental reaction fluxes for *S. elongatus* as reported in [15]. Metabolic reactions and metabolites are indicated by their BiGG identifier (bigg.ucsd.edu). Flux values normalized to 100 units of RubisCO carboxylase flux are shown below the reaction abbreviations.

Table 4 Predicted excitation energy flow in *S. elongatus* acclimated to low and high light. Φ_{CO_2} : quantum yield of net carbon fixation, Φ_{O_2} : quantum yield of net oxygen evolution. Abbreviations: ET: energy transfer, PSII: photosystem II, PSI: photosystem I, CEF: cyclic electron flow, CR: charge recombination.

	Fraction of absorbed quanta									State Trai	nsition
	ET loss	PSII	PSI	CEF	PSII CR	PSI/PSII	D1 repair cost ¹	$\Phi_{CO_2}^2$	${\Phi_{O_2}}^2$	PSI:PSII ³	Y(II) ⁴
High light	0.31	0.09	0.60	0.54	0.04	6.7	3.2x10 ⁻¹⁰	0.009	0.010	2.1	2.1
Low light	0.29	0.17	0.54	0.36	0.03	3.2	0.6x10 ⁻¹⁰	0.028	0.031		

¹ µmol ATP cell⁻¹ s⁻¹

² μ mol x μ mol⁻¹ photon

³ (High light PSI/PSII)x(Low light PSI/PSII)⁻¹

⁴ (Low light Y(II))x(High light Y(II))⁻¹



Figure 5 Correlation between simulated and experimental metabolic reaction fluxes for S. elongatus. (A) Comparison of low light predicted fluxes (gray bars) and experimental fluxes (white bars) reported in [15]. Flux ranges determined by flux variability analysis are shown for the predicted fluxes. Upper bounds that exceed the Y-axis scale are indicated by an arrow and the upper bound flux value. (B) Correlation between low light predicted fluxes and experimental fluxes reported in [15]. (C) Comparison of high light predicted fluxes (gray bars) and experimental fluxes (white bars) reported in [1]. Flux ranges determined by flux variability analysis are shown for the predicted fluxes. Upper bounds that exceed the Y-axis scale are indicated by an arrow and the upper bound flux value. (D) Correlation between high light predicted fluxes and experimental fluxes reported in [1]. Metabolic reactions and metabolites are indicated by their BiGG identifier (bigg.ucsd.edu). For (A) and (B), flux values are normalized to 100 units of RubisCO carboxylase flux. For (C) and (D) flux values are normalized to 100 units of inorganic carbon uptake. Abbreviations: ACONT: aconitase, CS: citrate synthase, ENO: enolase, FBA: fructose-bisphosphate aldolase, FBA3: sedoheptulose 1,7-bisphosphate D-glyceraldehyde-3-phosphate-lyase, FBP: fructose-bisphosphatase, FUM: fumarase, PGK: phosphoglycerate kinase, ICDH: isocitrate dehydrogenase, MDH: malate dehydrogenase, ME: malic enzyme, PDH: pyruvate dehydrogenase, PEPC: phosphoenolpyruvate carboxylase, PGI: glucose-6-phosphate isomerase, PGM: phosphoglycerate mutase, PGMT: phosphoglucomutase, PRUK: phosphoribulokinase, PYK: pyruvate kinase, RPE: ribulose-5-phosphate 3-epimerase, RPI: ribose-5-phosphate isomerase, SBP: sedoheptulose-bisphosphatase, SUCD: succinate dehydrogenase, TKT1: transketolase (S7P \rightarrow R5P + X5P), TKT2: Transketolase (F6P \rightarrow E4P + X5P), TPI: triosephosphate isomerase, ACLS: acetolactate synthase, ALAD: L-alanine-dehydrogenase, PGLYCP: phosphoglycolate phosphatase.

of the PKT pathway to the published oxidative pentose phosphate 592 581 (OPP) engineered pathway [17] for converting exogenous glucose 593 582 into 23BD (Fig. 7a,b). 583

First, using the model as a framework, we characterized the 58/ 596 OPP engineered pathway results to derive the necessary parame-585 ters for comparison. Based on the published culture conditions, the 597 586 feedstock was likely low light acclimated (30 μ mol photon m⁻² s⁻¹); 598 587 thus, we used the photophysiology values (a*_{cell}, P_O v. QF, pig- 599 588 ment composition, etc.) from our LL acclimated culture as simula- 600 589 tion parameters. Using the published results from Kanno et.al. [17], 601 590 we determined the glucose uptake rate of the optimized strain was 602 591

approximately 0.29 ± 0.1 mmol glucose gDW⁻¹ h⁻¹ during the first 3 days of culturing. Using a value of 0.27 mmol glucose gDW⁻¹ h⁻¹ and the biomass production rate set to 20% of the maximum, the experimental results were accurately recapitulated (Fig. S3a-c). Thus, these values were used for simulating photomixotrophic production of 23BD.

Using the derived glucose uptake and biomass partitioning values, we compared flux simulations from the OPP engineered pathway and the PKT designed pathway. Both designs resulted in identical titers and specific productivities at the published experimental conditions in Kanno et. al. (30 μ mol photon m⁻² s⁻¹, 1 g/L



Figure 6 Simulated versus experimental metabolic reaction fluxes for *S. elongatus* at high growth rates. (A) Predicted fluxes at high light by the *S. elongatus* genome-scale model *i*JB792 at low light. (B) Experimental reaction fluxes for *S. elongatus* as reported in [1]. Metabolic reactions and metabolites are indicated by their BiGG identifier (bigg.ucsd.edu). Flux values normalized to 100 units of inorganic carbon uptake are shown below the reaction abbreviations.

inoculation density) and were consistent with the experimental 623 603 results (Fig. 8a). Parsimonious FBA flux predictions between the 624 604 OPP and PKT designs suggested that while both designs resulted 625 605 606 in the same 23BD titer, the PKT design required 40% less flux 626 through the CBB cycle (Fig. 7a,b). Additionally, the PKT design 627 607 avoids carbon loss as CO₂ at both the OPP reaction phosphoglu- 628 608 conate dehydrogenase and at the pyruvate dehydrogenase (PDH) 629 609 reaction. The OPP pathway does generate 2 equivalents of NADPH 630 610 per glucose; however, these reactions would have to compete with 631 611 photosynthesis for the oxidized NADP+ pool, which may limit 632 612 the flux through the OPP pathway. The phosphoketolase enzyme 633 613 cleaves F6P into acetyl phosphate, which is converted to acetyl-634 614 CoA and used to generate biomass, and erythrose 4-phosphate, a 635 615 CBB intermediate. Thus, the PKT pathway coupled with a PDH 636 616 knockout would result in a maximum biomass partitioning of 33% 637 617 (2 out of 6 carbons from glucose) and effectively uncouple the CBB 638 618 from biomass production and towards 23BD biosynthesis. The flux 639 619 distributions suggest the PKT design could provide advantages 640 620 over the OPP pathway, especially at high irradiances when the 641 621 redox state of the NADPH pool may inhibit OPP flux. 622

Next, we assessed the impact of cell shading on 23BD production. Using an inoculation density of 1 g/L, simulations suggested increases in titer and specific productivity could be achieved for both photoautotrophic and photomixotrophic conditions (Fig. 8b). Holding the light intensity constant at 30 μ mol photon m⁻² s⁻¹ and varying the inoculation density indicated the photoautotrophic condition was more sensitive to the cell density compared to the photomixotrophic condition (Fig. 8c). We assessed the full production envelope from an inoculation density of 0.1 to 1 g/L and irradiance values from 30 to 900 μ mol photon m⁻² s⁻¹. The simulations suggested dramatic improvements in both 23BD titer and specific productivity could be achieved by increasing the available light (Fig. 8d). Additionally, the impact to production yields caused by high inoculation densities was dramatically attenuated at high irradiances. While it is important to mention these results are based on the photoautotrophic P_O vs. QF curves, even the photoautotrophic condition achieved theoretical titers 2-fold higher than the published photomixotrophic values with increased specific productivity.



Figure 7 Comparison of the phosphoketolase engineered pathway with oxidative pentose phosphate pathway. (A) Engineered pathway as described in [17] that routes extracellular glucose through the oxidative pentose phosphate toward 2,3-butanediol production. (B) Engineered pathway as described in this study that routes includes a phosphoketolase bypass toward 2,3butanediol production. Metabolic reactions and metabolites are indicated by their BiGG identifier (bigg.ucsd.edu). Flux values are in units mmol gram⁻¹ glucose uptake.

695

696

697

698

699

700

701

702 703

704

705

708

714

4. DISCUSSION 642

In this study we combined photophysiology constraints with a 643 genome-scale model of S. elongatus PCC 7942 to predict metabolic 706 644 differences between low and high light acclimated cultures. Over-707 645 all, the model underestimated the growth rate at both high and 646 low light but flux predictions were in good agreement with experi-709 647 mentally determined values. The genome-scale model predictions 710 648 allowed for an assessment of excitation energy routing through 711 649 650 the photosystem as a result of excess light absorption. Finally, we 712 651 employed this modeling construct to assess and improve current 713 elongatus production strategies for 2,3-butanediol. 652 S

The photophysiology constraints resulted in accurate predic- 715 653

tions of photoautotrophic growth. Whole cell absorption spectrum, cell dry weight and oxygen evolution are widely accessible experimental techniques that are often used to characterize photophysiology [50]. When coupled to genome-scale modeling, these inputs provided a detailed assessment of cellular metabolism to include growth rate and reaction fluxes. Such inputs could be used for realtime monitoring and/or process control parameters of large-scale, light-driven bioprocesses engineering.

While the upper bound of the simulations values approached the range of the experimental observations, the model tended to underestimate the growth rate at both high and low light. When determining the oxygen evolution rate, we did not supplement the sample with exogenous bicarbonate as it has been reported to affect photophysiology [47]. However, based on the cell densities used and photosythetic rates observed, it is likely the samples became carbon limited during the oxygen evolution experiment. This likely would have reduced P_{max} of the P_O vs. QF curve used to parameterize the model resulting in a underestimation of the growth rate.

Parsimonious FBA reaction fluxes predicted by the genomescale model were consistent with experimental ¹³C metabolic flux analysis [15, 1]. The observed accuracy is partially due to the nonredundant nature of the S. elongatus metabolic network. This lack of redundancy decreases the number of feasible flux states at the network level; evident by the similarity in experimental reaction fluxes in both ¹³C MFA studies. The agreement between the model predictions and MFA data suggests the photophysiology parameters are dominant constraints on photoautotrophy and the FBA assumption of optimality is appropriate. These factors coupled with emerging methods for combining constraint-based modeling with quantitative -omics data [52] brings a wide variety of phenotypes of interest to the phototrophic community into scope for in silico modeling.

While there were discrepancies in the simulation flux predictions and experimental data, the experimental values fell within the flux range of equally optimal solutions. For the high light/fast growth rate comparison (Fig. 6), the primary differences were in the Calvin-Benson cycle phosphatase reactions. The experimental values for these reactions did fall within the flux ranges determined by flux variability analysis (FVA) (Fig. 5c). The wide flux ranges reported by FVA are due to the fact these phosphatases are coupled to ATP-consuming kinases. As the GAM/NGAM assessment indicated, there was an excess of ATP at both LL and HL. Thus, when FVA is maximizing flux through the phosphatase, the corresponding kinase reaction has a large pool of ATP to drive the reaction pair resulting in a wide flux range. Despite these discrepancies, the overall flux into and out of the Calvin-Benson cycle was accurately predicted by the model. For the low light/slow growth rate comparison (Fig. 4), the primary differences were around the hypothesized malate dehydrogenase reaction. This MDH bypass of pyruvate kinase is hypothesized to be necessary due to regulatory inhibition of pyruvate kinase [22]. The MDH reaction, which has yet to be ascribed to a gene in S. elongatus, was added to our GEM based on biochemical evidence from MFA [15]. Regulatory mechanisms are not included in the genome-scale model; thus, the default prediction is for the bypass to not carry flux. While the pFBA solution predicted the MDH reaction carried no flux, the FVA flux ranges for this reaction were quite wide. Like the HL/fast growth rate comparison above, this was due to an ATP-coupled reaction (phosphoenolpyruvate synthase) driving flux through a loop that included MDH. Data-dependent incorporation of the PYK regulatory mechanism into a GEM could more accurately



Figure 8 Engineering photoautotrophic and photomixotrophic production of 2,3-butanediol in *S. elongatus*. (A) Specific productivity versus titer comparison of phosphoketolase (PKT) design (this study) with the oxidative pentose phosphate (OPP) engineered pathway as described in [17]. Solid and open markers represent OPP and PKT values respectively. Control marker: no carbon fixation (Rubisco bounds = 0). Validation marker: in silico simulation of the experimental conditions reported in [17] (inoculation density: 1 g/L, light: 30 μ mol photon m⁻² s⁻¹). (B) Specific productivity versus titer as a function of increasing light intensity. Select PAR values, in units of μ mol photon m⁻² s⁻¹, are indicated. (C) Specific productivity versus titer as a function of increasing inoculation density. (D) Specific productivity versus titer production envelope as a function of inoculation density and light intensity. Yellow shaded region: photoautotrophy. Blue shaded region: photomixotrophy. For all panels the experimental value as reported in [17] is shown and the total culture duration was 3 days.

constrain the flux through this bypass. Of note, despite the biochemical evidence from MFA showing an MDH-mediated bypass
of PYK, PYK is essential in vivo [43]. Therefore, in *S. elongatus*, the
in vivo MDH-mediated PYK bypass cannot carry sufficient flux to
maintain cell viability in the absence of PYK.

An advantage of genome-scale modeling over ¹³C MFA is the ⁷⁴² 721 ability to predict reaction fluxes beyond central metabolism. We 743 722 used this capability to assess alternate energy flows in S. elonga- 744 723 tus. Our simulations predicted approximately 37% and 58% of 745 724 the absorbed photons at low and high light respectively, were in 746 725 excess of growth requirements and energy transfer losses. These 747 726 numbers are likely overestimates since the energy transfer losses 748 727 728 included in the model are based on measurements in *S. elongatus* ⁷⁴⁹ permeaplasts [48] using chemical electron donor and acceptors; 750 729 thus, they represent the most efficient energy transfer rates. Lever-751 730 aging recent developments in cyanobacterial PAM fluorometry ⁷⁵² 731 techniques [35] may help constrain the physiological values. Still, 753 732 up to 40% of photosynthetic flux was reportedly directed to the 754 733 Mehler AET reaction in the cyanobacterium Synechocystis [12], sug- 755 734 gesting our simulated values are in a biologically realistic range. 735 756 The model predicts an increase in excitation energy directed to 757 736

PSI with an increase in QF (Table 4), consistent with known state transitions in cyanobacteria [33]. Additionally, our prediction of increased cyclic electron flow at high light, evident by increased flux through the NDH-1 complex, is in agreement with the known role of this complex in cyanobacteria [36][5]. The absolute fluxes through PSII versus PSI depends on accurate accounting of the metabolic cost of ROS detoxification at both reaction centers. Currently, the metabolic cost to repair the D1 protein, as represented in the model, drives the predicted excitation energy routing. Additionally, the GEM assigns a ROS generation rate that scales linearly with reaction flux. The kinetics of ROS generation are likely not linear in vivo and properly constraining the flux-dependent ROS generation rates stands as an area of improvement for the GEM. Still, the fold change in predicted PSI versus PSII flux predicted by the model was in close agreement in the change in Y(II) at the experimental QF (Table 4). This suggests coupling photon uptake constraints with the GEM assumption of optimality results in accurate qualitative assessments of excitation energy routing between low and high light.

It should be emphasized that FBA and MFA are complementary methods. Often GEM simulations result in multiple

mathematically-equivalent flux states for a given set of constraints. 814 758 MFA results restrict these alternate, equivalent optima to a nar-759 rower, biologically realistic subset. MFA results also validate or 760 816 refute assumptions in the GEM. For example, in S. elongatus a phos-761 817 phoketolase bypass of glycolysis is feasible based on the genome 762 818 annotation [6]. The GEM uses a hypothesized constraint that limits 763 this bypass flux. The agreement between the model predictions 764 and MFA data validates this constraint on phosphoketolase flux. 765 GEMs also support and extend discovery and engineering in MFA 766 experiments. Metabolic reconstructions define the core metabolism 821 767 of the organism, assisting in the development of the isotopomer 768 models needed for MFA. Additionally, ¹³C MFA experiments in 822 769 phototrophs are resource intensive. A validated GEM can explore 770 phenotypes and engineering strategies in silico prior to committing 771 823 resources on experimental validation of the predictions. Finally, 772 genome-scale models extend MFA flux measurement outside of 773 central metabolism either through direct constraints [30] or by 774 analyzing the full flux distribution from a simulation that was 775 validated against MFA central carbon flux, as we have done in this 776 study. 777

The framework presented in this study provided insights into 778 an existing 23BD production strain. Computational analysis of 779 the published data [17] established the glucose uptake rate of the 780 photomixotrophic strain as well as constrained the fraction of car-781 bon allocated to biomass. This analysis included the culture vessel 782 geometry, total culture volume, light intensity, inoculation density 783 and photophysiology; all parameters that can be optimized dur-784 ing bioprocess design. Characterization of the engineered strain 785 enabled an assessment of the theoretical yield, suggesting that 786 an increase in irradiance would result in higher production titers. 787 While our assessment assumed photophysiology parameters from 788 our study, replacing the P_{O} vs. QF curve with an experimentally 789 derived curve from the photomixotrophic strain would enable 790 a more accurate characterization of the production culture. The 791 phosphoketolase design suggested by our flux simulations may 792 793 provide unique S. elongatus bioengineering solutions. In particular, 794 growth-coupled engineering strategies could be developed for bioproducts that are synthesized from the acetyl-CoA pool, such as 795 isoprene [10]. 796

797 5. CONCLUSIONS

Engineering of cyanobacteria shows promise for generating energy-798 dense products with minimal input requirements. In this study we 799 presented an in silico methodology for accurately characterizing 800 photoautotrphic metabolism. These experimentally accessible con-801 straints enable phototrophic genome-scale engineering equivalent 802 to classical heterotrophic in silico design. Additionally, by incorpo-803 rating photophysiology constraints with engineering design, we 804 were able to assess an existing photomixotrophic engineering strat-805 egy and revealed the current design was light limited. Coupling genome-scale modeling-driven in silico design with experimental 807 validation, to include ¹³C metabolic flux analysis, is a promising 808 strategy to accelerate the iterative bioprocess design of light-driven 809 metabolic engineering strategies. 810

ACKNOWLEDGEMENTS

The authors would like to thank Marc Abrams for his critical review of the manuscript.

FUNDING

This work was supported by the U.S. Department of Energy, Office of Science, Office of Biological and Environmental Research, under Award Number DE-SC0008593 to B.O.P. and DE-SC0008595 to G.P.; the National Institutes of Health under research grants R35GM118290 to SSG; and the CRES postdoctoral award from the University of California San Diego to DGW.

COMPETING FINANCIAL INTERESTS

The authors declare no competing financial interests.

AUTHOR CONTRIBUTIONS

B.O.P and G.P. conceived and designed the study. JTB, DGW and DJ performed the experiments. JTB analyzed the data and performed the genome-scale modeling. All authors contributed to drafting and revising the manuscript.

LITERATURE CITED

- Abernathy, M. H., J. Yu, F. Ma, M. Liberton, J. Ungerer, *et al.*, 2017 Deciphering cyanobacterial phenotypes for fast photoautotrophic growth via isotopically nonstationary metabolic flux analysis. Biotechnology for Biofuels **10**: 273.
- [2] Adebiyi, A. O., L. J. Jazmin, and J. D. Young, 2014 13c flux analysis of cyanobacterial metabolism. Photosynthesis Research 126: 19–32.
- [3] Allakhverdiev, S. I. and N. Murata, 2004 Environmental stress inhibits the synthesis de novo of proteins involved in the photodamage-repair cycle of Photosystem II in Synechocystis sp. PCC 6803. Biochim Biophys Acta 1657: 23–32.
- [4] Bennett, A. and L. Bogorad, 1973 COMPLEMENTARY CHRO-MATIC ADAPTATION IN a FILAMENTOUS BLUE-GREEN ALGA. The Journal of Cell Biology 58: 419–435.
- [5] Bernat, G., J. Appel, T. Ogawa, and M. Rogner, 2010 Distinct roles of multiple NDH-1 complexes in the cyanobacterial electron transport network as revealed by kinetic analysis of p700+ reduction in various ndh-deficient mutants of synechocystis sp. strain PCC6803. Journal of Bacteriology 193: 292–295.
- [6] Broddrick, J. T., B. E. Rubin, D. G. Welkie, N. Du, N. Mih, et al., 2016 Unique attributes of cyanobacterial metabolism revealed by improved genome-scale metabolic modeling and essential gene analysis. Proceedings of the National Academy of Sciences 113: E8344–E8353.
- [7] Carroll, A. L., A. E. Case, A. Zhang, and S. Atsumi, 2018 Metabolic engineering tools in model cyanobacteria. Metabolic Engineering.
- [8] Ebrahim, A., J. A. Lerman, B. O. Palsson, and D. R. Hyduke, 2013 COBRApy: COnstraints-Based Reconstruction and Analvsis for Python. BMC Systems Biology 7: 74.
- [9] Feist, A. M. and B. O. Palsson, 2010 The biomass objective function. Current Opinion in Microbiology **13**: 344–349.
- [10] Gao, X., F. Gao, D. Liu, H. Zhang, X. Nie, *et al.*, 2016 Engineering the methylerythritol phosphate pathway in cyanobacteria for photosynthetic isoprene production from CO2. Energy & Environmental Science 9: 1400–1411.
- [11] Gudmundsson, S., L. Agudo, and J. Nogales, 2017 Applications of genome-scale metabolic models of microalgae and cyanobacteria in biotechnology. In *Microalgae-Based Biofuels and Bioproducts*, pp. 93–111, Elsevier.

- [12] Helman, Y., 2005 Fractionation of the three stable oxygen isotopes by oxygen-producing and oxygen-consuming reactions in photosynthetic organisms. PLANT PHYSIOLOGY 138: 2292–2298.
- [13] Hirokawa, Y., Y. Maki, T. Tatsuke, and T. Hanai, 2016 Cyanobacterial production of 1,3-propanediol directly from carbon dioxide using a synthetic metabolic pathway. Metabolic Engineering 34: 97–103.
- [14] Jallet, D., M. A. Caballero, A. A. Gallina, M. Youngblood, and G. Peers, 2016 Photosynthetic physiology and biomass partitioning in the model diatom Phaeodactylum tricornutum grown in a sinusoidal light regime. Algal Research 18: 51–60.
- [15] Jazmin, L. J., Y. Xu, Y. E. Cheah, A. O. Adebiyi, C. H. Johnson, *et al.*, 2017 Isotopically nonstationary 13C flux analysis of cyanobacterial isobutyraldehyde production. Metabolic engineering **42**: 9–18.
- [16] Kanno, M. and S. Atsumi, 2016 Engineering an obligate photoautotrophic cyanobacterium to utilize glycerol for growth and chemical production. ACS Synthetic Biology 6: 69–75.
- [17] Kanno, M., A. L. Carroll, and S. Atsumi, 2017 Global metabolic rewiring for improved CO2 fixation and chemical production in cyanobacteria. Nature Communications 8: 14724.
- [18] Kim, W. J., H. U. Kim, and S. Y. Lee, 2017 Current state and applications of microbial genome-scale metabolic models. Current Opinion in Systems Biology 2: 10–18.
- [19] King, Z. A., C. J. Lloyd, A. M. Feist, and B. O. Palsson, 2015 Next-generation genome-scale models for metabolic engineering. Current Opinion in Biotechnology 35: 23–29.
- [20] Kirilovsky, D. and C. A. Kerfeld, 2012 The orange carotenoid protein in photoprotection of photosystem ii in cyanobacteria. Biochimica et Biophysica Acta (BBA) - Bioenergetics 1817: 158 – 166, Photosystem II.
- [21] Knoop, H., M. Gründel, Y. Zilliges, R. Lehmann, S. Hoffmann, et al., 2013 Flux balance analysis of cyanobacterial metabolism: The metabolic network of synechocystis sp. PCC 6803. PLoS Computational Biology 9: e1003081.
- [22] Knowles, V. L., C. S. Smith, C. R. Smith, and W. C. Plaxton, 2001 Structural and regulatory properties of pyruvate kinase from the Cyanobacterium SynechococcusPCC 6301. Journal of Biological Chemistry 276: 20966–20972.
- [23] Kramer, D. M., G. Johnson, O. Kiirats, and G. E. Edwards, 2004 New fluorescence parameters for the determination of QARedox state and excitation energy fluxes. Photosynthesis Research 79: 209–218.
- [24] Lan, E. I., D. S. Chuang, C. R. Shen, A. M. Lee, S. Y. Ro, et al., 2015 Metabolic engineering of cyanobacteria for photosynthetic 3-hydroxypropionic acid production from CO 2 using synechococcus elongatus PCC 7942. Metabolic Engineering 31: 163–170.
- [25] Lan, E. I. and C. T. Wei, 2016 Metabolic engineering of cyanobacteria for the photosynthetic production of succinate. Metabolic Engineering 38: 483–493.
- [26] Lea-Smith, D. J., P. Bombelli, R. Vasudevan, and C. J. Howe, 2016 Photosynthetic, respiratory and extracellular electron transport pathways in cyanobacteria. Biochimica et Biophysica Acta (BBA) - Bioenergetics 1857: 247–255.
- [27] Levering, J., J. Broddrick, and K. Zengler, 2015 Engineering of oleaginous organisms for lipid production. Current opinion in biotechnology 36: 32–39.
- [28] Lewis, N. E., K. K. Hixson, T. M. Conrad, J. A. Lerman, P. Charusanti, *et al.*, 2010 Omic data from evolved E. coli are consistent with computed optimal growth from genome-scale

models. Molecular Systems Biology 6: 390.

- [29] Machado, D. and M. Herrgård, 2014 Systematic evaluation of methods for integration of transcriptomic data into constraintbased models of metabolism. PLoS Computational Biology 10: e1003580.
- [30] Martín, H. G., V. S. Kumar, D. Weaver, A. Ghosh, V. Chubukov, et al., 2015 A method to constrain genome-scale models with 13c labeling data. PLOS Computational Biology 11: e1004363.
- [31] McEwen, J. T., I. M. P. Machado, M. R. Connor, and S. Atsumi, 2012 Engineering synechococcus elongatus PCC 7942 for continuous growth under diurnal conditions. Applied and Environmental Microbiology 79: 1668–1675.
- [32] Moore, L. R., R. Goericke, and S. W. Chisholm, 1995 Comparative physiology of synechococcus and prochlorococcus: influence of light and temperature on growth, pigments, fluorescence and absorptive properties. Marine Ecology Progress Series 116: 259–275.
- [33] Mullineaux, C. W., 2004 State transitions: an example of acclimation to low-light stress. Journal of Experimental Botany 56: 389–393.
- [34] Nogales, J., S. Gudmundsson, E. M. Knight, B. O. Palsson, and I. Thiele, 2012 Detailing the optimality of photosynthesis in cyanobacteria through systems biology analysis. Proceedings of the National Academy of Sciences 109: 2678–2683.
- [35] Ogawa, T., M. Misumi, and K. Sonoike, 2017 Estimation of photosynthesis in cyanobacteria by pulse-amplitude modulation chlorophyll fluorescence: problems and solutions. Photosynthesis Research 133: 63–73.
- [36] Ohkawa, H., H. B. Pakrasi, and T. Ogawa, 2000 Two types of functionally distinct NAD(p)h dehydrogenases inSynechocystissp. strain PCC6803. Journal of Biological Chemistry 275: 31630–31634.
- [37] Oliver, J. W. K., I. M. P. Machado, H. Yoneda, and S. Atsumi, 2013 Cyanobacterial conversion of carbon dioxide to 2,3-butanediol. Proc Natl Acad Sci U S A 110: 1249–1254.
- [38] Oliver, N. J., C. A. Rabinovitch-Deere, A. L. Carroll, N. E. Nozzi, A. E. Case, *et al.*, 2016 Cyanobacterial metabolic engineering for biofuel and chemical production. Current Opinion in Chemical Biology 35: 43–50.
- [39] Orth, J. D., I. Thiele, and B. O. Ø. Palsson, 2010 What is flux balance analysis? Nature biotechnology 28: 245–248.
- [40] Pérez, F., B. E. Granger, and P. rez Fernando, 2007 IPython: A system for interactive scientific computing. Computing in Science and Engineering 9: 21–29.
- [41] Platt, T., C. L. Gallegos, and W. G. Harrison, 1980 Photoinhibition of Photosynthesis in Natural Assemblages of Marine-Phytoplankton. Journal of Marine Research 38: 687–701.
- [42] Ritchie, R. J., 2008 Universal chlorophyll equations for estimating chlorophylls a, b, c, and d and total chlorophylls in natural assemblages of photosynthetic organisms using acetone, methanol, or ethanol solvents. Photosynthetica 46: 115–126.
- [43] Rubin, B. E., K. M. Wetmore, M. N. Price, S. Diamond, R. K. Shultzaberger, *et al.*, 2015 The essential gene set of a photosynthetic organism. Proc Natl Acad Sci U S A 112: E6634–43.
- [44] Schindelin, J., C. T. Rueden, M. C. Hiner, and K. W. Eliceiri, 2015 The ImageJ ecosystem: An open platform for biomedical image analysis. Mol Reprod Dev 82: 518–529.
- [45] Schreiber, U., W. Bilger, and C. Neubauer, 1995 Chlorophyll fluorescence as a nonintrusive indicator for rapid assessment of in vivo photosynthesis. In *Ecophysiology of Photosynthesis*, pp. 49–70, Springer Berlin Heidelberg.

- [46] Schuurmans, R. M., P. van Alphen, J. M. Schuurmans, H. C. P. Matthijs, and K. J. Hellingwerf, 2015 Comparison of the photosynthetic yield of cyanobacteria and green algae: Different methods give different answers. PLOS ONE 10: e0139061.
- [47] Shimakawa, G., K. Shaku, and C. Miyake, 2018 Reductioninduced suppression of electron flow (rise) is relieved by non-atp-consuming electron flow in synechococcus elongatus pcc 7942. Frontiers in Microbiology **9**: 886.
- [48] Stamatakis, K., M. Tsimilli-Michael, and G. C. Papageorgiou, 2014 On the question of the light-harvesting role of β-carotene in photosystem II and photosystem I core complexes. Plant physiology and biochemistry : PPB 81: 121–7.
- [49] Tichy, M., W. Vermaas, U. Information, S. Pcc, M. Tichy, et al., 1999 In vivo role of catalase-peroxidase in synechocystis sp. strain pcc 6803. J. Bacteriol pp. 1875–1882.
- [50] Wagner, H., T. Jakob, and C. Wilhelm, 2006 Balancing the energy flow from captured light to biomass under fluctuating light conditions. New Phytologist 169: 95–108.
- [51] Young, J. D., A. A. Shastri, G. Stephanopoulos, and J. A. Morgan, 2011 Mapping photoautotrophic metabolism with isotopically nonstationary 13c flux analysis. Metabolic Engineering 13: 656–665.
- [52] Yurkovich, J. T. and B. O. Palsson, 2018 Quantitative -omic data empowers bottom-up systems biology. Current Opinion in Biotechnology 51: 130 – 136, Systems biology • Nanobiotechnology.

- Supplementary Material for "Predicting the metabolic capabilities of *S. elongatus* PCC 7942 adapted to different
 light regimes"
- 3 Authors: Jared T. Broddrick, David G. Welkie, Denis Jallet, Susan S. Golden, Graham Peers and Bernhard O. Palsson
- ⁴ The following Supporting Information is available for this article:
- 5 Modeling files can be found at http://systemsbiology.ucsd.edu/Downloads/SupplementalData



Fig. S1. Effect of path length correction on quantum flux calculations *S. elongatus*. Accounting for cell shading in the determination of quantum flux affects the calculated oxygen evolution rate at the experimental conditions. +/- PL refers to plots with (+) or without (-) accounting for path length. Abbreviations. LL: low light, HL: high light, PL: path length, QF: quantum flux.



Fig. S2. Chlorophyll fluorescence parameters versus quantum flux for *S. elongatus*. (A) Quantum yield of photosystem II (PSII) versus QF curves. The maximal quantum yield (Fv/Fm) is equal to the y-intercept of the curves. (B) Fraction of open reaction centers (RCs) versus quantum flux. Vertical dashed lines represent the maximum quantum flux received by the cultures at the experimental irradiance. Abbreviations. LL: low light, HL: high light, QF: quantum flux.



Fig. S3. In silico recapitulation of an S. elongatus strain designed for 2,3-butanediol production. (A) Biomass, (B) 2,3-butanediol (23BD) production and (C) glucose consumption over the first 3 days of culturing. Experimental data points (Exp) were taken from published values (1). Simulations were set with the biomass production at 20% of the maximum and a glucose uptake rate of 0.27 mmol glc gDW⁻¹ h⁻¹

Table S1. Content edits to *i*JB785 in the construction of *i*JB792.

Reaction ID	Reaction name	Notes
MPTSS	Molybdopterin synthase sulfurylase	Added. Molybdopterin cofactor biosynthesis.
MOADSUx	MoaD sulfuration (nadh, assumed)	Added. Molybdopterin cofactor biosynthesis.
GTPC	GTP 3,8-cyclase	Added. Molybdopterin cofactor biosynthesis.
CPMPS	Cyclic pyranopterin monophosphate synthase	Added. Molybdopterin cofactor biosynthesis.
MPTS	Molybdopterin synthase	Added. Molybdopterin cofactor biosynthesis.
MPTAT	Molybdopterin adenylyltransferase	Added. Molybdopterin cofactor biosynthesis.
MOCOS	Molybdenum cofactor synthase	Added. Molybdopterin cofactor biosynthesis.
MDH	Malate dehydrogenase	Added. Based on fluxomics data (2). Gene reaction rule unknown.
ORNTA	Ornithine transaminase	Deleted. Gene model results in a truncated protein that appears to be inactive in vivo (3)

1. Kanno M, Carroll AL, Atsumi S (2017) Global metabolic rewiring for improved CO2 fixation and chemical production in cyanobacteria. Nature Communications 8:14724. 6 7

 Jazmin LJ, et al. (2017) Isotopically nonstationary 13C flux analysis of cyanobacterial isobutyraldehyde production. *Metabolic engineering* 42:9–18.
 Broddrick JT, et al. (2016) Unique attributes of cyanobacterial metabolism revealed by improved genome-scale metabolic modeling and essential gene analysis. *Proceedings of the National Academy* 8 9 of Sciences 113(51):E8344-E8353.